

ECAR-5067 Computational Evaluation on Effect of Edge-rounding in Circular to Annular Flow Transitions within a Hexagonal Duct

SuJong Yoon

December 2020



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Title: Computational Evaluation on Effect of Edge-rounding in Circular to Annular Flow Transitions within a Hexagonal Duct

ECAR No.: 5067 Rev. No.: 0 Project No.: 32833 Date: TBD

1.	VTR Consequence Level	[VTR CL DESIGNATION; [3]
2.	<p>Objective/Purpose:</p> <p>The pressure loss of the fuel rod bundle is an important parameter that can directly affect the primary pump specification, the flow distribution and the safety behavior of the core. The pressure loss of the fuel rod bundle mainly occurs at the inlet module and the fuel region. There are several empirical correlations for the wire-wrapped fuel region whereas the inlet module still remains to be studied. Since the local pressure loss is dominant in the inlet module, the effect of internal structures in the inlet module on the pressure loss needs to be investigated. For instance, the edge rounding-off of internal geometry could reduce the form loss in the inlet module effectively. The computational fluid dynamics (CFD) analysis of the internal flow with varying cross-section from circle to annulus was carried out focusing on the effect of edge-rounding of the internal structure.</p>	
3.	<p>If revision, please state the reason and list sections and/or pages being affected:</p> <p>Initial Release</p>	
4.	<p>Conclusions/Recommendations (Note: Clearly state any actions or additional reviews that were identified within the body of the report):</p> <p>In this ECAR, the computational fluid dynamics (CFD) simulation of the duct with a cross-section varying from circle to annulus was performed to evaluate the effect of edge-rounding of the internal edges. The edge of circular channel and the edge of inner annular channel were rounded with the radius of curvature ranged from 0 mm to 20 mm. The CFD results show that the pressure loss of the duct can be reduced by increasing the radius of the rounded edge. Case-A results showed that the pressure drop can be significantly reduced by the edge-rounding, e.g., the pressure drop was reduced approximately 56% by the radius of curvature of 5.0mm, and reduced 70% by the radius of curvature of 20.0 mm although its effectiveness would be attenuated as the radius of curvature of edge increases. Results from Case-B showed the impact of rounding the inlet edge was practically negligible compared to the outlet edge. This ECAR could provide a guideline to determine the optimum inlet module design of the VTR fuel rod bundle.</p>	

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ECAR Approvals

Project Role	Name (Printed)	Signature	Date
Performer	S. Yoon, D. Shaver		
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Responsibilities

The program manager has the ultimate responsibility and authority to determine required reviews and approvals in this section and may deviate from the guidance in the Responsibilities section. In most cases the following guidance will be used to determine required reviews and approvals, and scope of the review.

- Required for VTR Consequence Levels 1, 2, and 3: Confirmation of completeness, references used, compliance to engineering inputs, appropriateness of assumptions, mathematical accuracy, correctness of calculated data employing, as appropriate, different or independent analytical methods from the ones used to produce the original engineering deliverable, and validity of conclusions and recommendations. Must not check own work.
- Required for VTR Consequence Levels 1 and 2: Concurrence of method or approach, validity of assumptions, and compliance to input requirements of both performer and checker output. Must not check own work.
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- Required for all VTR consequence levels: Concurrence indicates that competent individuals performed and checked the ECAR and that this ECAR represents the appropriate inputs, methods, and approach, that outputs and recommendations are clear and understandable and represent the appropriate outcome for the program including compliance with design basis. Contributing to ECAR that is reviewed is acceptable.
- Required for all VTR consequence levels: Owner concurrence indicates that the document content is appropriate for program use, that appropriate reviews have been completed; signature accepts the document for program use UNLESS VTR executive director signature is not NA'ed.
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NOTE: VTR Consequence Levels are found in SP-60.2.1.1, "VTR Program Documents," Appendix A.

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SCOPE AND BRIEF DESCRIPTION

The pressure loss of the fuel rod bundle is an important parameter that can directly affects the primary pump specification, the flow distribution and the safety behavior of the core. The pressure loss of the fuel rod bundle mainly occurs at the inlet module and the fuel region. There are several empirical correlations ([1], [2], [3] [4] and [5]) for the wire-wrapped fuel region, but the inlet module still remains to be studied. Since the form loss is dominant in the inlet module, the effect of internal geometries in the inlet module on the pressure loss needs to be investigated. For instance, the edge rounding-off of internal geometry could reduce the form loss in the inlet module effectively. Since the form loss in the inlet module is geometry-dependent and difficult to be evaluated by simple methods using hydraulic (equivalent) diameter, the experiment or computational method is required.

