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OXIDATION, VOLATILIZATION, AND REDISTRIBUTION OF MOLYBDENUM FROM TZM ALLOY IN AIR

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ABSTRACT

The excellent high temperature strength and thermal conductivity of molybdenum-base alloys provide attractive features for components in advanced magnetic and inertial fusion devices. Refractory metal alloys react readily with oxygen and other gases. Oxidized molybdenum in turn is susceptible to losses from volatile molybdenum trioxide species, (MoO₃)_m, in air and the hydroxide, MoO₂(OH)₂, formed from water vapor. Transport of radioactivity by the volatilization, migration, and re-deposition of these volatile species during a potential accident involving a loss of vacuum or inert environment represents a safety issue. In this report we present experimental results on the oxidation, volatilization and re-deposition of molybdenum from TZM in flowing air between 400 and 800°C. These results are compared with calculations obtained from a vaporization mass transfer model using chemical thermodynamic data for vapor pressures of $MoO_3(g)$ over pure solid MoO_3 and an expression for the vapor pressures of MoO₂(OH)₂ from the literature. Calculations correlate well with experimental data. The volatilization process is dominated by MoO₃ above 550°C and by MoO₂(OH)₂, formed from the small ingress of water vapor, at temperatures below 550°C. Partial saturation of gaseous species of (MoO₃) near specimen surfaces accounts for observed reductions in volatilization rates at lower flow rates at 700°C. We have thus demonstrated predictive capabilities of the model to account for volatilization as influenced by temperature, humidity (vapor content), and flow rate.

We obtained oxidation rates (mm/h) as indicated by the recession into the base metal. These rates which accounted for the concurrent processes of oxidation and volatilization showed trends similar to other refractory metals, namely, niobium and tantalum.

Deposition of MoO_3 downstream at lower temperatures was calculated with a model using saturation ratios of $(MoO_3)_m$ within segmented regions. Calculated locations of peak distributions and maximums within the temperature gradients generally correlate reasonable well with experimental measurements. Scanning electron microscopy showed that deposits collected in a final filter consisted of small agglomerated particles. We might expect such nucleation, growth and agglomeration of particles to result from the supersaturation of the $(MoO_3)_m$ upon cooling during transport. Hydroxide molecules also decompose back into $MoO_3(s)$ and water vapor at low temperatures. These latter two processes and increased surface areas due to extensive crystal growth from $(MoO_3)_m$ are plausible explanations for differences in peak height and distribution predictions between the model and experiments.

The oxidation-driven mobilization data, along with activation calculations determining radioactive isotope inventories, were used to determine airborne dose rates. These calculations showed that site boundary doses from TZM alloy would be one to two orders of magnitude lower than tungsten at comparable temperatures.

SUMMARY

In this report we present the results of experimental and modeling approaches used to define the oxidation, oxidation-driven vaporization, and re-condensation behavior of TZM alloy tested in air environments between 400 and 800°C. Experimental procedures are presented in Section 2. This section describes the test system used to expose specimens at various temperatures and flow rates in an air environment. Included are descriptions of the system and procedures used to collect, quantify, and examine the volatilized and re-deposited oxide products.

Experimental results are presented in Section 3. This includes the integration of mass change and inductively coupled plasma-atomic emission spectroscopy (ICP-AES) results to account for the concurrent processes of oxygen pick-up and oxide volatilization. These integrations provide oxidation rates (mm/h), the relative amount of the oxide that is volatilized, and the mobilization rate of molybdenum (g/m^2 -h). Features of the oxidized specimens based on physical appearance, optical metallography, scanning electron microcopy (SEM), and x-ray diffraction (XRD) are given in Section 3.2. Illustrations of re-deposited oxides are shown in Section 3.3. Detailed descriptions of deposited oxide products on various system components, the chemical analyses procedures, and ICP-AES results providing mass flux calculations and distribution information are given in Appendices A, B, and C, respectively.

Experimental results are discussed in Section 4. Oxidation rates, mechanisms and the relative amount volatized at various temperatures are compared to the available information in the literature in Sections 4.1 and 4.2. A description of our vaporization mass transfer model including the procedure to handle partial saturation of volatilizing oxide species near specimen surfaces is given in Section 4.3. The treatment for partial saturation helped to explain flow rates In this section we also present equilibrium vapor pressures for both volatilizing effects. polymers of (MoO₃)_m and MoO₂(OH)₂ as a function of temperature and various water vapor concentrations. The combined results from these two species, with MoO₂(OH)₂ dominating at low temperatures and (MoO₃)_m dominating at high temperatures, provide a very good correlation with experimental measurements. Our model predicting the re-deposition from $(MoO_3)_m$ vapors is described and compared with experimental molybdenum profiles in Section 4.4. The model provides good correlation with the locations of peak deposition for tests performed at and above 600°C. Plausible reasons for differences between predicted and measured peak heights and subsequent deposition profiles include: 1) nucleation, growth, agglomeration, and transport of particles due to supersaturation of $(MoO_3)_m$ upon cooling, 2) extra surface areas for re-deposition resulting from crystal development, 3) the role of $MoO_2(OH)_2$ in the mobilization process at lower temperatures. A comparative study showing mobility-based doses derived for TZM alloy and tungsten is given in Section 4.5. This comparison shows that doses from the activated products of TZM alloy are one to two orders lower than tungsten for similar accident conditions of a conceptual fusion device.

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CONTENTS

ABSTRACT	ii
SUMMARY	iii
ACKNOWLEDGMENTS	iv
1.0 INTRODUCTION	1
2.0 EXPERIMENTAL PROCEDURES	1
3.0 EXPERIMENTAL RESULTS	3
 3.1 Oxidation and Mobilization Rates	3 5 6
3.2.3 Phase and Chemistry Determinations 3.3 Features of Re-deposited Oxide	11 12
4.0 DISCUSSION	14
 4.1 Oxidation Rate of TZM Alloy 4.2 Volatilization Process from Oxidized TZM Alloy 4.3 Model of Volatilization Rates 4.4 Model Re-deposition of Mobilized Molybdenum 4.5 Mobility-Based Dose Derived from Oxidation Driven Volatility 	14 14 16 19 26
5.0 CONCLUSIONS	30
REFERENCES	31
Appendix A: Descriptions of Molybdenum Oxide Products Deposited in Quartz Test Components	.A-1
Appendix B: Procedures for Cleaning the Molybdenum-Bearing Test Components and Processing the Solutions for ICP-AES Analyses	. B- 1
Appendix C: ICP-AES Analyses, Mass Flux Calculations, Molybdenum Distributions, and Temperature Profiles	.C-1

1.0 INTRODUCTION

The potential of high temperature strength has motivated much interest in the oxidation behavior of refractory metals. Many of these studies have been oriented toward extremely high temperatures, e.g., up to 1700°C, often under vacuum or environments with low oxygen activities [1,2,3,4]. Studies [1,5,6] on molybdenum at lower temperatures in high levels of oxygen report: 1) parabolic rate law at 250 to 450°C, 2) linear behavior above 400°C, 3) a role of MoO₂ and other oxides (MoO₂), where 2 < Z < 3, between 450 to 650°C. At temperatures above 650°C, oxidation rates are largely influenced by the high rates of the vaporization of the various polymers of MoO₃. Water vapor will also react with MoO₃(s) to form a volatile hydroxide. Vapor pressures of this MoO₂(OH)₂ species have been documented by Speiser and St. Pierre [6]. We performed this study to explore conditions more typical to future fusion devices and to demonstrate predictive capabilities of a vaporization mass transport model. The model had provided excellent mass transport predications for the highly volatile species produced in the tungsten-steam system.[7]

2.0 EXPERIMENTAL PROCEDURES

We tested specimens of TZM alloy between 400 and 800°C in air flowing at a rate of 1000 sccm. Flow rates were varied from 10 sccm to 2500 sccm for tests at 700°C. Gas velocities for these flow rates at 700°C, the pressure at the INEEL, and the test chamber cross section ranged from 0.033 to 8.3 meters per minute. The specimens were prepared from a 22-mm diameter bar made by vacuum arc casting and then hot extrusion. The composition was Mo – 99.25 wt%, Ti - 0.50 wt%, Zr - 0.102 wt%, C - 0.018 wt%, Si – 0.0034 wt%, Fe – 0.001 wt%, Ni - 0.001 wt%, O - 0.0009 wt%, and N – 0.0005 wt%. Disc-shaped specimens of either 1.75- or 3.5-mm thickness were sectioned from the bar. Surfaces were polished to a 600-grit finish.

The specimens were tested in a dual furnace arrangement as shown in Figure 1. The test system consisted of three regions, the reaction furnace, a transition zone, and a furnace in which deposition occurred. The dimensions of the quartz components in the system were as follows: reaction chamber (4.0 cm I.D. x 36 cm long), the transition zone (1.5 cm I.D. x 13 cm long), and the deposition tube (1.5 cm I.D. x 90cm long). Air from a compressed cylinder flowed through a column of Drierite and was preheated to 400°C before passage into the reaction furnace containing the specimen. Upon exiting the reaction furnace the gas stream then passed through a transition zone and a three-zone furnace with a prescribed temperature gradient. Oxidation products transported from the specimen were re-deposited in these components downstream at temperatures between 800 and 25°C. The quartz collection tube in the three-zone furnace was lined with sections of 1-in., or 3-in., long quartz tube. These were used to determine the distribution to the re-deposited molybdenum oxide products along the temperature gradient. A final filter of quartz wool was used to ensure the complete capture of products at the end of the collection tube.





Specimens were weighed before and after testing to obtain mass change. The quartz components were visually inspected following the tests. Descriptions of the oxide products deposited on the components are given in Appendix A. The quartz components were then separately processed as described by the procedures in Appendix B. This involved cleaning the components with 2.9 molar $NH_4(OH)$ solution to remove the molybdenum oxide products. The solutions were heated to drive off NH_3 and then acidified with nitric acid and diluted to 100 ml or 250 ml samples. The diluted solutions were analyzed by inductively coupled plasma-atomic emission spectroscopy (ICP-AES). We examined oxidized specimens with optical metallography, scanning electron microcopy (SEM), and x-ray diffraction (XRD).

3.0 EXPERMENTAL RESULTS

3.1 OXIDATION AND MOBILIZATION RATES. The test matrix with temperatures, times, and flow rates, along with mass changes and total amounts of molybdenum transported as measured by ICP-AES are given in Table 1. Oxidation rates and molybdenum mass flux rates can be obtained from the data in Table 1. However, mass changes need to be corrected to allow for concurrent oxygen pick-up and losses by molybdenum oxide volatilization. For these calculations we assume that the oxidation process essentially produces molybdenum trioxide by the reaction: $Mo + (3/2) O_2 \rightarrow MoO_3$. The total mass of molybdenum (M_t^{Mo}) reacted can then be determined by the relationship expressed in Eq.(1):

$$(M_t^{Mo}) = (M_V^{Mo}) + (96/48)[\Delta m + (M_V^{Mo})],$$
(1)

where Δm is the mass change and $(M_V{}^{Mo})$ is the amount of volatilized molybdenum as measured by ICP-AES. The results of these calculations are given in Table 2. We used these values to determined recession rates (mm/h) and the fraction of oxidized molybdenum that volatilized. Recession considered as the depth of alloy converted to oxide was calculated using 10.2 g/cm^3 as the density of molybdenum and initial surface area. We used metallography to measure recession rates (mm/h) for a limited number of specimens. Average mass flux values were obtained from the sum of the ICP-AES measurements for all system components for a given test, the initial surface area of the specimen, and the test duration. The detailed calculations from the ICP-AES measurements are reported in Appendix C. The calculations in Appendix C show the average mass flux from the specimen, molybdenum distributions, and temperature profiles. Essentially there was no indications of molybdenum mobilization at 400°C. We use a flux value, which we refer to as the Engineering Maximum Flux Value (EMFV), at this temperature. It is determined from the ICP-EAS detection limit from a blank solution. The flux values at 500°C are orders of magnitude higher than the detection limit and more than ten times greater than the uncertainty based on ICP-AES limitations. A summary of the measurements and calculations refer to above are shown in Table 2.

