

Failure Modes and Effects Analysis of Biorefinery Pathways

November 2023

hanging the World's Energy Future

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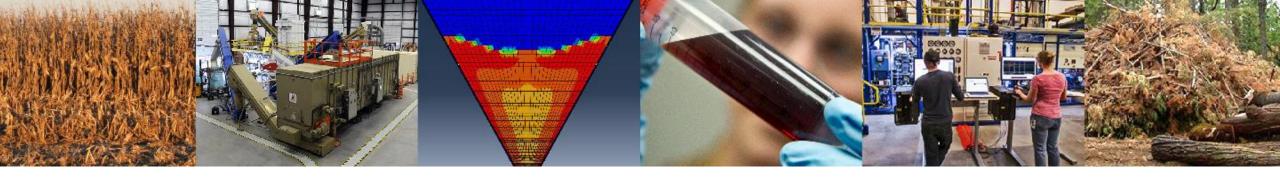
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2023 AIChE Annual Meeting Feedstock Conversion Interface Consortium: Understanding Feedstock Variability to Enable Next Generation Biorefineries

November 6, 2023

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U.S. DEPARTMENT OF ENERGY

Acknowledgement







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Risk: Variability in Biomass Properties



Variability in biomass feedstock properties translates to **risk** for bio-projects

- Shutting down of existing biorefineries
- High capital costs for emerging bio-projects

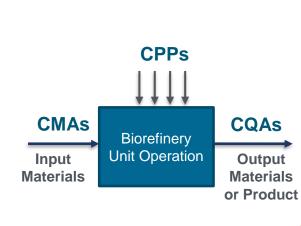
Variability in critical material attributes

Technical Risk

- Equipment failure
- Inconsistent product quality
- Environmental consequences
- Safety

Quality by Design

Emphasis on systematic understanding of processes and control



Example: Jet Fuel Production

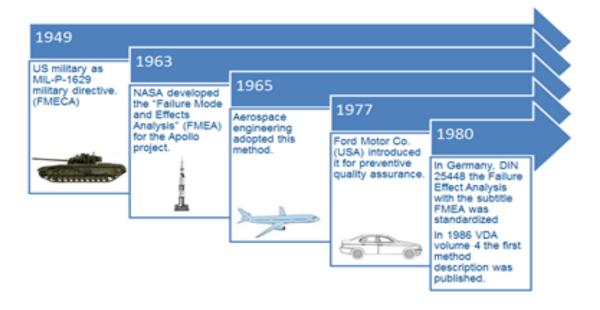
CMA: lignin content, H_2 content CPP: process design & operation CQA: Aromatic content < 25%



Process Risk Assessment

FMEA Background





Benefits Failure Mode and Effects Analysis (FMEA)

- Well-accepted risk assessment tool
- Combining qualitative and quantitative data
- Easily adaptable
- Couples well with Quality-by-Design approaches

Overview

- Extensive interviews with subject matter experts (SMEs)
- Systematic semi-quantitative analysis based on failure identification for a given operation or system of operations for a process
- Failure defined as "not performing or producing as intended".

Ranking of **Severity** (S), **Occurrence** (O) and **Detection** (D) by Subject Matter Experts to calculate **Risk Priority Number** (RPN).

 $RPN = S \times O \times D = Risk \times D$

Semi-quantitative criticality value for each identified CMA, CPP, CQA for given material/unit operation/system configuration

Systematic Data Collection



Date: Interviewee: Interviewer: Which unit operation sh		nterview F	orm				• Equ	nation (uipment eration (scal
What is the primary purp Should this be considered	pose of this unit operation	.?					• Lev	el of ex	perti
Can you briefly describe Inputs parameters/pro- outputs								ablish p figuratio	
What scale is the target u 1ab ->0.5 DTP pre pilot - 0.5 I pilot - 1 DTPD demonstration	DTPD - 50 DTPD	r							
	Background								
What scale do we usuall				ollow-up Questions:					
	Interviewer		FG	blow-up Questions:					
	Date								
How often are we runnin	Rev								
	Unit Operation/Equipment								
	Material								
	Input format (approx)								
	Output format (approx)								
	System Design (Product)								
	Nameplate Capacity		-						
	TRL (A-C)								
	Decesso Stevillevent	Detential Failure Made	Detential Failure Fffere	COA	Laura		Detential Course	СМА	CDD
	Process Step/Input	Potential Failure Mode	Potential Failure Effect What is the impact on the customer if this failure is not prevented or corrected?		Layer Failure/CQA impacts: Process efficiency (Proc), Product quality (Prod), Economics (Eco), Sustainability (LCA)	SEVERITY (1 - 10)	Potential Causes What causes the step, change or feature to go wrong? (how could it occur?)	CMA Identified CMA (and ranges if known) associated with failure and cause	CPP Identified CPP associated with failure and cause
									<u> </u>
				+					