This ECAR aims at evaluating the effect of edge-rounding in the duct with cross-section varying from circle to annulus on the pressure loss to provide a useful guideline for design optimization of the VTR fuel rod bundle.

DESIGN OR TECHNICAL PARAMETER INPUT AND SOURCES

Relevant information is provided throughout the discussion and analysis section of this document.

RESULTS OF LITERATURE SEARCHES AND OTHER BACKGROUND DATA

Ref. [6] provides the formulas for the abrupt expansion and contraction pressure losses derived by processing the experimental results. The total resistance coefficient (ζ) through abrupt expansion

downstream of circular tube with uniform velocity distribution ($\geq 3.3 \times 10^3$) is given as follows:

(1)

(2)

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where λ is the local resistance coefficient, λ is the friction coefficient, λ is the frictional resistance coefficient,

Δp is the pressure drop through the channel (Pa), ρ is the fluid density (kg/m³), n_{ar} is the cross-sectional area ratio ($=F_2/F_0$), w_0 is the upstream velocity (m/s), w_2 is the downstream velocity (m/s), F_0 is the cross-sectional area of upstream channel (m²), F_2 is the cross-sectional area of downstream channel (m²). The local resistance coefficient ζ_{loc} is tabulated in Table 1 [6].

Table 1 Local resistance coefficient through abrupt expansion downstream of circular tube with uniform velocity distribution ($Re_0 \geq 3.3 \times 10^3$)

	0.0	0.1	0.2	0.3	0.4	0.5	0.6	0.7	0.8	1.0
	1.0	0.81	0.64	0.5	0.36	0.25	0.16	0.09	0.04	0

The coefficient of local resistance to an abrupt contraction at large Reynolds number greater than 10^4 can be approximately determined by following formula [6]:

(3)

where F_0 is the downstream cross-sectional area (m²) and F_1 is the upstream cross-sectional area (m²).

Although Ref. [6] provides a vast amount of data for the hydraulic resistances of various geometries, the data for specific geometries of interest in this ECAR are not available. The local resistance of the complex geometry can only be determined by either the experiment or the computational fluid dynamics. In this ECAR, the computational fluid dynamics (CFD) was adopted to determine the pressure loss of interested geometries.

ASSUMPTIONS

1. Three-dimensional, steady-state, isothermal, incompressible and turbulent flow of liquid sodium
2. Constant sodium density, dynamic viscosity were assumed to be 860 kg/m³ and 3.0×10^{-4} Pa·s, respectively.
3. Uniform inlet velocity distribution

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COMPUTER CODE VALIDATION – Star-CCM+

- A. Computer type: INL LEMHI cluster
- B. Operating System and Version: CentOS 7.6 operating system
- C. Computer program name and revision: STARCCM+ 13.06.012-R8
- D. Inputs (may refer to an appendix): Relevant information is provided throughout the discussion and analysis section of this document.
- E. Outputs (may refer to an appendix): Relevant information is provided throughout the discussion and analysis section of this document.
- F. Evidence of, or reference to, computer program validation: Siemens's STAR-CCM+, The commercial multiphysics computational fluid dynamics (CFD) software, has achieved ASME Nuclear Quality Assurance-1 compliance. The addition of NQA-1 compliance in rigorous ASME QA certification program ensures the code meets industry-standard requirements for nuclear industry customers in support of safe-related application.
- G. Bases supporting application of the computer program to the specific physical problem: Calculation of flow velocity and pressure gradient calculations performed herein have been acceptably performed and are common analysis types for which the identified program, STARCCM+ is designed to be used and has been acceptably demonstrated through commercial use and application. The identified software package is well suited for the calculations documented by this report to the quality level indicated on the title page.

COMPUTER CODE VALIDATION – Nek5000

- A. Computer type: ANL - "Bebop": Intel Xeon E5-2695v4 Broadwell CPUs, INL – "Sawtooth": Intel Xeon 8268 Cascade Lake CPUs
- B. Operating System and Version: Beboop: CentOS 7 operating system, Sawtooth: CentOS 7.7 operating system
- C. Computer program name and revision: Nek5000 v19.0
- D. Inputs (may refer to an appendix): Relevant information is provided throughout the discussion and analysis section of this document.
- E. Outputs (may refer to an appendix): Relevant information is provided throughout the discussion and analysis section of this document.
- F. Evidence of, or reference to, computer program validation: Nek5000 is an open source

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CFD code, maintained and developed as part of the DOE NEAMS program. It has been in use for 30+ years as a high-fidelity CFD tool. It has been extensively validated through participation in international blind benchmarks.