Specimen	Temp.,	Flow rate,	Time,	Initial	Initial	Final	Mass	ICP-AES
_	°C	sccm	h	area,cm ²	weight, g	weight, g	change, g	total, g
TZM14	400	1000	24	10.345	13.6641	13.6684	0.0043	1.5E-6(a)
TZM15	500	1000	24	10.369	13.8827	13.94643	0.06373	1.02E-4
TZM1	500	1000	24	9.101	6.6733	6.7429	0.0696	5.97E-5
TZM16	550	1000	24	10.402	14.0636	14.4353	0.3717	9.04E-4
TZM11	602	1000	8	10.235	13.15934	13.35724	0.19790	3.25E-3
TZM7	599	1000	24	9.136	6.88303	7.65951	0.7765	3.56E-3
TZM8	650	1000	8	9.123	6.8263	7.3607	0.5344	2.51E-2
TZM4	699	10	2	8.994	6.1262	6.1887	0.0625	4.50E-3
TZM17	700	10	8	10.311	13.4955	13.7485	0.2530	1.91E-2
TZM5	699	50	2	9.111	6.7467	6.7988	0.0521	4.55E-3
TZM18	700	50	8	10.326	13.5565	13.7589	0.2024	5.75E-2
TZM10	699	100	2	9.112	6.71857	6.74414	0.02557	3.08E-2
TZM6	700	500	2	9.075	6.4623	6.4560	-0.0063	6.49E-2
TZM12	700	1000	2	10.343	13.67683	13.67773	0.0009	5.43E-2
TZM9	700	2500	2	9.069	6.52977	6.52907	-0.0007	5.67E-2
TZM3	750	1000	1	9.056	6.48254	6.1071	-0.3754	3.46E-1
TZM2	800	1000	1	9.150	6.9709	3.6501	-1.9056	2.22E+0

 Table 1. Test matrix with mass changes and ICP-AES measurements.

(a) The value reported for 400°C is a maximum as established by the detection limit from ICP-AES.

Specimen	Temp	Flow	Time	Total Mo	Calculated	Measured	Fraction of	Measured	Predicted
	°C	rate,	h	reacted,	recession	recession	reacted Mo	mass flux	mass flux
		sccm		g	rate,mm/h	rate,mm/h	volatilized	$g/(m^2-h)$	$g/(m^2-h)$
TZM14	400	1000	24	0.0086	3.40E-5		1.74E-4	6.04E-5(a)	8.22E-5
TZM15	500	1000	24	0.1277	5.03E-4		8.00E-4	4.10E-3	2.97E-3
TZM1	500	1000	24	0.1393	6.25E-4		4.30E-4	2.73E-3	2.97E-3
TZM16	550	1000	24	0.7457	2.93E-3		1.21E-3	3.62E-2	2.28E-2
TZM11	602	1000	8	0.4053	4.85E-3		8.02E-3	3.97E-1	2.97E-1
TZM7	599	1000	24	1.5628	6.99E-3	6.24E-3	2.28E-3	1.62E-1	2.97E-1
TZM8	650	1000	8	1.1434	1.54E-2		2.19E-2	3.43E+0	4.17E+0
TZM4	699	10	2	0.1384	7.55E-3		3.25E-2	2.50E+0	7.06E-5
TZM17	700	10	8	0.5631	6.69E-3		3.40E-2	2.32E+0	7.06E-5
TZM5	699	50	2	0.1178	6.33E-3		3.86E-2	2.50E+0	4.60E-1
TZM18	700	50	8	0.5745	6.85E-3		9.95E-2	6.95E+0	4.60E-1
TZM10	699	100	2	0.1435	7.72E-3	1.12E-2	2.15E-1	1.69E+1	2.81E+0
TZM6	700	500	2	0.1820	9.83E-3		3.57E-1	3.57E+1	2.79E+1
TZM12	700	1000	2	0.1645	7.80E-3		3.30E-1	2.62E+1	4.93E+1
TZM9	700	2500	2	0.1687	9.12E-3		3.36E-1	3.13E+1	8.67E+1
TZM3	750	1000	1	0.2873	3.11E-2	5.46E-2	1.20E+0	3.82E+2	4.75E+2
TZM2	800	1000	1	2.8435	3.05E-1	3.85E-1	7.80E-1	2.42E+3	3.79E+3

(a) The value reported for 400°C is a maximum as established by the detection limit from ICP-AES.

3.2 FEATURES OF OXIDIZED SPECIMENS.

SPECIMEN APPEARANCE. The oxidized specimens of the TZM alloy were 3.2.1 photographed at low magnification. Photographs in Figure 2 show specimens tested at various temperatures. Increasing amounts of residual oxide are apparent with increasing temperatures and times for up to 650°C. Above 700°C the amount of residual oxide is notably less due to oxide evaporation. The samples exposed at 750 and 800°C have only a thin darker oxide layer. The oxide on the specimen exposed at 800°C shows evidence of having been molten. It flowed down the surfaces of the specimen and formed a glob at the bottom. Figure 3 shows photographs of specimens tested at 700°C under various flow conditions. Data in Table 2 show that there were comparable amounts of molybdenum metal oxidized for all flow conditions, however, significantly greater amounts were volatilized with the higher flow rates. This is reflected in the appearance of the specimens in Figure 3. The specimens with the lower flow rates have crystals developed on the surfaces. Volatilizing molybdenum trioxide species apparently were not swept away but instead re-deposited on preferentially oriented seed crystals located on the specimen surfaces. The specimens with higher flow rates had smoother surfaces and evidence of a darker underlying oxide showing that more of the oxide was volatilized and transported from the specimens in agreement with the ICP-AES measurements.



Oxidized Specimens: Air Flow (1 liter/minute)

Figure 2. Specimens of TZM alloy oxidized at various temperatures and times in air.

Effect of Flow Rate on Specimens Oxidized at 700°C 0.05 lpm 0.10 lpm 0.50 lpm



Figure 3. Specimens of TZM alloy tested in air at 700°C with different flow rates.

3.2.2 MICROSTRUCTURAL OBSERVATIONS OF OXIDIZED SPECIMENS. Oxides formed on specimens were examined with the aid of optical metallography (OM), SEM and XRD. Metallographic cross sections showed both thicknesses of residual oxide layers and profiles of oxide formations on the specimens. A specimen exposed for 24 hours at 500°C possessed a 0.02-mm thick oxide layer with some irregularly distributed crystals extending to a height of 0.065 mm. A SEM image of surface oxides formed under such conditions is shown in Figure 4. Thicker oxide scales with multiple layers were apparent for higher temperature tests. A dense oxide layer with intrusions into the metal matrix and cusps-like formations on the outer oxide layer is shown for the 24-hour 600°C test in Figure 5. The outer regions of the oxide also show numerous cracks caused by the growth stresses in the oxide. This suggests that the surface area available for evaporation could be significantly higher than the initial geometric area of the specimen. However, the specimen tested for 8 hours at 600°C not showing such exaggerated oxide growth had a higher mass flux rate (see Table 2). This indicates that instead of the cracks within the oxide contributing to mobilization, the cusp-like formation may influence the flow pattern and reduce volatilization. The inner oxide layer and the extent of external oxide crystal growth depended upon the flow rate for 700°C tests. Figure 6 shows that the oxides existed primarily as externally protruding crystals on the specimens with a flow rate of 10 sccm. The specimen with a flow rate of 100 sccm had a more continuous 0.06-mm thick layer but still some external crystal growth (see Figure 7). Figure 8 shows only a 0.04-mm thick oxide layer with no evidence of external crystal growth for the specimen tested with a flow rate of 1000 sccm. This

correlates with the higher mass flux shown for TZM12 in Table 2. The thickness of the residual oxide layer was significantly less for tests at 700°C and higher. OM and SEM in Figure 9 show that the oxide layer for the 750°C is about 0.013-mm thick. OM provides evidence of crystal structure in the oxide layer while SEM provides better resolution of the porosity and layers within the oxide. A cross section of the very thin oxide layer (less than 0.01 mm) and glob-like formation near the bottom of the specimen tested at 800°C is shown in Figure 10. The thin residual oxide layers for the 750°C and 800°C tests agree with information in Table 2 showing that most of the oxide that formed on the specimens evaporated.



Figure 4. Oxides formed on the surface of specimen oxidized at 500°C for 24 hours.



Figure 5. Cross section of specimen oxidized in air 24 hours at 600°C. (a) Cusp-like oxide scale showing numerous cracks from growth stresses. (b) Layer at oxide to metal interface.



Figure 6. Oxide crystals on specimen oxidized at 700°C for two hours with 10 sccm flow.



Figure 7. Oxide formed on specimen oxidized at 700°C for two hours with 100 sccm flow.



Figure 8. Oxide scale formed on specimen at 700°C after two hours with 1000 sccm flow.



Figure 9. Residual oxide scale on specimen oxidized at 750°C for one hour with a flow rate of 1000 sccm. (a) optical micrograph (magnification: 400X). (b) SEM at 1000X.



Figure 10. Thin oxide layer and glob-like formation from molten oxide on specimen oxidized at 800°C for one hour with 1000 sccm flow rate.

3.2.3 PHASE AND CHEMISTRY DETERMINATIONS. Semi-quantitative analyses by energy dispersive x-ray spectroscopy (EDS) were obtained with the SEM from both cross sections and surfaces of oxidized specimens. In nearly all cases, i.e., including analyses near the oxide to metal interface and at outer regions of the oxide the molybdenum to oxygen ratio most closely indicated MoO₂. In addition, many analyses within the base metal indicated high oxygen level, e.g. up to 25 at%. The oxygen content in the base metal does not agree with phase diagram information showing no solubility of oxygen in molybdenum. XRD analyses from the surfaces of specimens tested at 550°C (TZM16) and 600°C (TZM7) indicated only MoO₃ as shown by the spectrum in Figure 11. We could not detect any MoO₂. Its presence, however, as a thin oxide layer at the oxide to metal interface as suggested by some authors cannot be discounted since XRD will not detect minor phases. The confirmation of MoO₃ by XRD and oxygen indications from the base metal causes us to question the validity of the EDS analyses. High molybdenum concentrations produce an excitation peak, which is located very near the oxygen peak. Perhaps the EDS software cannot appropriately handle background subtractions or other analytical corrections associated with the excitation peak.



Figure 11. XRD spectrum from specimen oxidized at 600° C for 24 hours showing only the presence of MoO₃.

3.3 FEATURES OF RE-DEPOSITED OXIDE.

The test components were examined after the test and the type, color and location of re-deposited oxide were recorded. Detailed records for each test are given in Appendix A. Photographs were taken of the collection tube for some of the tests. Some of these tests showed a start, or heavy concentration, of crystal growth at about 12 inches along the collection tube where temperature decreased to around 550 to 600°C. This region corresponded to the highest concentration of re-deposited molybdenum as determined by ICP-AES. Downstream from this region showing distinctive crystal growth there was often another type of deposit having either a smoky or sometime bluish hue. Sometimes a fairly heavy blue deposit collected at the front end of the quartz wool filter. Figure 12 shows the re-deposited oxides and molybdenum distribution for a test run at 700°C for two hours with a flow rate of 500 sccm. The SEM micrograph in Figure 12 shows that the product collected in the quartz wool consists of agglomerations of very small particles. Figure 13 shows an extremely heavy crystalline deposit for the 800°C tests. The deposit bridges and appears to nearly fill the collection tube at this location. Descriptions of deposits, molybdenum deposition profiles, and temperature profiles for all of the other tests are given in Appendices A and C.



Figure 12. Oxide deposition products from specimen tested in air at 700°C for two hours with a flow rate of 500 sccm.



Figure 13. Yellow crystalline deposit and white smoky deposit formed in the collection tube for a test run at 800°C for one hour with a flow rate of 1000 sccm.