cted - Background

- es
- ion
- se for combinations of erial/product (system)
- ry scope (e.g., material, system

What controls exist that either prevent or detect the failure?

Potententia

Systematic Data Collection



Date	FMEA Interview Form							Information Collected - F							
Interviewee:								/			aal!4.				
Interviewer:							• Imp	acts (pi	OCe	SS.	dualit				
Which unit operation sh	ould we focus on?						-								
							•	CQAs	— CI	TTTC	al Qua				
What is the primary pur	pose of this unit operation	1?					· Sev	verity (1	-10)						
									10)						
Should this be consider	ed one unit operation?						 Caι 	ises							
Can you briefly describ	e how it works?						•	CMAs		ritic	ol mot				
 Inputs 	now it works.						•	CIVIAS	- 0	IIIC	Jai mai				
 parameters/pro outputs 	cess						•	CPPs	– Cr	itic	al proc				
											•				
What scale is the target	unit operation intended fo	or					• Occ	currence	e (1-	10)				
 1ab - >0.5 DTF 	-								, , ,	~					
 pre pilot – 0.5 pilot – 1 DTPI 							 Det 	ection a	and	J01	ntrois				
 pilot – 1 DTPI demonstration 								а а.С. а. с. Г		1.	4 0)				
 commercial – 3 	>50DTPD						 Det 	ection F	kank	(1	-10)				
	Background														
What scale do we usual				llow-up Questions:			1								
	Interviewer		FO	llow-up Questions:											
	Date														
How often are we runni	r Rev														
	Unit Operation/Equipment														
	Material														
	Input format (approx)														
	Output format (approx)														
	System Design (Product)														
	Nameplate Capacity														
	TRL (A-C)														
	Process Step/Input	Potential Failure Mode	Potential Failure Effects	s CQA	Layer	ŝ.	Potential Causes	СМА	СРР	10)	Current Controls				
	What is the process step, change or feature under investigation?	In what ways could the step, change or feature go wrong?	What is the impact on the customer if this failure is not prevented or corrected?	What CQAs are impacted directly or indirectly by this failure	Failure/CQA impacts: Process efficiency (Proc), Product quality (Prod), Economics (Eco),	EVERITY (1 - 10)	What causes the step, change or feature to go wrong? (how could it occur?)	Identified CMA (and ranges if known) associated with failure and cause	Identified CPP associated with failure and cause		hat controls exist that either revent or detect the failure?				
					Sustainability (LCA)	s	,			000					

ailures

- y, cost, sustainability)
 - ality Attributes
 - terial attributes
 - cess parameters

Potententia

Guidance Scales



Severity

Effect	Rank	Criteria
Minor	1	None to minor disruption to production line. A small portion (< 5%) of product may have to be reworked online.
		Low disruption to production line. A portion (< 15%) of product may have to be reworked online. Process up.
Low	3	Minor annoyance exists.
		Moderate disruption to production line. A small portion (>20%) of product may have to be reworked online.
Moderate	6	Process up. Some inconvenience exists.
		High disruption to production line. A portion (>30%) of product may have to be scrapped. Process may be
High	8	stopped. Customer dissatisfied.
		Major disruption to production line. Close to 100% of product may have to be scrapped. Process unreliable.
Very high	10	Failure occurs without warning. Customer very dissatisfied. May endanger operator and/or equipment.

Occurrence

Occurrence	Rank	Criteria
		Failure is very unlikely. No failures
Remote	1	associated with similar processes.
		Few failures. Isolated failures associated
Low	3	with similar processes.
		Occasional failures associated with similar
Moderate	6	processes.
		Repeated failures. Similar processes have
High	8	often failed
Very high	10	Process failure is almost inevitable.