- G. Bases supporting application of the computer program to the specific physical problem: Calculation of flow velocity and pressure gradient calculations performed herein have been acceptably performed and are common analysis types for which the identified program, Nek5000 is designed to be used and has been acceptably demonstrated through research, academic, and industry use and application. The identified software package is well suited for the calculations documented by this report to the quality level indicated on the title page.

DISCUSSION/ANALYSIS

A. GEOMETRY DESCRIPTION

Figure 1 shows the schematic of the test geometry. The inlet of the duct is a circular channel with an inner diameter (D_C) of 60.0 mm and a length of 300.0 mm. There is 40.0 mm-long transition region between the circular and annular channels. The inner diameter ($D_{A,in}$) and outer diameter ($D_{A,out}$) of annulus are 80.0 mm and 100.0 mm, respectively. The length of annular channel is 300.0 mm. In Case-A, only the inner edge of the annulus was rounded off from 0.0 mm to 20.0 mm. In Case-B, the radius of curvature of inner edge of the annulus ($R_{A,Curv}$) was fixed at 5.0 mm, and the radius of curvature of the circular channel ($R_{C,Curv}$) was varied from 0.0mm to 20.0 mm. Test matrix is summarized in Table 2.

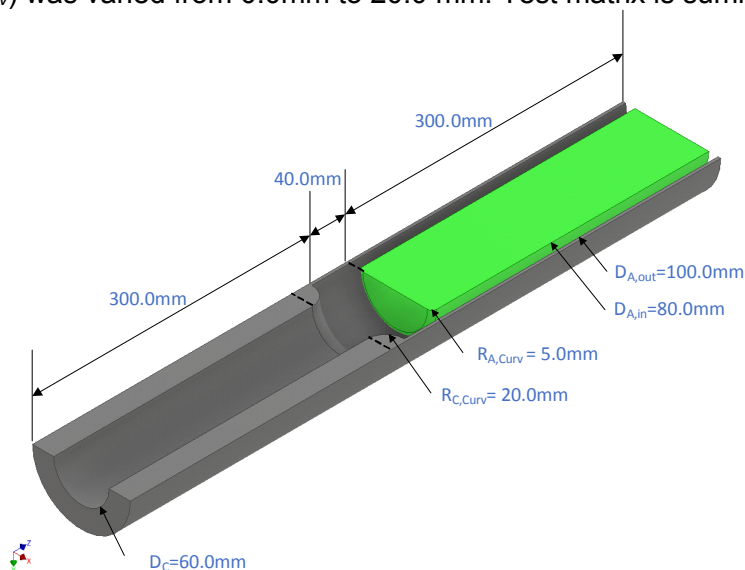


Figure 1. Schematic of the geometry sample ($R_{C,Curv} = 20.0\text{mm}$, $R_{A,Curv} = 5.0\text{ mm}$)

Table 2 TEST MATRIX

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Test Case	$R_{C, Curv}$ (mm)	$R_{A, Curv}$ (mm)
Case-A	0.0 (fixed)	0.0, 1.0, 2.0, 5.0, 10.0, 20.0
Case-B	0.0, 1.0, 2.0, 5.0, 10.0, 20.0	5.0 (fixed)

B. STAR-CCM+ MODEL DESCRIPTION

A commercially-available CFD software, STAR-CCM+ version 13.06.012-R8 [7] was adopted as a numerical solver. Three-dimensional, steady-state, incompressible, Reynolds-Averaged Navier-Stokes (RANS) equation-based simulation was solved by adopting the segregated flow, segregated isothermal, and Shear Stress Transport (SST) $k-\omega$ turbulence model with all y^+ wall treatment model. 2nd order convection schemes for the momentum and turbulence solver were adopted. Constant fluid properties were used in this analysis. The density and dynamic viscosity of sodium were specified by 860.0 kg/m^3 and $3.0 \times 10^{-3} \text{ Pa}\cdot\text{s}$, respectively. Inlet velocity and pressure outlet boundary conditions were specified to the inlet and outlet of the duct. Turbulent intensity of 0.01 and turbulent viscosity of 10.0 were employed to specify the turbulent parameters at the inlet boundary.