4.0 **DISCUSSION**

4.1 OXIDATION RATE OF TZM ALLOY. We have plotted the recession rates, fractions of "reacted" metal volatilized, and mass flux rates from Table 2 with respect to reciprocal temperature. The plot for the recession rates is shown in Figure 14. The plot shows a good correlation between rates obtained by the (Δm + ICP-AES) and metallographic methods. The plot shows a maximum at 650°C (the rate at 650°C is 2 to 3 times higher than at 600 and 700°C), and then sharply increasing rates from 700 to 800°C. This trend in oxidation rate is very similar to those observed for the other refractory metals of niobium[2] and tantalum[3]. The irregularities are attributed to various non-stoichiometric phases other than Nb₂O₅ or Ta₂O₅. Speiser and St. Pierre[6] reported that they sometimes observed a thin MoO₂ layer, or an external MoO₃ layer with a thin sub-layer of MoO₂ or other oxides during the oxidation of molybdenum in air between 450 to 770°C. The other oxides were reported as being non-stoichiometric, i.e., MoOz with "Z" varying between 2 and 3. The similar characteristics of the refractory metals and the observations above suggest the maximum at 650°C in Figure 14 is real and likely caused by different types of oxide. Although we have little data to show kinetic behavior, the two tests at 600°C indicate linear or even slightly accelerating behavior (Table 2).

4.2 VOLATILIZATION PROCESS FROM OXIDIZED TZM ALLOY. The plot of calculated fraction of "oxidized" molybdenum volatilized in Figure 15 show a marked increase above 650°C. Generally 20 to 33 percent of the oxide that formed volatilized at 700°C except for the tests with the lowest flow rates of 10 and 50 sccm. Although all 700°C tests formed similar amounts of oxides (Table 2), only about one-tenth as much of the oxide volatilized at the lower flow rates. Our model subsequently presented shows this is the result of partial saturation of the oxide was volatilized at 750 and 800°C. This corresponds with our metallographic observations of only a thin (3 to 10 μ m) oxide on these specimens. The high rate of volatilization is apparently linked to the increase in oxidation rate for these two temperatures as shown in Figure 14. Our data agree with that of Gulbransen, et al.[1], where all of the oxygen reacted at 800°C in 76 torr oxygen and formed volatile oxides. The specimen tested at 800°C showed evidence of a molten layer. The sides were smooth and parallel indicative of molten oxide flowing down the specimen. A thicker region at the bottom of the specimen contained



Figure 14. Oxidation rates of TZM alloy as shown the rate of metal reacted (mm/h).



Figure 15. The fraction the MoO₃ volatilized plotted with respect to temperature.

some oxides as revealed in the metallographic cross section. This agrees with temperatures reported for the melting points of MoO_3 (795°C) and a MoO_3 - MoO_2 eutectic (778°C)[6]. The higher vapor pressure above the melting point would increase volatilization rates, which in turn would increase oxidation rates by removing the oxide barrier.

Insight into the mechanisms governing oxidation and volatilization processes of molybdenum metal at temperatures from 827 to 1127°C is provided by Olander and Schofill[4]. They believe that very thin coatings of MoO₂ exist even at high temperatures where rapid evaporation occurs by the overall reaction: $Mo(s) + 3/2 O_2(g) = 1/m (MoO_3)_m(g)$. Although the influence of oxygen adsorption on the oxidation behavior of refractory metals has been widely reported,

Olander, et al.[4] relate the dissociative adsorption of oxygen as the controlling mechanism via $O(ads) + MoO_2 \rightarrow MoO_3$ (ads). The available active sites facilitating the the reaction: adsorption of oxygen in turn depend upon the anion vacancy concentration in the n-type semiconductor structure of molybdenum dioxide. The above theory may help explain some of our data at lower temperatures. The volatilization rate for the 24-h test of 0.162 g/(m²-h) was less than the rate of 0.397 g/(m^2 -h) for the 8-h test at 600°C. Perhaps the stoichiometry of the oxide changed as the oxide scale grew with time and influenced the number of active sites. It is also possible that as the oxide thickened the flow pattern around the specimen changed decreasing the volatilization rate.

4.3 MODEL OF VOLATILIZATION RATES. We used a vaporization mass transfer model to predict the mobilization of molybdenum from the specimens tested in air. The model based on the experimental geometry, thermal hydraulic conditions and vapor pressures of the volatile trioxides, (MoO₃)_m, and hydroxide, MoO₂(OH)₂, was used to predict the mobilization mass flux of molybdenum, J, as expressed by Eq.(2).

$$J = k(p^{Mo} - p^{bulk})/RT \qquad (2)$$

where

k = mass transfer coefficient (m/s),

 p^{Mo} = partial pressure of volatile molybdenum species at surface of the specimen, p^{bulk} = partial pressure of volatile molybdenum species in bulk steam flow.

Since the flow in the experiment is laminar, the mass transfer coefficient is given by [8]:

$$k = 1.86[Re Sc(1/d)]^{1/3} D/d$$
 (3)

D is the diffusion coefficient of the volatile molybdenum species in air based on classic Chapman-Eskong theory [8] and Re is the Reynolds number, Sc is the Schmidt number, and 1 and d are the length and diameter of the furnace. Surface to bulk pressures of the volatile molybdenum species are corrected for the partial saturation of the species in the bulk flow by Eq. (4), where Q is the volumetric flow rate of air (m^3/s) .

$$(p^{bulk}/p^{Mo}) = [1 - exp(-hA/Q)]$$
 (4)

The partial pressure of $(MoO_3)_m$ is determined as an effective value for the various polymeric forms of (MoO₃) existing at different temperatures over pure solid or molten MoO₃. Vapor pressures for the various polymer species were obtained from the HSC thermochemical computer code[9]. Correlations [10] for the effective average polymer number (m) in $(MoO_3)_m$ were also determined. The primary species within our temperatures of interest are (MoO₃)₃, (MoO₃)₄, and $(MoO_3)_5$. Average polymer numbers above solid (MoO_3) are given by Eq. (5).

$$m = 6.785 - 0.013193T + 1.432x10^{-5}T^{2} - 4.4235x10^{-9}T^{3}$$
(5)

The total vapor pressures of these average effective polymers over the solid phase up to the melting point as derived from the HSC thermochemical code are shown by Eq. (6).

$$\log_{10} P(\text{Torr}) = 8,599.81/\text{T} - 186.495 + 63.1654 \log_{10} \text{T} - 0.0078447\text{T} - 4,154,834/\text{T}^2$$
(6)

Vapor pressures of the hydroxide formed by the reaction: $MoO_{3(s)} + H_2O_{(g)} = MoO_2(OH)_{2(g)}$, have been experimentally determined by Speiser and St. Pierre.[6] They reported an equilibrium constant, K_m, for the reaction as expressed by K_m = P_{hydroxide}/P_{water}, to be given by Eq. (7).

$$\log K_{\rm m} = -7731/T + 5.45$$
 (for T = 873 to 963 K) (7)

We obtained vapor pressures for the hydroxide species by using the relationship for K_m , the saturation pressure for water vapor in ambient temperature air of 17.55 Torr (2340 Pa), and the relative humidity. We used a parametric analysis to show vapor pressures of the hydroxide species at various relative humidities. The humidity at the INEEL is typically around 40 percent. Although we dried the air prior to introduction into the test system we postulate that there was some backflow and/or leakage of ambient air into the test system. We show comparisons of the vapor pressures of (MoO₃)_m in dry air and MoO₂(OH)_{2(g)} in environments with the various relative humidities, including a postulated test condition with a ten percent ingress, in Figure 16. The plots show that the vapor pressure of (MoO₃)_m in air and MoO₂(OH)_{2(g)} in the postulated experimental condition are about equivalent at 550°C. In higher relative humidities, e.g., 80 to 100 percent, the temperature at which the vapor pressures of the two different species become equivalent would increase to about 650°C.



Figure 16. Vapor pressures of molybdenum trioxide and hydroxide species at various relative humidities and temperatures.

We calculated contributions to the molybdenum mass flux from both the trioxide and hydroxide species using Eq. (2) through Eq. (7). Comparisons of predicted total mass flux of molybdenum with experimental measurements for the various times, temperatures, and flow rates are given in Table 2. The predictions for tests with a flow rate of one liter per minute are plotted along with the experimental data in Figure 17. The calculations show that below 550°C contributions from $MoO_2(OH)_{2(g)}$ dominate the volatilization process, whereas $(MoO_3)_m$ is the major contributor above this temperature. The model incorporating both species agrees quite well with experimentally derived mass flux measurements over the entire temperature range. Simnad and Spilners [5] showed a very similar trend for molybdenum metal oxidized between 500 and 770°C including an inflection in volatilization rate at 600°C. They reported activation energies of 53.0 kcal/mole and 89.6 kcal/mole below and above 650°C, respectively. We obtained activation energies of 41.4 kcal/mole between 400 and 500°C and 85.3 kcal/mole between 600 and 800°C, respectively. We believe this supports the proposal that the hydroxide and trioxide species, respectively, are the active mechanisms in the two different temperature regions.

The trend of lower mass flux with lower flow rates at 700°C (shown in Table 2) is supported by our predictions using Eq. (3). The measured values, however, are still somewhat higher than predicted values for the lowest flow rates. Protruding crystals were observed growing from specimens tested in the low flow rates as evident in Figure 3 and Figure 6. We would expect environments with higher partial saturation to be more conducive to grow such crystals from preferential sites. Some of these crystals were quite needle, or ribbon-like, and would easily break off. In fact, ribbon and needle-like crystals were observed in the reaction tubes for 700°C tests with 10 and 50 sccm flow rates and molybdenum measurements were higher compared to the other components (see Appendices A and C). This supports the suggestion that the high measurements for mobilized material compared to predicted values result from spalled crystals.



Figure 17. Mass flux of molybdenum showing experimental and predictions from the $(MoO_3)_m$ and $MoO_2(OH)_{2(g)}$ vapor species at various temperatures.

4.4 MODEL FOR RE-DEPOSITION OF MOBILIZED MOLYBDENUM.

In this section, we present a simple condensation model that predicts the condensation profiles in the downstream components in the experiments. The $(MoO_3)_m$ vapors are assumed to be the primary species vaporized from the sample particularly at 600°C and higher as shown by the preceding section. For a given flow rate in the experiment, a concentration of $(MoO_3)_m$ in the gas phase is established by Eq. (8):

$$C_{gas} = (\Gamma^* A)/Q \tag{8}$$

where,

 $\begin{array}{ll} C_{gas} &= \mbox{concentration of } (MoO_3)_m \mbox{ in gas } (kg/m^3), \\ \Gamma &= \mbox{measured mass flux from surface } (kg/m^2-s), \\ A &= \mbox{initial surface area of sample } (m^2), \mbox{ and } \\ Q &= \mbox{volumetric flow rate of air } (m^3/s). \end{array}$

As a packet of gas travels down the tube, it cools and the $(MoO_3)_m$ becomes supersaturated. The saturation ratio expressed by Eq. (9) is that defined by Friedlander[11]:

$$S = C_{gas}(R^*T)/(p_{sat}(T)^*MW)$$
(9)

where,

The vapor pressure of (MoO₃)_m was obtained from the HSC thermochemical computer code[9].

Condensation to the wall will occur when the concentration in the gas exceeds the equilibrium vapor concentration at the given temperature. The rate of condensation given by Eq. (10) in that presented in Ref. [8]:

$$J_{\text{cond}} = k \left(C_{\text{gas}} - C_{\text{equ}} \right)$$
(10)

where,

 $\begin{array}{ll} J_{cond} &= \text{condensation mass flux (kg/m^2-s),} \\ k &= \text{mass transfer coefficient (m/s), and} \\ C_{equ} &= \text{equilibrium vapor concentration (kg/m^3).} \end{array}$

Using the ideal gas law to relate the equilibrium vapor concentration to the vapor pressure and the definition of supersaturation ratio, this relationship can be written as Eq. (11).

$$J_{cond} = k A_s MW p_{sat}(T) (S-1) / (R*T)$$
 (11)

The mass transfer coefficient expressed as k in Eq. (12) is given by Bird[8]:

k =
$$1.86 * (D/d) * [\text{Re *Sc } (L/d)]^{0.333}$$
 (12)

where

Re = Reynolds number of the flow,

Sc = Schmidt number,

 $D = diffusion \text{ coefficient of } (MoO_3)_m$ in air given by the Chapman-Eskong theory which is also presented in Bird[8],

- d = diameter of tube, and
- L = length of tube from sample to location of interest along the tube.