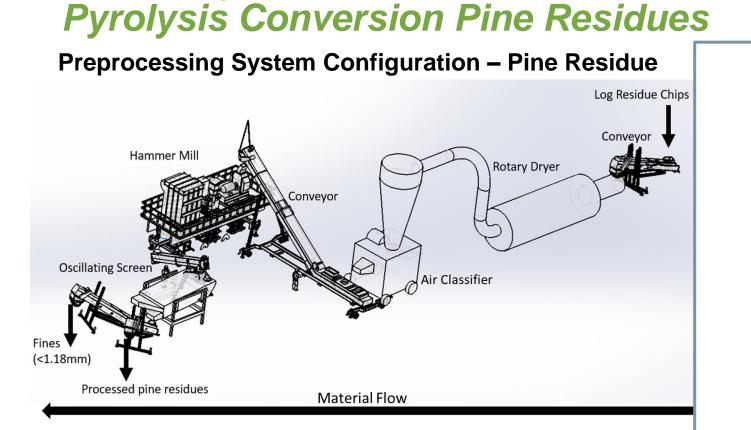
Detection

Detection	Rank	Criteria
		Process control will almost certainly detect or prevent the potential cause
Almost certain	1	of subsequent failure mode.
		High chance the process control will detect or prevent the potential cause
High	3	of subsequent failure mode.
		Moderate chance the process control will detect or prevent the potential
Moderate	6	cause of subsequent failure mode.
		Remote chance the process control will detect or prevent the potential
Remote	8	cause of subsequent failure mode.
		There is no process control. Control will not or cannot detect the potential
Very uncertain	10	cause of subsequent failure mode.

Systematic Data Collection



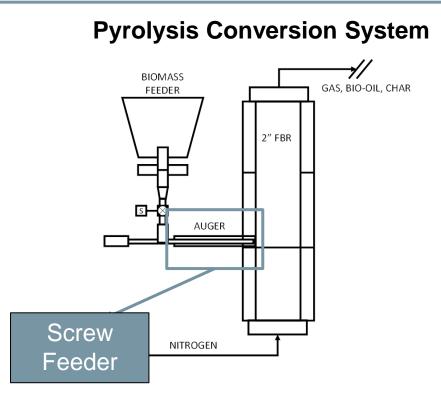
Date: Interviewee: Interviewee: Which unit operation should we focus on? What is the primary purpose of this unit operation? What is the primary purpose of this unit operation? Should this be considered one unit operation? Can you briefly describe how it works? Inputs parameters/process outputs What scale is the target unit operation intended for 1ab - >0.5 DTPD pilot - 1 DTPD otemostration - 50 DTPD otemostration - 50 DTPD commercial - >50 DTPD						 Information Collected - Mitigation What can be done to Reduce severity Decrease occurrence Improve detection Categorize as Idea Proposed scope In-Process Implemented 							
What scale do we usual How often are we runni	Interviewer Date r Rev		Fo	llow-up Questions:									
	Unit Operation/Equipment Material Input format (approx) Output format (approx) System Design (Product) Nameplate Capacity TRL (A-C)												
	Process Step/Input What is the process step, change or feature under investigation?	Potential Failure Mode	Potential Failure Effect What is the impact on the customer if this failure is not prevented or corrected?		Layer Failure/CQA impacts: Process efficiency (Proc), Product quality (Prod), Economics (Eco), Sustainability (LCA)	SEVERITY (1 - 10)	Potential Causes What causes the step, change or feature to go wrong? (how could it occur?)	CMA Identified CMA (and ranges if known) associated with failure and cause	CPP Identified CPP associated with failure and cause	Ň.	Current Controls What controls exist that either prevent or detect the failure?	DETECTION (1 - 10)	Potenten



- FMEA performed on theoretical **system-wide**
- FMEA on each individual **unit operation**

FMEA Implementation:





- FMEA performed on one problematic unit operation
- Experimental results for identified failures

Saha, N. et al. *Fuel Processing Technology* 245 (2023): 107725. <u>https://doi.org/10.1016/j.fuproc.2023.107725</u>