Figure 2 shows the typical mesh structure of computational domain. The polyhedral mesh with boundary prism layers was adopted for generating the computational mesh. The mesh structures of all CFD models are provided in **Appendix A**. The base size mesh of the CFD model was 1.0 mm. Target and minimum surface size were specified by 100% and 10% of the base size, respectively. The number of prism boundary layers was 8. Total thickness of the boundary prism layer was specified by 33.33% of the base size. The prism layer stretching ratio was specified by 1.2. The surface averaged wall y^+ value was less than 1. The radiuses of curvature of 1 mm and 2 mm resulted in larger number of cells than other cases. The mesh statistics are summarized in Table 3.

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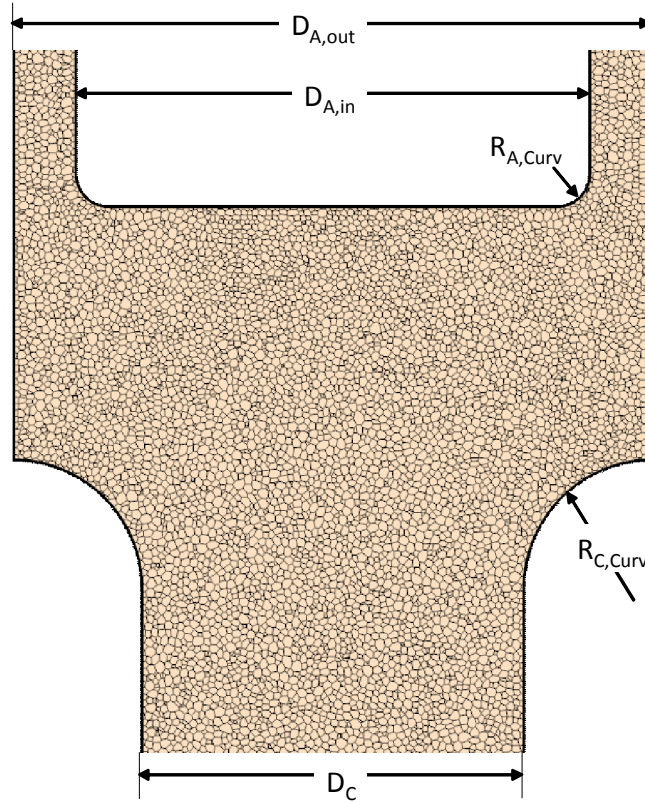


Figure 2. Mesh structure of STAR-CCM+ CFD Model ($R_{A,Curv} = 5\text{mm}$, $R_{C,Curv} = 20\text{mm}$)

Table 3. Mesh Statistics of the Star-CCM+ model

Test Case	$R_{C,Curv}$ (mm)	$R_{A,Curv}$ (mm)	Number of cells (Million)	Surface averaged Wall y^+ ($Re=1 \times 10^5$)
Case-A	0.0 (fixed)	0.0	3.58	0.84
		1.0	4.15	0.83
		2.0	3.98	0.81
		5.0	3.69	0.77
		10.0	3.53	0.75
		20.0	3.59	0.74
Case-B	1.0	5.0 (fixed)	4.81	0.77
	2.0		4.02	0.77
	5.0		3.94	0.77
	10.0		3.78	0.76

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	20.0		3.67	0.75
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C. STAR-CCM+ Results

Figure 3 shows the velocity distribution on the mid-plane of the Case-A geometry for Reynolds numbers of 2×10^4 . Figure 4 shows the pressure distribution on the mid-plane of the Case-A geometry for Reynolds numbers of 2×10^4 . The re-circulation region was observed at the corner of transition region. Flow separation and reattachment at the entrance of annulus were observed where the radius of curvature of internal structure was less than 10 mm. The peak velocity at the entrance of annulus was linearly proportional to the Reynolds number. Sudden contraction of flow area at the entrance of annulus resulted in Vena Contracta flow with the flow separation occurred only on one side. The peak velocity of Vena Contracta flow decreased as the radius of curvature increased.

The CFD results show that the pressure drop can be significantly reduced by the edge-rounding, e.g., the pressure drop was reduced approximately 56% by the radius of curvature of 5.0mm, and reduced 70% by the radius of curvature of 20.0 mm. The pressure drop of Case-A geometry as an inlet Reynolds number was shown in Figure 5. The pressure drop is proportional to the square of inlet Reynolds number. The second order polynomial fitting curves agreed with the CFD result. R-squared values of fitting curves were very close to unity. The pressure drop of Case-A geometry as a function of Radius of curvature was shown in Figure 6. The pressure drop of tested geometry decreased with increasing radius of curvature. For a large radius of curvature (e.g. in this test, greater than 10mm), increasing the radius of curvature would not yield a reduced pressure drop as much as small radius of curvature.