Thus, the mass balance equations that describe the mass of $(MoO_3)_m$ condensed and in the vapor phase are:

$$dC_{gas}/dt = -J_{cond} * A_{wall}/V$$
 (13)

$$dC_{cond}/dt = J_{cond} * A_{wall}/V$$
 (14)

where

 A_{wall}/V = surface to volume ratio of pipe equals (4/d).

Converting the concentration in the gas to supersaturation yields Eq. (15)

$$dS/dt = (kA_{wall}/V)^*(S-1)$$
(15)

Integration yields Eq. (16):

$$S(t) = 1 - (S_o - 1)exp(-kA_{wall}*t/V) = 1 - (S_o - 1)exp(-4kt/d),$$
 (16)

where S_o is the initial supersaturation at the start of the collection tube. The collection tube is then discretized into an equal number of uniform cells (usually 100 over the length of the collection tube each 1 cm each). In this case S_o is the initial supersaturation as the packet of gas enters the cell and S(t) is set to the final value as it exits the 1-cm long cell. This final value is given by Eq. (17):

$$S_{\text{final}} = 1 - (S_0 - 1) \exp(-4k\Delta t/d) = 1 - (S_0 - 1) \exp(-4kV_i/Q^*d),$$
(17)

where

Δt	= time for the packet to transit the cell,
V_i	= volume of segment i, and
Q	= volumetric flow rate.

And the mass condensed in a given cell is given by Eq. (18):

$$[S_{\text{final}} S_o] * p_{\text{sat}}(T) * MW / [R*T]$$
(18)

The final supersaturation exiting a cell is the initial supersaturation entering the next cell in the collection tube. Temperatures in the tube for each test were linearly fit (piecewise into two or three pieces in some cases to get the best fit) and then the linear fit was used in the calculations. The $(MoO_3)_m$ deposition was converted to molybdenum by multiplying by the ratio of the molecular weights. The measured and calculated depositions were converted to deposition per unit length given the limited number of measurements and the large variation in the calculated deposition along the tube.

The results for various cases of temperatures, flow rates and times as listed in Table 3 are shown in Figures 18(a) through Figure 18(h).

Case Number	Temperature (°C)	Flow rate of Air (slpm)	Duration (hr)
1	800	1	1
2	700	0.5	2
3	700	2.5	2
4	700	1	2
5	650	1	8
6	600	1	8
7	600	1	24
8	500	1	24

 Table 3. Cases calculated by deposition model.

The results show that the start of condensation is very well predicted with the model for all the cases. The peak deposition is well predicted in the majority of cases (e.g., Cases 2, 3, 5 and 7) and in the worst cases overpredicts the peak deposition by between 50 and 100%. The deposit model predicts a broad tail of deposition beyond the peak deposition location. This broad tail in most cases overpredicts the observed deposition in the tube. Deviations in the peak heights and the broad tail distribution can be explained by deposition occurring at preferential macroscopic sites provided by growing crystals. For example, this is most apparent for the 800°C test that had crystals bridging the I.D. and nearly plug the tube. Deposition on these crystals would substantially deplete the (MoO₃)_m concentration causing lower than predicted deposition in downstream locations. The experimental data also showed significant molybdenum deposition near the end of the tube and in the glass wool. This deposition was bluish colored and SEM showed that the deposition in the quartz wool consisted of agglomerated small particles. We might expect particle nucleation and transport upon cooling the supersaturated gas. Such aerosol formation was not considered in the model. Had nucleation been incorporated into the model, some of the condensation would have occurred onto those nucleated particles decreasing the

calculated condensation onto the tube in regions where supersaturation is high enough to support both nucleation and condensation onto both particle and walls. The role of $MoO_2(OH)_{2(g)}$ was also not considered. Decomposition of this vapor at lower temperatures may have produced the oxide with the bluish color. This latter mechanism also provides an explanation for the large discrepancy for the 500°C test, i.e., Case 8. Most of the molybdenum is shown to be volatilized as $MoO_2(OH)_{2(g)}$ in Section 3.3 rather than $(MoO_3)_m$. Analyses from the ICP-AES showed that most of the re-deposited oxide was in the reaction chamber as reported in Appendix C. In conclusion, given the simplicity of the model, it does a reasonable job at broadly describing deposition behavior at 600°C and higher where volatilization is dominated by $(MoO_3)_m$.



Figure 18(a). Case 1—Test at 800°C with one liter per minute flow rate for one hour.



Figure 18(b). Case 2 – Test at 700°C with 0.5 liter per minute flow for two hours.



Figure 18(c). Case 3 – Test at 700°C with 2.5 liter per minute flow for two hours.



Figure 18(d). Case 4 – Test at 700°C with one liter per minute flow for two hours.



Figure 18(e). Case 5 – Test at 650°C with one liter per minute flow rate for 8 hours.



Figure 18(f). Case 6 – Test at 600°C with one liter per minute flow for 8 hours.



Figure 18(g). Case 7 – Test at 600°C with one liter per minute flow rate for 24 hours.



Figure 18(h). Case 8 – Test at 500°C with one liter per minute flow rate for 24 hours.

4.5 MOBILITY-BASED DOSE DERIVED FROM OXIDATION DRIVEN VOLATILITY

We can use the oxidation-driven mobilization data to calculate a mobility-based dose. This dose can be used as a metric to compare with other fusion materials or with appropriate confinement factors used in a safety analysis of a conceptual fusion design.

The fractional rate of mobilization of a particular element in an alloy at a given temperature is calculated using the Eq. (19):¹²

$$\dot{MF} = \frac{\Gamma}{WP \times \rho \times \delta} \tag{19}$$

where \dot{MF} is the mobilization fraction per unit time, Γ is the cumulative mass flux of the element (kg/m²-s) based on the test data, WP is the weight fraction of the element in the material, ρ is the density of the material (kg/m³), and δ is the thickness of the component (m) that is being analyzed.

The oxidation-driven mobility-based dose rate is then given by the following equation:

$$DoseRate = [RI \times DI] \times MF \times A_{FW} \times \rho \times \delta$$
(20)

where,

RI = radioactive inventory of isotope per unit mass of material (Bq/kg) in the component, DI = dose impact of isotope (Sv/Bq), A_{FW} = surface area of first wall (m²).

The inner summation is over all isotopes produced and the outer summation is over all of the elements in the alloy.

Thus, the dose rate is simply given by:

$$DoseRate = \frac{[RI \times DI] \times \Gamma \times A_{_{FW}}}{WP}$$
(21)

For the TZM alloy, an activation calculation for the first wall based on the EVOLVE design assuming TZM as the first wall structural material was used.¹³ The dose impact of each isotope was calculated for both ground level and elevated releases using conservative meteorology (class F and 1 m/s wind speed as needed in a traditional "design basis" safety analysis), and using best estimate meteorology (class D and 4 m/s wind speed as needed in a no-evacuation assessment).¹⁴ A one-kilometer site boundary and the regulatory-accepted Pasquill-Gifford dispersion set were used in the evaluation. All results are early doses (7-day exposure) to the maximum exposed individual (at the site boundary for the ground level cases and where the plume touches the ground for the elevated releases). These data are reproduced in Table 4.

Isotope	Radioactive	Dose Impact	Dose Impact	Dose Impact	
	Inventory	D and 4 m/s	D and 4 m/s	F and 1 m/s Ground	
	(Ci/g)	Ground level	Elevated	level	
		(Sv/TBq)	(Sv/TBq)	(Sv/TBq)	
Mo 93	2.60E-03	4.10E-05	3.72E-06	4.26E-04	
Mo 93m	1.35E-02	5.43E-07	4.89E-08	5.53E-06	
Mo 99	2.13E-01	6.98E-06	6.38E-07	7.23E-05	
Mo101	1.83E-01	5.45E-08	7.01E-09	2.69E-07	
Tc 98	1.81E-07	4.66E-05	4.27E-06	4.83E-04	
Tc 99	4.88E-05	8.01E-06	7.28E-07	8.34E-05	
Tc 99m	2.80E+00	1.81E-07	1.97E-08	1.73E-06	
Tc101	1.83E-01	7.01E-09	8.44E-10	3.20E-08	
All Mo isotope contribution to		5.97E-08	5.46E-09	6.16E-07	
dose $(Sv/g)^*$					
All Tc isotope contribution to		1.88E-08	2.05E-09	1.79E-07	
dose $(Sv/g)^*$					

Table 4. Radioactive inventory and Dose Impact of Mo and Tc Isotopes.

* Calculated by summing the product of the radioactive inventory of an isotope and its dose impact.

The mobility-based dose rate for Mo from the TZM alloy is based on the cumulative maximum¹ method from data presented in Table 2 in Section 3.1. Mobilization of the Tc isotopes produced by activation of the Mo is assumed to follow that of the Mo at all temperatures because of the very high vapor pressure of the technetium oxides.¹⁵ The other elements in the TZM alloy did not mobilize in the experiments because of their extremely low volatility and are not included in the evaluation. The results, based on a 500 m² first wall with no radiological confinement, are shown in Table 5. They are compared graphically to the mobilization from tungsten alloy for two of the dose cases studied in Figures 19 and 20.

	Oxidation-driven Mobilization-based Dose Rate					
	D&4 m/s	D&4 m/s	F&1 m/s			
	Ground	Elevated	Ground			
Temperature (°C)	(Sv/hr)	(Sv/hr)	(Sv/hr)			
400	2.37E-09	2.27E-10	2.40E-08			
500	1.61E-07	1.54E-08	1.63E-06			
600	1.57E-05	1.50E-06	1.59E-04			
650	1.35E-04	1.29E-05	1.36E-03			
700	1.40E-03	1.34E-04	1.42E-02			
750	1.50E-02	1.43E-03	1.52E-01			
800	9.51E-02	9.10E-03	9.64E-01			

Table 5. Oxidation-driven Mobilization-base Dose Rates as a Function of Temperature Under Different Exposure Conditions.

The results show that the mobilization dose for TZM alloy is about two orders of magnitude lower than that for tungsten below about 600°C, and decreases to about one order of magnitude up to 800°C. Above 800°C, the Mo in the TZM that converts to molybdenum trioxide melts making measurements very difficult. The results can also be used to determine the degree of radiological confinement needed in accidents involving oxidation driven mobilization of material from the first wall. In a decay heat transient involving air ingress that reaches 750°C for five days, the oxidation driven mobilization dose would be approximately 2 Sv (see Figure 20). Thus, to meet a 10 mSv no-evacuation dose would require the radiological confinement to reduce this source term by about a factor of 200. After five days at 750°C, approximately 70 percent of the affected first wall area would have been mobilized. Transients that result in shorter times at lower temperatures would require less radiological confinement to meet the no-evacuation goal. If temperatures always remained below 500°C in a transient then this would not be a significant contribution to the off-site radiological source term in an accident.

¹ The concept of cumulative maximum is a conservative formulation used for safety assessments. The cumulative maximum mobility at temperature X is the maximum mobility measured at all temperatures up to and including X. Thus, if the maximum mobility measured at 600° C is higher than the value measured at 700° C, the value from the 600° C test is used in place of the value at 700° C.



Figure 19. Oxidation driven mobilization doses for W and Mo in air. The design basis for release are 500 m^2 surface area with no confinement.



Figure 20. Oxidation driven mobilization doses for W and Mo in air. Releases are for 500 m^2 surface area with no confinement and class D and 4 m/s wind speed for no-evacuation criteria.

5. CONCLUSIONS

We have observed good correlation between experimental volatilization rates and those predicted by our mass transport model. The volatilization process occurs by two different mechanisms at low and high temperatures. At low temperatures, e.g., below 550°C volatilization is dominated by $MoO_2(OH)_{2(g)}$ formed from even small concentrations of water vapor. Above this temperature volatilization occurs predominately by the volatile (MoO₃) polymeric species. Our model accounted for both of these mechanisms in the two different temperature regions. It can therefore be used to accurately predict molybdenum mobilization for different climatic conditions, or ambient and humidity conditions of the air, involved in the ingress accident. The model also proved capable of accounting for flow rates which affected near-surface partial saturation of the volatilizing species and reduced mobilization.