High Temperature Screw Feeder FMEA



Failure	Impacts	CQAs	SEVERITY	Causes	CMAs	CPPs	OCCURRENCE	Detection methods	DETECTION	RPN
Feed system plug	 Complete Shutdown Downtime Potential equipment damage Product quality 	 Throughput Biomass feedrate Product quality 	10	 Sudden and severe build-up of material: Particle agglomeration and compaction In-feed and out-feed inconsistencies Reactions between properties and heated auger Auger properties 	 Particle size and distributions Moisture (<10%; >25-30%) Particle surface Compaction Particle density 	 Auger geometry Temperature profile Auger speed 	1	Visual observations by trained operator of differential pressure and motor current		100
Char buildup on auger	 Reduction in throughput Potential shutdown Downtime Product quality 	 Biomass feedrate Throughput Particle size (fines) Product quality 	8	 Particle agglomeration on auger: Auger flight deformation Reactions between properties and heated auger Particle agglomeration through volatilization and recondensation. 	 Particle size and distributions Moisture (<10%; >25-30%) Particle morphology Particle surface Particle density Volatiles Flow properties Inorganics composition 	 Auger geometry (screw pitch) Auger metallurgy Auger temperature profile Auger cooling configuration Auger speed Auger surface finish Auger fill volume Sweep gas rate 	8	 Scheduled maintenance burnouts Observed increase in motor current, temperature fluctuation in reactor bed, and pyrolysis exit gas rates by trained operator. 	3	192
Deviation from target particle size through agglomeration or attrition	 <u>Attrition</u> Reactor performance and yield efficiency Further particle agglomeration and/or plugging Increased wear rate Material flowability <u>Agglomeration</u> Decline in fluidized bed performance (incomplete conversion) Plugging or buildup downstream Product quality Downtime based on burnout requirements 	 Particle Size Distributions Biomass Feedrate Consistency Product Quality Process Efficiency 	6	 <u>Attrition</u> Particles trapped in flights <u>Agglomeration</u> Heat flux issue in augur Heat transfer from auger to particles Incoming particle properties causing cohesion. Slower rotation speeds contributing to longer particle-auger contact time. 	 Particle size distribution Moisture Particle morphology Particle surface roughness Volatile content 	 Auger geometry Temperature profile Rotation speed Compression forces 	6	Observed increase in motor current and temperature fluctuation in reactor bed	6	216

High Temperature Screw Feeder FMEA

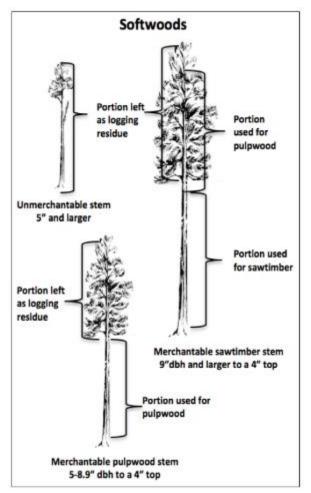


Failure	Impacts	CQAs	SEVERITY	Causes	CMAs	CPPs	CURRENCE	Detection methods	DETECTION	RPN
Feed system plug	 Complete Shutdown Downtime Potential equipment damage Product quality 	 Throughput Biomass feedrate Product quality 		 Reactions between properties and heated 	 Particle size and distributions Moisture (<10%; >25-30%) Particle surface Compaction Particle density 	 Auger geometry Temperature profile Auger speed 	001	Visual observations by trained operator of differential pressure and motor current		100

Flowability Biomass – Feed System Plugs



- Material Pine Residue Whole Chips
- Material Attributes:
 - Approximate Particle Size (2, 4, 6 mm)
 - Moisture Levels (Dry (less than 5%), 20% and 40%)
 - Anatomical Fractions (whole, stem, bark, needles)
- Process Parameters
 - Auger Rotational Speed (24, 36, 48 rpm)
- Parameters of interest
 - Flowrate
 - Power Consumption



Depiction of products produced from different fractions of Southeastern softwood trees (*Figure credit:* Bardon and Hazel, 2014).