The flow separation occurred at the exit of circular channel and the recirculation region at the corners of transition region formed by the impinging jet flow from the circular channel. The minor pressure loss due to this flow separation and recirculation can be reduced by adding the curved edge at the exit of circular channel. To evaluate the effect of edge smoothing at the exit of circular channel, the CFD simulations of Case-B geometries were carried out. Figure 7 shows the velocity distribution on the mid-plane of Case-B geometry for three Reynolds number of 2×10^4 . Figure 8 shows the pressure distribution on the mid-plane of the Case-B geometry for Reynolds number of 2×10^4 . The effect of radius of curvature at the exit of circular channel, i.e., the entrance of transition region, was relatively less than that of inner radius which faces the flow. As show in Figure 9, a large radius of curvature at the exit of circular channel is needed to get the pressure loss reduction greater than 10%. Hence, it can be concluded that the benefit of edge rounding of exit of flow channel is not significant.

In summary, if there is no other geometrical restriction, the radius of curvature of 10.0 mm for both sides of edge would be applicable to reduce the local pressure loss in the channel which has sudden expansion and contraction in the flow area. In this ECAR, the ratio of channel diameters and the radius of curvature was not investigated. A further parametric study on the design parameters is necessary to provide a general guideline for the design optimization. The velocity distributions and pressure distributions by other Reynolds numbers are provided in **Appendix B** and **Appendix C**, respectively. All pressure drop results are summarized in **Appendix D**.

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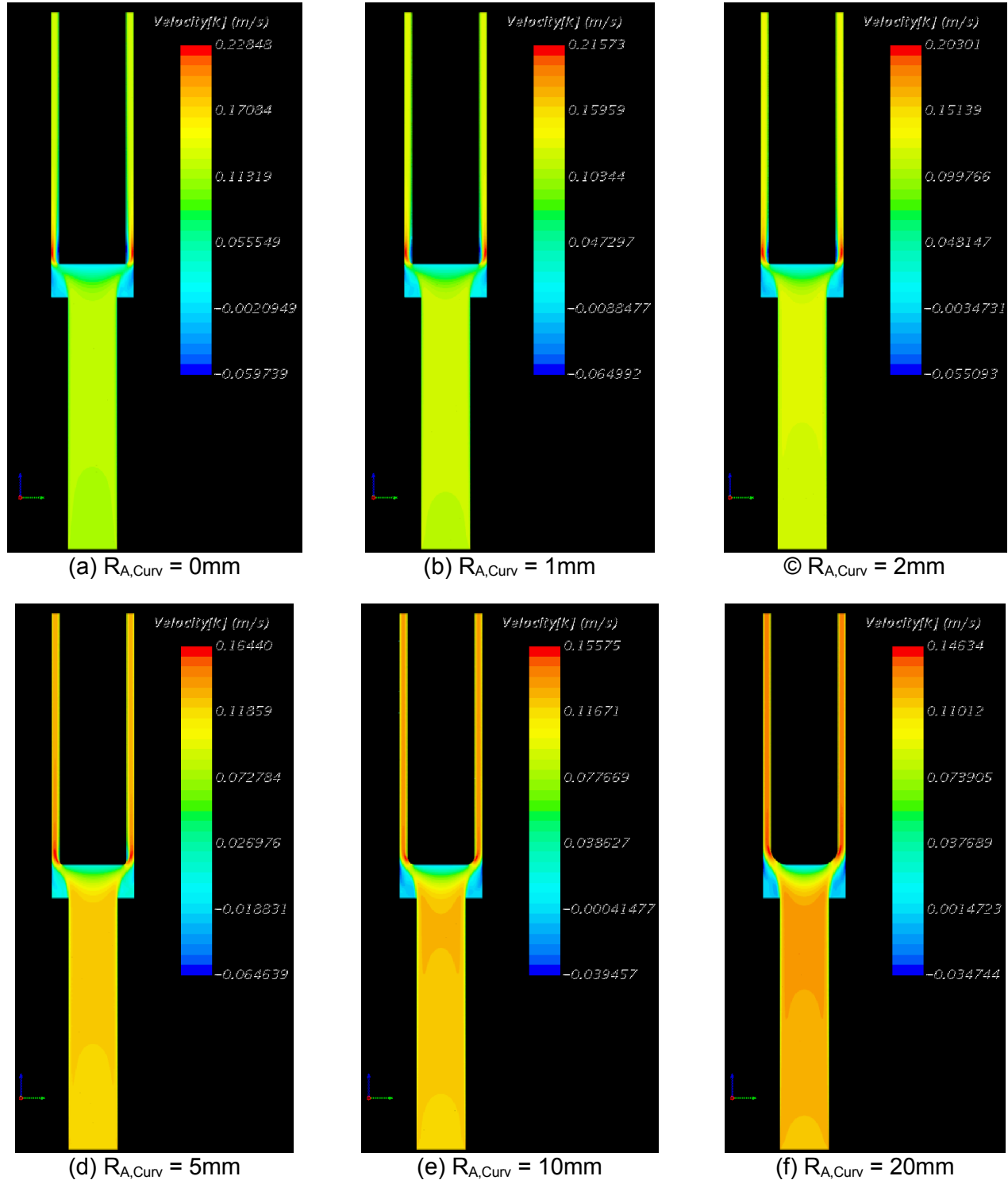