The oxidation rate (mm/h) as indicated by recession, i.e., the amount of metal reacted, shows an increasing trend to 650°C, then a slight decrease, and then sharply higher rates due to high volatilization. This trend with a maximum near 650°C simulates that observed with other refractory metals and has been associated with different oxide types. The higher oxidation rates at higher temperature, e.g., 700 to 800°C are due to the very high volatilization rates of the molybdenum trioxide.

Our model for the re-deposition of volatilized molybdenum species of (MoO_3) accurately predicted the downstream peak-deposition locations. The model provided best results for the higher temperatures where volatilization by the various polymeric forms of (MoO_3) is dominant. Differences between predicted and experimental peak heights and subsequent deposition profiles resulted when extensive crystal growth at the peak-deposition locations provided greatly increased surface area for re-deposition to occur.

Mobility-based dose calculations derived from oxidation-driven mobilization data showed TZM alloy to have lower radiological dose impact than tungsten at comparable temperatures and conditions. Dose levels from TZM alloy were two orders of magnitude lower below 600°C and about one order of magnitude lower at 800°C.
REFERENCES

- 2 J. N., Ong, Jr. and W. M Fassell, Jr., Corrosion, 18, (1962) 382t-389t.
- 3 Kofstad, P., J. Inst. of Metals, 90, (1962) 253-264.
- 4 D.R. Olander and J. L. Schofill, Jr., *Metallurgical* Transactions, <u>1</u> (1970) 2775-2784.
- 5 M. Simnad and A. Spilners, J. Metals, 7, (1955) 1011-1016.

6 R. Speiser and G.R. St. Pierre, in *The Science ad Technology of Tungsten, Tantalum, Molybdenum, Niobium and Their Alloys* ed. by N.E.Promisel, Pergamon Press (1964) 289-330.

7 D. A. Petti, G. R. Smolik, and K. A. McCarthy, Tungsten Mobilization During Steam Between 400 and 1200°C, 20th SOFT, Sept. 9-11,1998, Marseille, France 1483-1486.

8 R. B. Bird, W. E. Steward and E. N. Lightfoot, "Transport Phenomena", John Wiley and Sons (1960).

9 A. Roine, Outokumpu HSC Chemistry for Windows, Version 2.0 (1994)

10 Unpublished work by J.D. Christian at the INEEL.

11 S.K. Friedlander, "Smoke, Dust, and Haze: Fundamentals of Aerosol Behavior", John Wiley and Sons, New York (1977).

12 K. A. McCarthy, G. R. Smolik, and S. L. Harms, "A Summary and Assessment of Oxidation Driven Volatility Experiments at the INEL and Their Application to Fusion Reactor Safety Assessments," EGG-FSP-11193, September 1994

13 Unpublished calculations performed by H. Khater at U-Wisconsin Madison Fusion Institute.

14 M. Abbott letter to D. A. Petti, "Revised Results - MACCS2 Doses for Fusion Isotopes Release to the Atmosphere using P-G Dispersion Parameters," MLA-11-99, April 14, 1999.

15 R. G. Bennett, J. D. Christian, D. A. Petti, W. K. Terry, and S. B. Grover, "A System of Tc-99m Production Based on Distributed Electron Accelerators," *Nuclear Technology*, Vol. 126, No. 1, April 1999.

¹ Gulbranson, et al., J. Electrochemical Soc. 110 (1963) 952-959.

APPENDIX A

DESCRIPTIONS OF MOLYBDENUM OXIDE PRODUCTS DEPOSITED IN QUARTZWARE TEST COMPONENTS

Description of Oxidation Products from TZM <u>14</u>





Deposition chamber



Description of oxidation products Location (inches from left) Temp. (°C)

1. Clear, there is no evidence of any reaction products in collection tube, inserts, or quartz wool filter.

2.

3.

4.

5.

Description of Oxidation Products from TZM 1





1. Nothing apparent in the reaction chamber



Description of Oxidation Products from TZM <u>15</u>





Deposition chamber



Description of oxidation products Location (inches from left) Temp. (°C)

1. Clear, there is no evidence of any reaction products in collection tube, inserts, or quartz wool filter.

2.

- 3.
- 4.

5.

6.

Description of Oxidation Products from TZM <u>16</u>





1. Nothing apparent



5. Clear
6. Very light bluish hue
21 to 22
22 to 31
31 to quartz wool

Description of Oxidation Products from TZM <u>11</u>

```
        Test temperature (°C) __600
        Time (h) __8
        Flow rate (lpm) __1 lpm_

        Specimen mass (g):
        Initial __13.15934
        Final __13.35724
        Mass gain __0.1970_
```



1. Localized white deposit on wall 12-14(This be due to the close positioning of the specimen to the wall of the reaction tube or to a localized cold spot in the wall of the reaction tube.)



8	
2. Light, white deposit	12.5 - 15.5
3. Heavier white, smokey deposit	15.5 - 27.5
4. Clearer region, less deposit	27.5 - 34
5. Blue-grey deposit in front of quartz wool	34 - 35
6. Back of quartz wool is still white	35 - 36

Description of Oxidation Products from TZM <u>7</u>





Deposition chamber



	Description of oxidation products	Location (inches from left)	<u>Temp. (°C)</u>
1.	Clear, nothing present	0 to 10	
2.	Sporadic small crystals with small partic	les 10 to 11	
3.	Smoky deposit, i.e., small particles	11 to 13	
4.	White, to smoky, to light blue deposits	13 to 21.5	
5.	Clear	21.5 to 34	

6. Quartz wool is blue in front and white in back

Description of Oxidation Products from TZM <u>8</u>





Deposition chamber



Description of oxidation products	Location (inches from left)	Temp. (°C)
1. Clear through first three inserts.	0 to 10.25	
2. Small crystals	11 to 12	
3. Heavy, white smoky deposit.	12 to 14.5	
4. Medium white smoky deposit.	14.5 to 16.5	
5. Clearing (no evidence of deposit)	17	

6. Quartz wool is very blue in front, clear (white) in back.

Description of Oxidation Products from TZM _4_

 Test temperature (°C) _____0
 Time (h) _____
 Plow rate (lpm) ____0.010

 Specimen mass (g):
 Initial _____6.1262
 Final _____6.1887
 Mass gain _____0.0625___



Deposition chamber



Description of oxidation products Location (inches from left) Temp. (°C)

1. No apparent deposit in collection tube, inserts, or Q.W. filter.

- 2.
- 3.
- 4.
- 5.
- 6.

Description of Oxidation Products from TZM <u>17</u>

 Test temperature (°C) __700
 Time (h) __8
 Flow rate (lpm) __0.01

 Specimen mass (g):
 Initial __13.4955
 Final __13.7485
 Mass gain __0.2530





- 1. Smoky deposit from 0 to 2.5 in., The cap has some smoky, white deposit.
- 2. Silvery crystals to ribbon-like needles 2.5 to 3.5
- 3. Thinly, distributed, very thin ribbon-like crystals 13.5 to 18.5

The crystals irradiant (showing green, blue, red or transparent depending upon angle of reflection).

Deposition chamber



	Description of oxidation products	Location (inches from left)	Temp. (°C)
1.	Few, thin ribbon-like crystals.	6 to 12	
2.	Medium to small crystals	12 to 13.25	
3.	Light blue to smoky, thin deposit	13.25 to 16	
4.	Regions of light smoky blue deposits	18.5 to 31.	

5. Nothing apparent on the quartz wool

Description of Oxidation Products from TZM <u>5</u>

```
Test temperature (°C) __700 Time (h) _2 Flow rate (lpm) __0.05 lpmSpecimen mass (g): Initial __6.7467 Final __6.7988 Mass gain __0.0521_
```



1. Small silvery needle-like crystals, widely spaced18.5 to 19.52. Very large crystals (1/8 to ½ in. long)19.5 to 20.5

- 3.
- 4.



	Description of oxidation products	Location (inches from left)	<u>Temp. (°C)</u>
1.	Few speck-size crystals, widely spaced.	0 to 1	
2.	Mostly clear	0 to 12	
3.	Small crystals, widely spaced	10.75 to 12.25	
4.	Clusters of very small particles.	11.75 to 12.25	
5.	Particles become smaller and disappear.	12.25 to 13	
6.	Clear thereafter.	13 to 36	

Description of Oxidation Products from TZM <u>18</u>



- 6. Fewer, small crystals on wall27 to 33.5
- 7. Heavy collection of ribbon-like crystals in front 33.5 to 34.5 quartz wool filter
- 8. No indication on any color on quartz wool.

Description of Oxidation Products from TZM <u>10</u>

```
        Test temperature (°C)
        700
        Time (h)
        2
        Flow rate (lpm)
        0.10

        Specimen mass (g):
        Initial
        6.71857
        Final
        6.74414
        Mass gain
        0.02557
```



Deposition chamber



	Description of oxidation products	Location (inches from left)	<u>Temp. (°C)</u>
1. (Clear	0 to 10	
2. \$	Silvery sliver-like crystals	10 to 13.5	
3. 5	Smoky deposit on wall	13.5 to 17	
4. \$	Smaller yellowish needle-like crystals	11 to 13	

5. White smoky deposit: heavy 12.5 to 16, Becomes light to clear at about 16 inches.

6. Large silver crystals at 34 to 36 likely dislodged during transport.

7. None to barely detectable deposit in quartz wool.

Description of Oxidation Products from TZM 6____

Test temperature (°C) __700 _ Time (h) __2 Flow rate (lpm) __0.5Specimen mass (g): Initial __6.4623 __ Final __6.4560 __ Mass loss __0.0063



1. Clear over most of the chamber.

- 2. Silvery crystals on the wall Last 2 inches
- 3. The amount of crystals are less than those observed for the test with 0.05 lpm flow.
- 4.



	Description of oxidation products	Location (inches from left)	<u>Temp. (°C)</u>
1.	Very small crystals on first insert.	2 to 2.5	
2.	Clear	2.5 to 10	
3.	Larger silvery crystals.	10 to 12.5	
4.	White deposit.	12.5 to 17	
5.	Very light blue deposit	17 to 31.5	
6.	Heavier blue deposit	31.5 to 34.5	
7.	Quartz wool is blue in front, white in bac	ck. 34.5 to 36.	

Description of Oxidation Products from TZM <u>12</u>



1. There is only a few small clear crystals at one location likely from when the specimen contacted the surface during removal.



	Description of oxidation products	Location (inches from left)	<u>Temp. (°C)</u>
1.	Formation of clear crystal start	9.75 inches	
2.	Crystal become larger	9.75 to 10.75	
4.	Crystals become smaller	10.75 to 12.25	
5.	White to smoke color deposit	12.25 to 16.25	
6.	Very light haze	16.25 to 23.5	
7.	Clear region	23.5 to 29	
8.	Hazy deposit increases (bluish hue)	29 to 34	
9.	Quartz wool is blue in front, white in ba	10 34 to 36	

Description of Oxidation Products from TZM <u>9</u>







	Description of oxidation products	Location (inches from	<u>left</u>) <u>T</u>	emp. (°C)
1.	Clear, except for a few small needle-like	crystals.	0 to 10.5	
2.	Small crystal, heavier deposition.		10.5 to 11.5	5
3.	White deposit on walls.		11.5 to 17	
4.	Smokey deposit		17 to 33.5	
5.	Blue deposit		33.5 to 34	
6.	Blue deposit in front half, white at end o	f quartz wool.	34 to 36	

Description of Oxidation Products from TZM 3

Test temperature (°C) <u>750</u> Time (h) <u>1</u> Flow rate (lpm) <u>1</u> Specimen mass (g): Initial <u>6.48253</u> Final <u>6.1071</u> Mass loss <u>0.3754</u>



10. Heavy greenish deposit in quartz wool, the end is still white. 34.25 to 36

34.25

9. Greenish smoky deposit becomes heavier.

Description of Oxidation Products from TZM 2

Test temperature (°C) __800 __Time (h) _1 __Flow rate (lpm) _1Specimen mass (g): Initial __6.9709 Final __5.0653 Mass loss __1.9056Final weight includes 3.6498 g from specimen plus 1.4152 from molten oxide.