Flowability Biomass – Feed System Plugs



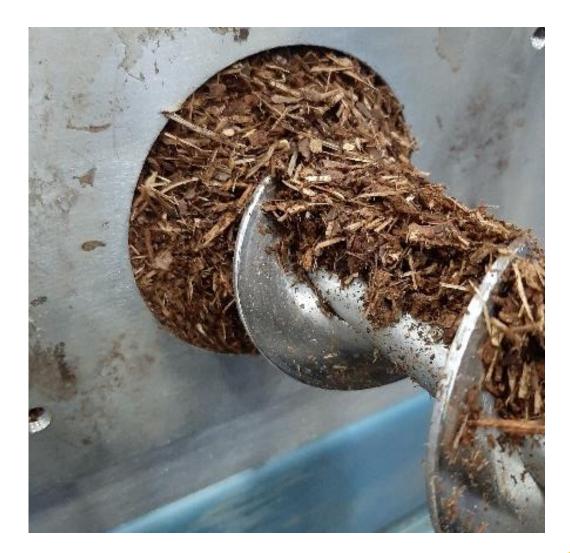
Sample		Power x 10 ³ (kW)	Flowrate (kg/hr)					
	24 RPM	36 RPM	48 RPM	24 RPM	36 RPM	48 RPM		
2mm_Dry	8.1 ± 5.4	7.3 ± 6.7	4.1 ± 7.5	37.3 ± 1.2	58.3 ± 1.6	78.3 ± 2.1		
4mm_Dry	37.6 ± 16.4	31.4 ± 22.0	24.8 ± 20.6	35.0 ± 1.6	55.5 ± 1.7	73.5 ± 2.8		
6mm_Dry	85.3 ± 42.0	81.1 ± 59.6	25.0 ± 27.0	35.4 ± 1.8	56.0 ± 3.8	76.1 ± 5.34		
2mm_20%MC	16.2 ± 10.5	14.2 ± 11.5	14.2 ± 12.7	38.0 ± 1.2	56.5 ± 1.8	73.9 ± 2.3		
4mm_20%MC	77.8 ± 40.0	67.1 ± 56.0	61.0 ± 62.5	37.5 ± 1.6	56.0 ± 2.5	73.4 ± 3.2		
6mm_20%MC	229.0 ± 122.2	171.0 ± 116.5	194.3 ± 167.0	35.9 ± 2.2	55.4 ± 2.9	74.9 ± 5.5		
2mm_40%MC	22.9 ± 8.6	17.8 ± 8.4	13.0 ± 10.7	46.4 ± 1.5	68.4 ± 2.2	89.3 ± 2.5		
4mm_40%MC	79.1 ± 36.0	90.9 ± 45.3	120.6 ± 40.0	53.6 ± 2.1	80.3 ± 2.6	106.6 ± 4.1		
6mm_40%MC	143.2 ± 70.5	118.0 ± 71.9	106.2 ± 82.3	55.0 ± 2.9	82.2 ± 4.7	106.5 ± 5.0		

Whole chip material

- Increases in rotational frequency resulted increases in flow rate and decrease in power consumption
- Increases in particle size increased power consumption
- Higher flow rates in general seen with increases in moisture

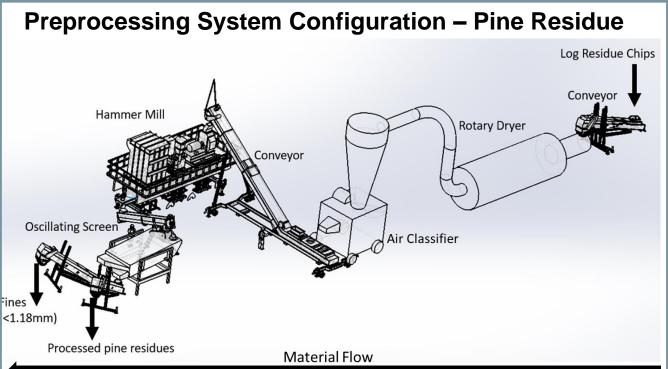
Plug Conditions – Higher Moistures





- Needle rich material
- 4 mm particle size
- 40% moisture

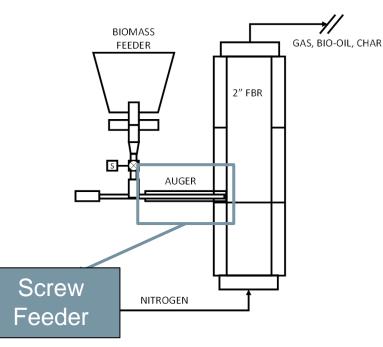
FMEA Implementation: Pyrolysis Conversion Pine Residues