Figure 3 Velocity profiles on the mid-plane of the channel (Case-A, $Re_D = 2 \times 10^4$)

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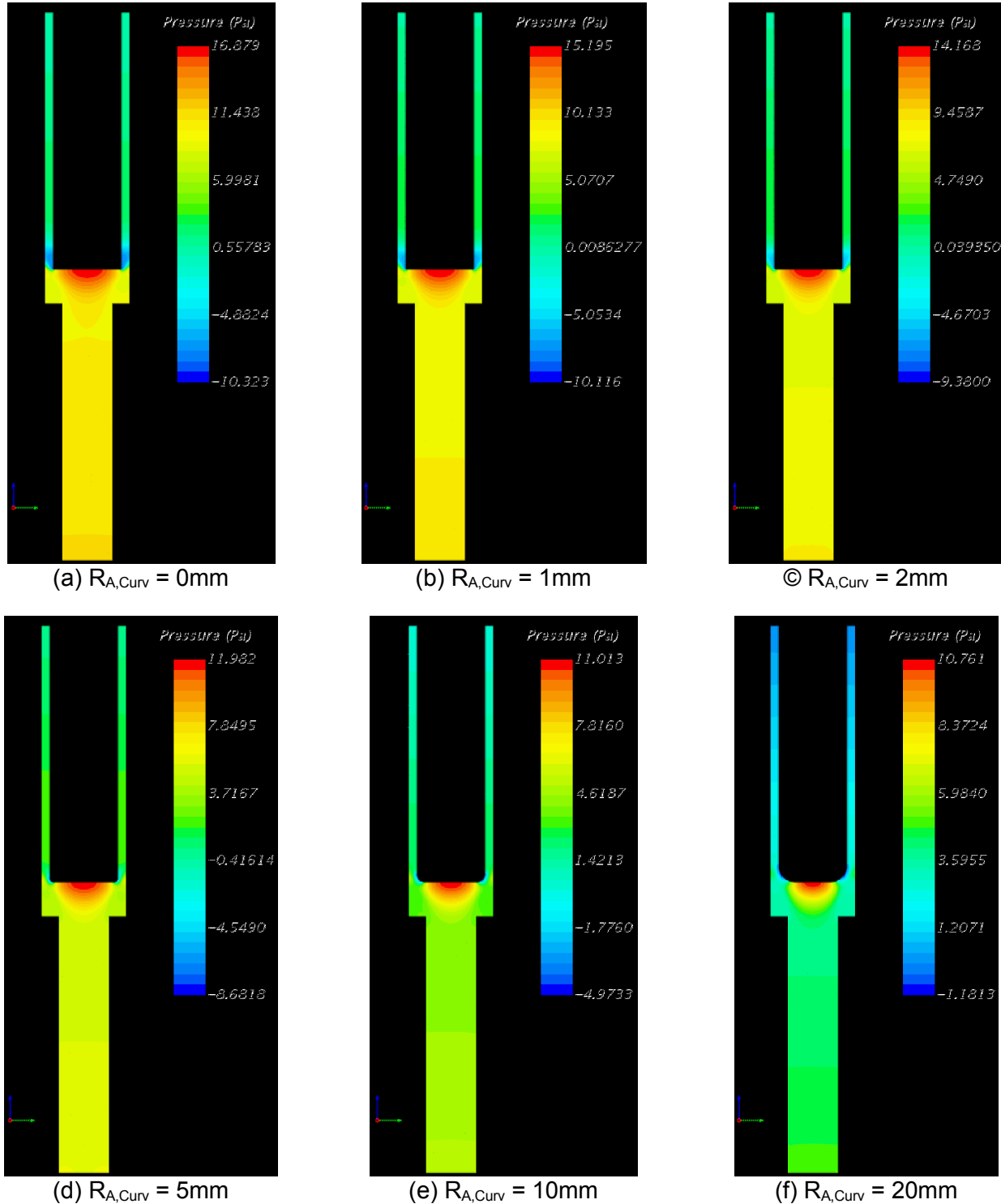