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-						96	> /11,					

	Description of oxidation products	Location (inches from left)	Temp. (°C)
1.	Clear.		0 to 11
2.	Few, yellow (silver) crystals		11 to 14
3.	Heavy yellow, greenish crystals extend	across I.D.	14 to 16
4.	Heavy white smoky deposit with some	crystals	16 to 20
5.	Deposit becomes yellow (or light green	ish) again with some crystals	20 to 34
6.	Heavy conc. of yellow-greenish crystal	s in front of quartz wool.	34 to 35
7.	Heavy yellow-greenish deposit in front (The back portion to the quartz wool is	of quartz wool. still white.)	35 to 36

APPENDIX B

PROCEDURES FOR CLEANING THE MOLYBDENUM-BEARING TEST COMPONENTS AND PROCESSING THE SOLUTIONS FOR ICP-AES ANALYSES

Processing and Analytical Procedures for Molybdenum –Bearing Glassware. for Molybdenum Oxidation Tests IHRG# IRC-99-740

Scope: This procedure describes chemically removing molybdenum oxidation products from quartz test components. The test components the reaction chamber, collection tube, quartz tube inserts, and quartz wool filters as described in IHRG #IRC-99-740.

The following basic procedures will be used for all components (there will be only minor differences used to handle the various components).

- 1. Wash the component once or twice with 2.9 Molar NH₄OH solution.
- 2. Rinse with nanopure water.

3. Heat solutions in covered Teflon beakers on hot plate to drive off NH_3 . Transfer solution to 100-ml volumetric flask. Add 5 ml of concentrated nitric acid (Normality of 15.8). Dilute to 100 ml with nanopure water. Analyze by ICP-AES.

The reaction chamber and 36-long collection tube will be sealed with Parafilm at on end. The 25 ml of the 2.9 M NH₄OH will then be added and the other end sealed with Parafilm. The component will then be manipulated to wash the inner surfaces. This solution will be transferred to a Teflon beaker and the process repeated with another batch of 2.9 M NH₄OH. The inside surfaces of the component will then be rinsed with nanopure water using a squirt bottle. The rinse water will be drained directly into the Teflon beaker. This rinsing process will be done at least twice. The solution collected in the Teflon beaker will be processes as indicated above.

There are two different sizes of quartz tube inserts: 1-in. long pieces and 3-in. long pieces. Molybdenum oxidation products will be cleaned from these pieces by rinsing them with of 2.9 M NH_4OH solution dispensed from a squirt bottle. Approximately 50 ml will be used to rinse each segment directly into a Teflon beaker. Each segment will then be rinsed with about 30 ml of nanopure water. The solution collected in the Teflon beaker will be processes as indicated above.

The quartz wool filter will be placed in a 50-ml plastic disposable beaker. It will be soaked in 25 ml of the 2.9 M NH₄OH solution overnight. The 25 ml of solution will be transferred to a Teflon beaker. Another 25 ml of 2.9 M NH₄OH solution will be added to the quartz wool for a second soak (approx. 10 minutes). The quartz wool will then be rinse with 2.9 M NH₄OH solution from a squirt bottle followed by a nanopure water rinse. All solutions will have been collected in the Teflon beaker which will be processes as indicated above.

APPENDIX C

ICP-AES ANALYSES, MASS FLUX CALCULATIONS, MOLYBDENUM DISTRIBUTIONS, TEMPERATURE PROFILES

TZM14: Tested at 400°C for 24 hours (1000 sccm flow)

Test TZM14 ICP-AES measurements for 100 ml aloquits, except RXN Tube is 250 ml.								
			Mo 202.0					
Calculated per ED	F SA-17, i.e., 2 s	igma (S.D.) for uncertainities						
and 3 sigma (S.D.)	for detection lim	its.						
For Data analyzed		% SD of Cal. Stds	sigma %	3.300				
on 6-21-99		SD of Blk Std	sigma prime ug/ml	0.005				
TZM14	400C/24h		F1, ug/ml	-0.008				
Tested 6-2-99	air		F2, ug/ml	-0.006				
time	24.000		F3, ug/ml	-0.006				
			F4, ug/ml	-0.008				
			F5, ug/ml	-0.007				
			F6, ug/ml	-0.008				
area,cm2	10.34500		F7, ug/ml	-0.011				
			F8,ug/ml	-0.013				
			F9,ug/ml	-0.013				
			F10,ug/ml	-0.012				
			F11,ug/ml	-0.013				
			QW,ug/ml	-0.010				
Flux set by EMFV.			C.T.,ug/ml	0.000				
			RXN T,ug/ml	-0.001				
			subtotal, ug	-11.750				
			(+/-) ug	0.228				
			Blk sub, ug	-8.400				
"IF" statement com	pares Total		(+/-) ug	3.742				
with 3*SD(ug), and	d all "FX" & "Co	mponent"	Total, ug	-3.350				
measurements with	3*SD(ug/ml).	(+/-) ug of Sum		3.749				
Total is selected if a	any of the							
"FX",QW,CT or R	XN T measureme	ents are	DL (3*SD),ug/ml	0.015				
greater than 3*SD(ug/ml).		DL (3*SD), ug	1.500				
		Detection Limit (EMFV)	g/m2-h	6.04E-05				
		Total correct for DL (IF statement), ug		1.500				
		Calculated from Total	Mass Flux, g/m2-h	-1.35E-04				
		Calc. from 'IF" statement	Mass Flux, g/m2-h	6.04E-05				
			\pm g/m2-h	1.51E-04				
			± %	249.91				

Mo (Oxidation Te	est: TZM15	500C for 24	h at 1 lite	er/min.				
ICP Result	202.0	Volume	Mass Mo						
sample	Mo µg/mL	sample(mL)	ug						
TZM15G1	0.010	100	1.04						
TZM15G2	0.011	100	1.1						
TZM15G3	0.012	100	1.2						
TZM15G4	0.018	100	1.82						
TZM15G5	0.013	100	1.28						
TZM15G6	0.004	100	0.38						
TZM15G7	0.001	100	0.1						
TZM15G8	0.000	100	0						
1ZM15G9	0.004	100	0.35						
TZM15G10	0.003	100	0.25						
TZMISGI	0.003	100	0.34						
TZM15QW	0.013	100	1.25						
TZM15 CI	0.020	250	1.90						
I ZIMI J KA	0.334	230	83.475						
		Total (ng)	94 545						
		Total (mg)	0.00						
	Amount ex	cluding RXN	V and Col tube (9 1 1					
	Amountex			7.11					
			Mass Mo (119)	April 29					
	Position	Mass Mo	w Col tube	Temp.,	Temp.,				
	in.	ug	redistributed	C	x 0.01				
T7M15G1	2	1.04	1.3	101	1 9/	Sr	ecimen (ci	m^2)	
TZMIJOI		1.04	1.5	777	F.00	<u></u>		<u></u>	
TZM15G2	5	1.1	1.3	539	5.39		10.369		
TZM15G3	8	1.2	1.5	508	5.08				
TZM15G4	11	1.82	2.2	456	4.56				
TZM15G5	14	1.28	1.6	349	3.49		2		
TZM15G6	17	17 0.38 0.5 274 2.74 <u>Rate (g/m²-h):</u>							
TZM15G7	20	0.1	0.1	238	2.38		3.8E-03		
TZM15G8	23	0	0.0	211	2.11				
TZM15G9	26	0.35	0.4	187	1.87				
TZM15G10	29	0.25	0.3						
TZM15G11	32	0.34	0.4						
TZM15QW	35	1.25	1.5						
TZM15 CT		1.96							
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\vdash			Distance a	long coll	ection tu	be, in.			. —
1									1

TZM15: Tested at 500°C for 24 hours (1000 sccm flow)

TZM15: Tested at 500°C for 24 hours (1000 sccm flow)

Test TZM15		ICP-AES measurements for 100 ml a	loquits, except RXN T	ube is 250 ml.				
				Mo 202.0				Percent
Calculated per ED	F SA-17, i.e., 2 s	igma (S.D.) for uncertainities					Mass M	o in
and 3 sigma (S.D.)	for detection lim	its.					ug	Componen
For Data analyzed		% SD of Cal. Stds	sigma %	5.100				
on 7-06-99		SD of Blk Std	sigma prime ug/ml	0.004	RXN CHM	BR	83.475	88.81
					CT&INSR	TS	9.27	9.86
TZM15	500C/24h		G1, ug/ml	0.010	QW FL	TR	1.25	1.33
Tested 6-8-99	air		G2, ug/ml	0.011				
time	24.000		G3, ug/ml	0.012	Te	otal	93.995	
			G4, ug/ml	0.018				
			G5, ug/ml	0.013				
			G6, ug/ml	0.004	100			
area,cm2	10.36900		G7, ug/ml	0.001				
			G8,ug/ml	-0.006	90			
			G9,ug/ml	0.004	80	_		
			G10,ug/ml	0.003	70			
			G11,ug/ml	0.003	70			
			QW,ug/ml	0.013	60	-		
Flux set by EMFV.			C.T.,ug/ml	0.020	50			
			RXN T,ug/ml	0.334				
			subtotal, ug	93.995	40	-		
			(+/-) ug	8.524	30	_		
			Blk sub, ug	-8.400				
"IF" statement compares Total			(+/-) ug	2.993	20			
with 3*SD(ug), and all "IS" & "DB"		•	Total, ug	102.395	10	_		
measurements with 3*SD(ug/ml).			(+/-) ug of Sum	9.034	0			
Total is selected if	any of the							
"GX",QW,CT or F	XN T measurem	ents are	DL (3*SD),ug/ml	0.012		\$F	5 5	ج _
greater than 3*SD(ug/ml).			DL (3*SD), ug	1.200	CH		NSK NKY	
-		Detection Limit (EMFV)	g/m2-h	4.82E-05	- the	්ර	e. O.	
		Total correct for DL (IF statement), ug	-	102.395	~ ~	Ũ		
		· · · · · · · · · · · · · · · · · · ·						
		Calculated from Total	Mass Flux, g/m2-h	4.11E-03				
	1	Calc. from 'IF" statement	Mass Flux, g/m2-h	4.11E-03				
			$\pm g/m2-h$	3.63E-04				
			± %	8.82				

TZM1: Tested at 500°C for 24 hours (1000 sccm flow)

Test TZM1	ICP-AES meas	surements for 100 ml aloquits	1) is 250 ml.			
				Mo 202.0		
Calculated per E						
and 3 sigma (S.D						
For Data analyze	d	% SD of Cal. Stds	sigma %	2.600		
on 12-03-99		SD of Blk Std	sigma prime ug/ml	0.007		
TZM1	500C/24h					
Tested 11-15-99	air		I2, ug/ml	0.020		
time	24.000		I3, ug/ml	0.027		
			I4, ug/ml	0.016		
			I5, ug/ml	0.001		
			I6, ug/ml	-0.003		
area,cm2	9.1010		I7, ug/ml	0.007		
			I8,ug/ml	0.003		
			I9,ug/ml	-0.003		
			I10,ug/ml	-0.007		
			I11,ug/ml	-0.004		
			QW,ug/ml	0.022		
Flux set by EMF	V.		(C.T+I1).,ug/ml	0.014		
			RXN T,ug/ml	0.405		
			subtotal, ug	51.900		
			(+/-) ug	2.127		
			Blk sub, ug	-7.800		
"IF" statement co	mpares Total		(+/-) ug	5.048		
with 3*SD(ug), a	nd all "IX" & "C	Component"	Total, ug	59.700		
measurements wi	th 3*SD(ug/ml).		(+/-) ug of Sum	5.477		
Total is selected i	Total is selected if any of the					
"IX",QW,CT or I	DL (3*SD),ug/ml	0.021				
greater than 3*SI	D(ug/ml).		DL (3*SD), ug	2.100		
		Detection Limit (EMFV)	g/m2-h	9.61E-05		
		Total corrected for DL (IF statement), ug		59.700		
		Calculated from Total	Mass Flux, g/m2-h	2.73E-03		
		Calc. from 'IF" statement	Mass Flux, g/m2-h	2.73E-03		
			\pm g/m2-h	2.51E-04		
			± %	9.18		