- FMEA performed on theoretical **system-wide**
- FMEA on each individual unit operation



Pyrolysis Conversion System



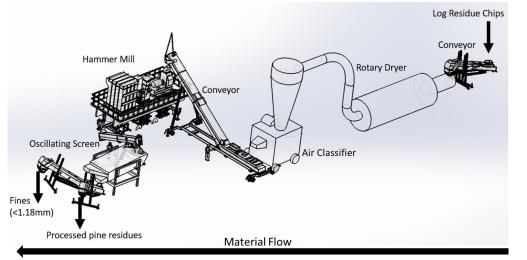
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System Wide FMEA Results



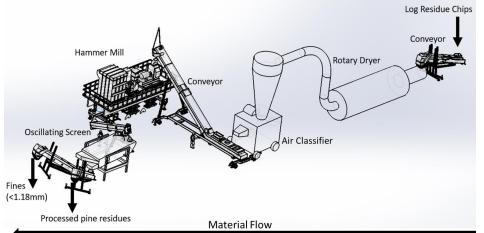


- FMEA interviews on whole system
- FMEA interviews on each unit operation
- Target CQAs
 - Moisture (<10%)
 - Fixed Carbon (≥ 18%)
 - Particle Size (1.18–6mm)
 - Ash Content ($\leq 1.75\%$)
 - Throughput

Unit Operation	System	Dryer (Rotary)	Air Classifier	Grinder (Hammer mill)	Oscillating Screen
Nameplate Capacity Throughput	1 tons/hr	5 tons/hr	1 tons/hr	5 tons/hr	5 tons/hr
Typical Throughput	1 ton/hr	1 ton/hr	1 tons/hr	5 tons/hr	3 ton/hr
Input Format	<2" chipped residues	<2" chipped residues	<2" chipped residues	<2" white wood rich	< ¹ / ₂ " white wood rich
Output Format	1.18mm > white wood rich material < 6mm	<2" chipped residues	Heavy stream: white wood rich; Light stream(s): bark, needle, fines rich	1⁄2" minus white wood rich material	1.18mm > white wood rich material < 6mm
Fixed process parameters	Screen sizes and mill speed on grinder and screen size on oscillating screen			Screen size: ¹ ⁄ ₂ " Mill speed	Top screen: 1⁄4" Bottom screen: 10 mesh

FMEA on Preprocessing





Highlights

• Rotary dryer failures resulted in cascading failures downstream due to increased moisture.

- Fire risk

- Best control for ash content (lowest risk scores).
- Fixed carbon risk score based on lack of chemical specific sensors.

Critical Quality Attributes	Specification	Impacting Unit Operation(s)	Max RPN ^a (layer)	Mitigation
Childal Quality Attributes	Specification		wax RPN [®] (layer)	Use of visual AI
Moisture content	≤ 10%	Rotary Dryer	180 (Product Quality)	1
			144 (Process Efficiency)	to detect non-
Fixed carbon	≥ 18%	Air Classifier	192 (Product Quality)	white wood
			72 (Process Efficiency)	concentrations
Particle size	1.18mm–6mm	Grinder, Oscillating Screen, Air Classifier	108 (Process Efficiency)	RPN 72
Ash content	≤ 1.75%	Air Classifier, Oscillating Screen	90 (Process Efficiency)	
			80 (Product Quality)	
Throughput	Not defined	All equipment	180 (Product Quality)	
			54 (Process Efficiency)	

^aRPN=risk priority number; ranges from 1-1000 and is based on quantifying the severity, occurrence, and detection of a given risk



Key Takeaways and Future Work



Outcomes

- Standardized framework to represent and semi-quantitatively rank CMAs, CPPs, and CQAs in the context of a 'Failure' across multiple unit operations.
- Help in identifying experimental needs.
- System-wide identification of pinch points
- Ability to quantify impacts of research driven improvements through mitigation.

Challenges

- Very dependent on SMEs expertise
- Unidentified critical properties
- Unidentified impacts (e.g., Economic)

- Multiple SMEs
- Use of literature or experimental results
 - Input for techno-economic analyses



Questions





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