Figure 4 Pressure distributions on the mid-plane of the channel (Case-A, $Re_D = 2 \times 10^4$)

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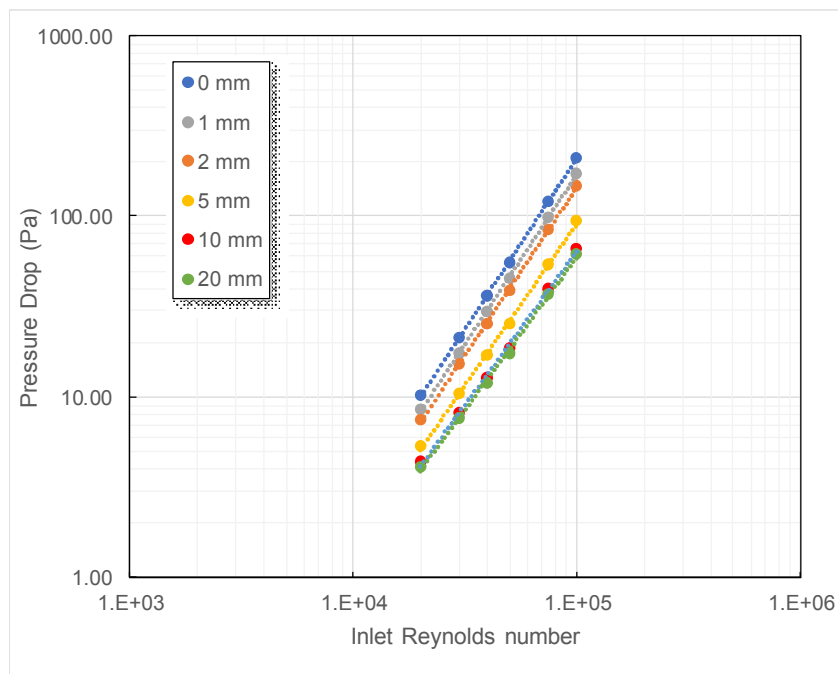


Figure 5 Pressure drop of Case-A geometry plotted as a function of Inlet Reynolds number

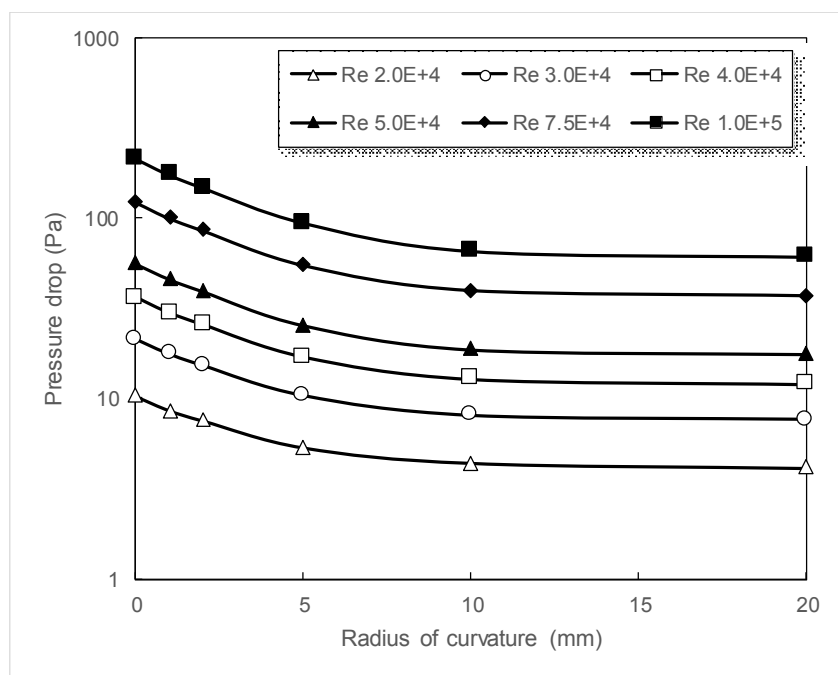


Figure 6 Pressure drop of Case-A geometry plotted as a function of radius of curvature