TZM1: Tested at 500°C for 24 hours (1000 sccm flow)



TZM16: Tested at 550°C for 24 hours (1000 sccm flow)



TZM11: Tested at 600°C for 8 hours (1000 sccm flow)



TZM7: Tested at 600°C for 24 hours (1000 sccm flow)



TZM8: Tested at 650°C for 8 hours (1000 sccm flow)



TZM4: Tested at 700°C for 2 hours (10 sccm flow)



TZM17: Tested at 700°C for 8 hours (10 sccm flow)



TZM5: Tested at 700°C for 2 hours (50 sccm flow)

TZM18: Tested at 700°C for 8 hours (50 sccm flow)

							M M.	Percent
							Mass Mo	In Component
Mo Ovidation Tes	st· TZM18 '	700C for 8 h at	0 05 liter/min				ug	Component
	st. 1210110		0.05 mer/mm.		RXN CHMBR		3001.0	5.22
ICP Results	202.0	Volume	Mass Mo		CT&INSRTS		53302.3	92.78
sample	Mo μg/mL	sample(mL)	ug		QW FLTR		1148.0	2.00
TZM18 H1, ug/ml	0.190	100	19.000		Total		57451.3	
TZM18 H2, ug/ml	3.359	100	335.900					
TZM18 H3, ug/ml	140.600	100	14060.000		100			<u> </u>
TZM18 H4, ug/ml	237.400	100	23740.000					
TZM18 H5, ug/ml	6.535	100	653.500					
TZM18 Ho, ug/ml	0.481	100	48.100		80			
TZM18 H8 ug/ml	0.901	100	154 700					
TZM18 H9 ug/ml	12 830	100	1283.000		/0			
TZM18 H10.ug/ml	38.120	100	3812.000		60			
TZM18 H11,ug/ml	81.680	100	8168.000					
TZM18 QW,ug/ml	11.480	100	1148.000					
TZM18 (C.T.).,ug/ml	9.320	100	932.000		40			
TZM18 RXN T,ug/ml	30.010	100	3001.000					
					30			
		Total (ug)	57451.300		20 -			
		Total (mg)	57.451					
	Amount exclue	ling RXN and	Col tube (ug):	53518.300	10			
	D '4'		Mass Mo (ug)			RXN CHMBR C	C&INSRTS Q	N FLTR
	Position	Mass Mo	w Col tube			-		
	111.	ug	TeuistTibuteu					
T7M19U1	2	10	10 221			Spacimon (am^2)		
TZM18H1	5	335 000	341 750			<u>Specimen (cm)</u>		
TZM18H3	8	14060.000	14304 849			10.320		
TZM18H4	11	23740.000	24153.423					
TZM18H5	14	653.500	664.880					
TZM18H6	17	48 100	48 938			Rate (g/m^2-h) .		
TZM18H7	20	96 100	97 774			6.95E+00		
TZM18H8	23	154.700	157.394			0.002.00		
TZM18H9	26	1283.000	1305.343					
TZM18H10	29	3812.000	3878.384					
TZM18H11	32	8168.000	8310.242					
TZM18QW	35	1148.000	1167.992					
TZM18CT		932.000						
Нĕ								
⊢∣မိဋ 25000 [- Mass		
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Ц ,		40		<u>_</u>		20	25	
Ч°	5	10	15	20	25	30	30	40
			Distance	along collect	ion tube, in.			

Mo Oxidation Test TZM10 ---- 700C for 2 h at 0.1 liter/min. Percent Mass M in ug **Component ICP Results** 202.0 336.1 339.1 Volume Mass Mo RXN CHMBR 6940 22.53 CT&INSRTS Mo µg/m Ti µg/mL 23118 75.04 sample Zr µg/mL sample(mL ug **QW FLTR** 751.2 2.44 TZM 10 E1 1.941 0.001 -0.002 100 194.1 TZM 10 E2 0.424 -0.002 -0.004 100 42.4 Total 30809.2 TZM 10 E3 21.705 0.000 0.016 100 2170.5 TZM 10 E4 139.900 0.012 0.085 100 13990 100 TZM 10 E5 3.068 -0.005 -0.006 100 306.8 16.260 TZM 10 E6 0.000 0.003 100 1626 90 TZM 10 E7 0.001 0.000 100 6.315 631.5 80 TZM 10 E8 14.420 -0.001 0.000 100 1442 70 TZM 10 E9 3.164 0.001 0.002 100 316.4 TZM 10 E10 -0.003 5.311 -0.001 100 531.1 60 TZM 10 E11 9.064 0.012 0.041 100 906.4 50 TZM 10 OW 7.512 0.003 0.003 100 751.2 40 TZM 10 CT 9.608 -0.001 0.004 100 960.75 TZM 10 RXN 0.001 30 27.760 0.017 250 6940 20 Total (ug) 30809 10 Total (mg) 30.8 0 Amount excluding RXN and Col tube 22908.4 RIN CHNER CISINERIS ON FIR Mass Mo (ug) April,28 w Col tube Position Mass Mo Temp. x 10 Temp., redistributed in. С ug TZM 10 E1 2 194.1 202.2 6720 672 Specimen (cm²) Summer'99 Temp. TZM 10 E2 42.4 Temp.(2),C 5 44.2 7060 706 9.112 x 10 2170.5 16 TZM 10 E3 8 2261.5 6790 679 0 659 6590 TZM 10 E4 11 13990 14576.7 5990 599 17 676 6760 TZM 10 E5 14 306.8 319.7 4750 475 18 2 683 6830 17 Rate (g/m²-h): 19 690 TZM 10 E6 1626 1694.2 3850 385 3 6900 TZM 10 E7 20 3270 327 16.91 20 699 6990 631.5 658.0 4 23 282 21 708 TZM 10 E8 1442 1502.5 2820 5 7080 TZM 10 E9 26 316.4 329.7 22 6 707 7070 29 23 7 696 6960 TZM 10 E10 531.1 553.4 TZM 10 E11 32 906.4 944.4 24 8 685 6850 TZM 10 QW 35 751.2 782.7 25 9 671 6710 26 TZM 10 CT 960.75 10 648 6480 27 11 609 6090 16000.0 28 12 563 5630 14000.0 -D-Mass 29 13 518 5180 **Micrograms of Mo** 30 14 476 4760 12000.0 -D-Temp.(1)x10 32 16 415 4150 collected Temp.(2)x10 10000.0 36 20 319 3190 8000.0 40 24 255 2550 ៰៰៰៰៰៰ 6000.0 44 28 220 2200 a 46 30 174 1740 4000.0 48 32 96 960 2000.0 49 33 63 630 7770 0.0 50 34 39 390 0 5 10 15 20 25 35 40 30 51 35 30 300 Distance along collection tube, in. 52 20 36 200

TZM10: Tested at 700°C for 2 hours (100 sccm flow)
]	Mo Oxidatio	n Test TZM6	700C for 2 h	at 0.5 liter/minut	te			Percent	
							Mass Mo	in	
ICP Results	202.0	Volume	Mass Mo				ug	Componen	t
sample	Mo µg/mL	Sample(mL)	ug						
				RXN	CHMBR		12560	19.36	
TZM 6 D1	3.204	100	320.4	СТ	&INSRTS		44242	68.19	
TZM 6 D2	0.460	100	46		QW FLTR		8080	12.45	
TZM 6 D3	0.266	100	26.6						
TZM 6 D4	0.147	100	14.7		Total		64882		
TZM 6 D5	0.120	100	12						_
TZM 6 D6	0.102	100	10.2		100				
TZM 6 D7	0.167	100	16.7		100				
TZM 6 D8	0.425	100	42.5		90				
TZM 6 D9	39.470	100	3947		80				
TZM 6 D10	124.700	100	12470		70				
TZM 6 D11	92.540	100	9254		70				
TZM 6 D12	63.440	100	6344		60				
TZM 6 D13	40.130	100	4013		50				
TZM 6 D14	22.030	100	2203		40				
TZM 6 D16	3.568	100	356.8		40				
TZM 6 D17	2.217	100	221.7		30				
TZM 6 D18	2.251	100	225.1		20				
TZM 6 D19	1.680	100	168		10				
TZM 6 D20	1.423	100	142.3		10				
TZM 6 D21	1.339	100	133.9		0				
TZM 6 D22	1.379	100	137.9			Not al		<i>(</i> ?	
TZM 6 D23	1.428	100	142.8		c)	ANN NSK	NEN	•	
TZM 6 D24	1.183	100	118.3		th .	C. ON	O,		
TZM 6 D25	0.948	100	94.8		~	0			
TZM 6 D26	1.080	100	108						
TZM 6 D27	0.836	100	83.6						
TZM 6 D28	0.888	100	88.8						
TZM 6 D29	1.430	100	143						
TZM 6 D30	2.259	100	225.9						
TZM 6 D31	2.759	100	275.9						
TZM 6 D32	4.910	100	491						
TZM 6 D33	5.436	100	543.6						
TZM 6 QW	80.800	100	8080						
TZM 6 Col Tube	18.205	100	1820.5						
TZM 6 RXN	125.6	100	12560						
		Total (ug)	64882						
		Total (mg)	64.9						
	Amount exc	luding RXN a	nd Col tube (mg)	50502					

TZM6: Tested at 700°C for 2 hours (500 sccm flow)

TZM6: Tested at 700°C for 2 hours (500 sccm flow)

Mass Mo,ug Mass Mo,mg									
	Position	Mass Mo	w Col tube	w Col tube	Temp.,				
	in.	ug	redistributed	redistributed	С				
TZM 6 D1	1.5	320.4	331.9	0.3319					
TZM 6 D2	2.5	46.0	47.7	0.0477		Specimen (cm ²)			
TZM 6 D3	3.5	26.6	27.6	0.0276		9.075			Summer'99
TZM 6 D4	4.5	14.7	15.2	0.0152					
TZM 6 D5	5.5	12.0	12.4	0.0124			16	0	662
TZM 6 D6	6.5	10.2	10.6	0.0106			17	1	676
TZM 6 D7	7.5	16.7	17.3	0.0173		$\underline{\text{Rate } (g/m^2-h):}$	18	2	683
TZM 6 D8	8.5	42.5	44.0	0.0440		35.75	19	3	690
TZM 6 D9	9.5	3947.0	4089.3	4.0893			20	4	697
TZM 6 D10	10.5	12470.0	12919.5	12.9195			21	5	705
TZM 6 D11	11.5	9254.0	9587.6	9.5876			22	6	704
TZM 6 D12	12.5	6344.0	6572.7	6.5727			23	7	693
TZM 6 D13	13.5	4013	4157.7	4.1577			24	8	683
TZM 6 D14	14.5	2203	2282.4	2.2824			20	9	647
TZM 6 D10	15.5	221.7	220.7	0.3097			20	10	609
TZM 6 D17	10.5	221.7	229.7	0.2297			28	11	564
TZM 6 D18	17.5	168	174.1	0.2332			20	12	522
TZM 6 D20	19.5	142.3	147.4	0.1741			30	13	483
TZM 6 D21	20.5	133.9	138.7	0.1387			32	14	418
TZM 6 D22	21.5	137.9	142.9	0.1429			34	18	371
TZM 6 D23	22.5	142.8	147.9	0.1479			36	20	330
TZM 6 D24	23.5	118.3	122.6	0.1226			40	24	265
TZM 6 D25	24.5	94.8	98.2	0.0982			44	28	225
TZM 6 D26	25.5	108	111.9	0.1119			48	32	132
TZM 6 D27	26.5	83.6	86.6	0.0866			49	33	104
TZM 6 D28	27.5	88.8	92.0	0.0920			50	34	76
TZM 6 D29	28.5	143	148.2	0.1482			51	35	60
TZM 6 D30	29.5	225.9	234.0	0.2340			52	36	30
TZM 6 D31	30.5	275.9	285.8	0.2858					
TZM 6 D32	31.5	491	508.7	0.5087					
TZM 6 D33	32.5	543.6	563.2	0.5632					
TZM 6 QW	34	8080	8371.3	8.3713					
TZM 6 Col Tube		1820.5							
L									
Ц 🔁 14000 г							L		
		Я		_					
	-	/ \		-	-D-Mass				
: : 10000	-		Р	_	-D-Temp.>	k10		-	
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H & 6000	-								
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H o	5	10	15	20	25 3	30 35	40		
H			Distance alon	a collection	tube. in.				
Π				J J			H		

	Mo Oxidation Test TZM12 700C for 2 h at 1.0 liters/minute											Percent	
						Mass Mo (mg)		April,28			Mass Mo	in	
ICP Results	202.0	Volume	Mass Mo	Position	Mass Mo	w Col tube	Temp.x10	Temp(1)			ug	Component	
sample	Mo µg/mL	Sample(mL)	ug	in.	ug	redistributed	С	С					
										RXN CHME	R 975.25	1.80	
D1	0.957	100	95.7	1.5	95.7	98.7	6720	672		CT&INSR	S 42197.7	77.77	
D2	0.476	100	47.6	2.5	47.6	49.1	6860	686	-	QW FL1	R 11090	20.44	
D3	0.424	100	42.4	3.5	42.4	43.7	6970	697					
D4	0.415	100	41.5	4.5	41.5	42.8	7060	706	<u>'</u>	To	al 54262.95		
D5	0.270	100	27	5.5	27	27.8	/040	/04	-				
D6	0.255	100	25.5	6.5	25.5	26.3	6920	692	-	#			_
D/	0.422	100	42.2	7.5	42.2	43.3	6620	663					
D0	14.96	100	1496	9.5	1496	1542.9	6380	638		90			
D10	115 000	100	11500	10.5	11500	11860.8	5990	590	,	80			
D11(avg.)	78.590	100	7859	11.5	7859	8105.6	5550	555		70			
D12	60.370	100	6037	12.5	6037	6226.4	5100	510)				
D13	45.970	100	4597	13.5	4597	4741.2	4750	475		60			
D14	34.580	100	3458	14.5	3458	3566.5	4400	440		50 -			
D16	17.760	100	1776	15.5	1776	1831.7	4130	413		1 40 L			
D17	1.435	100	143.5	16.5	143.5	148.0	3850	385					
D18	0.937	100	93.7	17.5	93.7	96.6	3660	366		30			
D19	0.977	100	97.7	18.5	97.7	100.8	3470	347	'	20 -			
D20	1.030	100	103	19.5	103	106.2	3270	327	'	10			
D21	1.108	100	110.8	20.5	110.8	114.3	3080	308					
D22	1.237	100	123.7	21.5	123.7	127.6	2950	295		↓			
D23	1.271	100	127.1	22.5	127.1	131.1	2820	282	_	l .i	st sé		· _
D24	1.184	100	118.4	23.3	118.4	122.1	2690	205		CHI	allysi	CM'Y	-
D23	1.077	100	107.7	24.5	107.7	111.1	2300	230	'	- 2 ⁴ 9	ۍ ۳	0	-
D20	0.981	100	98.1	25.5	98.1	123.9				╢	-		
D28	1.035	100	103.5	27.5	103.5	101.2							Temp.(2)
D29	1.651	100	165.1	28.5	165.1	170.3						Summer'99	x10
D30	2.672	100	267.2	29.5	267.2	275.6					6 0	662	6620
D31	3.994	100	399.4	30.5	399.4	411.9					7 1	676	6760
D32	4.802	100	480.2	31.5	480.2	495.3					8 2	683	6830
D33	8.193	100	819.3	32.5	819.3	845.0					9 3	690	6900
Quartz Wool	110.900	100	11090	34	11090	11437.9				-	20 4	697	6970
ZM12 CT-D	16.210	100	1621								21 5	705	7050
ZM12 RXN	3.901	250	975.25						_	-	6	704	7040
						Specimen (cm ²)			_		23 7	693	6930
		Total (ug)	54263.0			10.343			_		24 8	683	6830
		Total (mg)	54.263							· ·	25 9	609	6690
						Rate (g/m ² -h):					26 10	647	6470
	Amount exc	luding RXN an	a Col tube (u	51666.7		26.23					11	609	6090
								L	+		12	502	5040
\vdash	14000.	0						ר ⊢	+	+		<u> </u>	J220
	12000	n L			-Mass						$\frac{14}{32}$ 16	418	4180
	12000.	0	Я		- Temp.(*	1)x10	7				34 18	371	3710
	10000.	0 -			- Temp (2	, 2)x10					36 20	330	3300
			17		- 10mp.(2	- , , , , , , , , , , , , , , , , , , ,					0 24	265	2650
ž	8000.		· 14								4 28	225	2250
of	6000.	0 F	~~~~~				1			·	18 32	132	1320
su su	4000		00	GO-							19 33	104	1040
	4000.	v⊦		Jugo Co	Son-						50 34	76	760
	2000	0	1	У	0000	\neg					35	60	600
	_000.	-	/	٦			×		-		36	30	300
┝──┤╸	0.	0		000			TO TO	┛┝─	-				
		0	10		20	30		40	-		+		
			Distand	e along	collectio	n tube. in.			+				

TZM12: Tested at 700°C for 2 hours (1000 sccm flow)

Percent Mo Oxidation Test TZM9 ---- 700 for 2 h at 2.5 liters/minute Mass Mo in ug Component 202.0 339.1 336.1 Mass Mo **ICP Results** Volume Mo µg/mL Ti µg/mL Zr µg/mL RXN CHMBR sample sample(mL) 3442.5 6.07 ug CT&INSRTS 44212.8 77.97 TZM 9 H1 15.28 -0.007 0.004 100 1528 **QW FLTR** 9050 15.96 TZM 9 H2 3.031 -0.008 -0.002 100 303.1 56705.3 TZM 9 H3 0.683 -0.004 -0.002 100 68.3 Total TZM 9 H4 141.400 0.001 0.062 100 14140 0.039 100 9278 TZM 9 H5 92.780 0.000 100 0.005 100 1626 TZM 9 H6 16.260 -0.004 TZM 9 H7 5.268 -0.004 -0.001 100 526.8 90 TZM 9 H8 4.558 -0.007 -0.002 100 455.8 80 TZM 9 H9 5.224 -0.006 -0.002 100 522.4 TZM 9 H10 2.233 -0.006 -0.002 100 223.3 70 TZM 9 H11 -0.005 -0.001 100 581.1 5.811 60 90.500 0.001 0.039 100 9050 TZM 9 QW 149.600 100 14960 TZM 9 CT 0.006 0.068 50 -0.002 TZM 9 RXN 13.770 0.005 250 3442.5 40 Total (ug) 56705 30 Total (mg) 56.7 20 Amount excluding RXN and Col tube 38302.8 10 Mass Mo (ug) April,28 0 Position Mass Mo w Col tube Temp. x 10 Temp., PANCHNER CRANSELS ONITIP in. ug redistributed С TZM 9 H1 1528 2124.8 6720 672 TZM 9 H2 421.5 706 5 303.1 7060 TZM 9 H3 8 95.0 6790 68.3 679 Temp.(2) Specimen (cm²) TZM 9 H4 11 14140 19662.7 5990 599 Summer'99 x10 TZM 9 H5 14 9278 12901.7 4750 475 9.069 16 0 652 6520 TZM 9 H6 17 1626 2261.1 3850 385 17 668 6680 TZM 9 H7 20 3270 327 18 675 6750 526.8 732.6 2 TZM 9 H8 23 2820 19 683 6830 455.8 633.8 282 3 TZM 9 H9 26 522.4 726.4 Rate (g/m²-h): 20 4 692 6920 TZM 9 H10 29 31.26 21 5 223.3 310.5 701 7010 TZM 9 H11 32 22 581.1 808.1 6 701 7010 TZM 9 QW 35 9050 12584.7 23 7 692 6920 TZM 9 CT 14960 24 8 682 6820 25 9 667 6670 16000 10 26 641 6410 Micrograms of Mo collected 27 14000 11 601 6010 -D-Mass 28 12 554 5540 12000 29 13 505 5050 Temp.(2)x10 30 14 470 4700 10000 32 16 404 4040 8000 36 20 326 3260 6000 40 24 2500 250 44 28 2220 222 4000 46 30 2070 207 2000 48 32 172 1720 П 49 33 148 1480 0 50 34 990 99 5 0 10 15 20 25 30 35 40 51 35 98 980 Distance along collection tube, in. 52 36 30 300

TZM9: Tested at 700°C for 2 hours (2500 sccm flow)



TZM3: Tested at 750°C for 1 hour (1000 sccm flow)

TZM2: Tested at 800°C for 1 hour (1000 sccm flow)

]	Mo Oxidatio	n Test TZM2	800C for 1 h	at 1.0 liters/mi	inute			Percent			
							Mass Mo	in			
ICP Results	202.0	Volume	Mass Mo				ug	Componen	t		
sample	Mo µg/mL	Sample(mL)	ug					-	-		
				R	XN CHMBR		518000	23.35			
TZM 2 E1	6.67	100	667		CT&INSRTS		1604391	72.32			
TZM 2 E2	53.78	100	5378		QW FLTR		95960	4.33			
TZM 2 E3	121.5	100	12150								
TZM 2 E4	13030	100	1303000		Tota	l	2218351				
TZM 2 E5	433.6	100	43360								
TZM 2 E6	522.4	100	52240								
TZM 2 E7	67.48	100	6748		100						
TZM 2 E8	46.74	100	4674		90						
TZM 2 E9	55.94	100	5594		80	-					
TZM 2 E10	1435	100	143500		70	_					
TZM 2 QW	959.6	100	95960		/0						
TZM 2 Col Tube	270.8	100	27080		60						
TZM 2 RXN	2072	250	518000		50						
					40						
		Total (ug)	2218351		30						
		Total (mg)	2218.4		20						
	Amount exc	luding RXN a	nd Col tube (mg)	1673271	10						
			Mass Mo,ug	Mass Mo,mg							
	Position	Mass Mo	w Col tube	w Col tube		NBP at	, ,	K.			
	in.	ug	redistributed	redistributed		ithe ansi	NºF.				
					at a	ోస	0-				
TZM 2 E1	2	667.0	677.8	0.6778	L `						
TZM 2 E2	5	5378.0	5465.0	5.4650						July,12	Temp.
TZM 2 E3	8	12150.0	12346.6	12.3466		Specimen (cm ²)				Temp.	x2
TZM 2 E4	11	1303000.0	1324087.6	1324.0876		9.15		16	0	777	1554
TZM 2 E5	14	43360.0	44061.7	44.0617				17	1	790	1580
TZM 2 E6	17	52240.0	53085.4	53.0854				18	2	793	1586
TZM 2 E7	20	6748.0	6857.2	6.8572		Rate (g/m ² -h):		19	3	801	1602
TZM 2 E8	23	4674.0	4749.6	4.7496		2424.43		20	4	807	1614
TZM 2 E9	26	5594.0	5684.5	5.6845				21	5	815	1630
TZM 2 E10	29	143500.0	145822.4	145.8224				22	6	811	1622
TZM 2 QW	35	95960.0	97513.0	97.5130				23	7	797	1594
TZM 2 Col Tube		27080.0						24	8	785	1570
					l		L	25	9	770	1540
								26	10	748	1496
9 1600	Lann	00ne						27	11	713	1426
9 1400			h n		-0-	Mass (mg)		28	12	666	1332
						TempCx(2)		29	13	624	1248
0 1200						- F / - (/		30	14	587	1174
≥ 1000 ¥	-	/		<u>م</u>				32	16	522	1044
S 800	F		\	Ъ	n			34	18	466	932
Ë 600	-			· · · · · · · · · · · · · · · · · · ·		<		36	20	417	834
<u>10</u> 400	ŀ		\					40	24	344	688
200	ŀ	/	\		~			44	28	296	592
≥0		╺╾──		<u> </u>		, <u> </u>	[48	32	175	350
	0	5 10) 15	20	25	30 35	40	49	33	130	260
			Dieterre					50	34	90	180
			Distance ald	ong collection	n tupe, in.			51	35	72	144
		I				Ι		52	36	30	60