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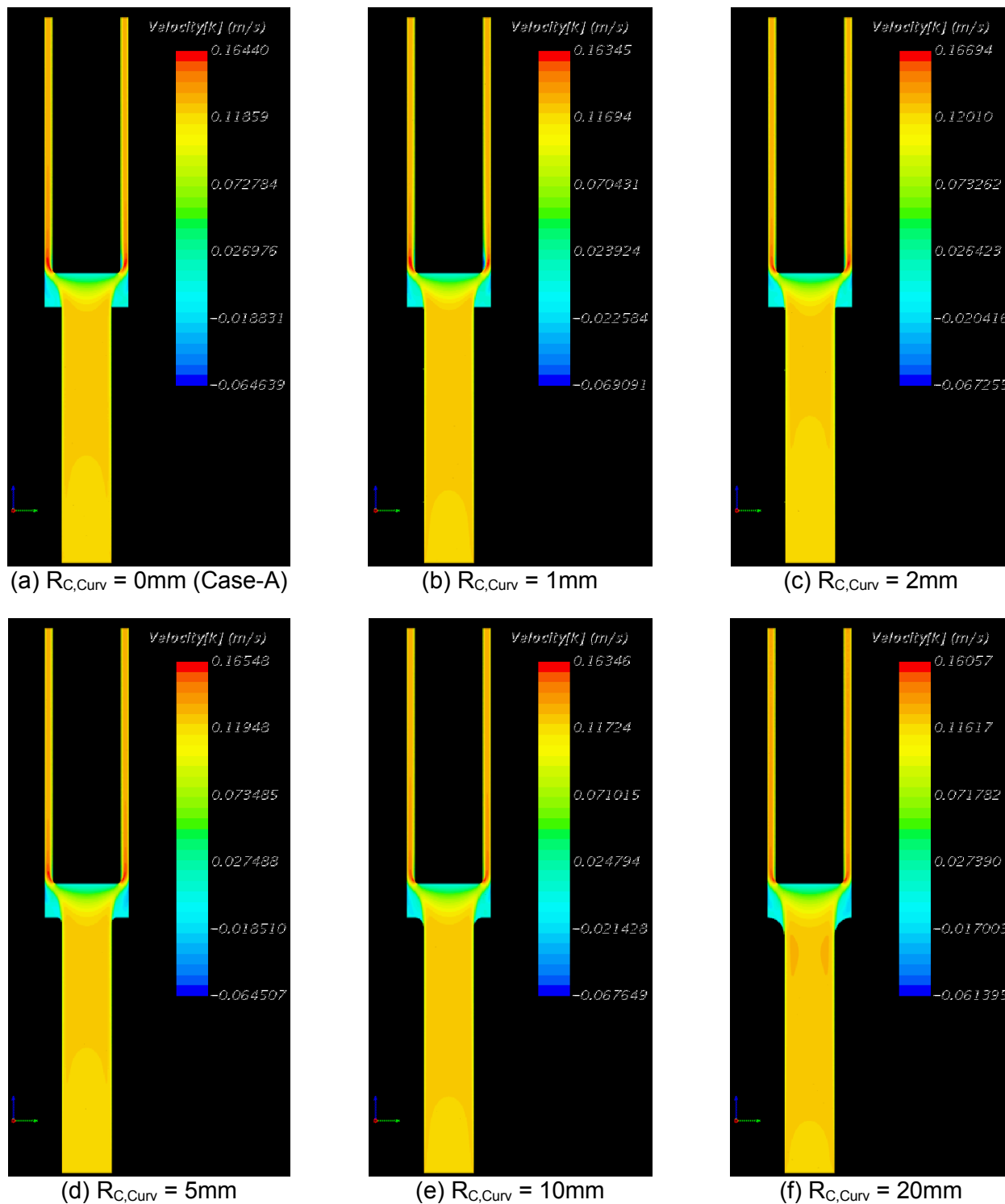


Figure 7 Velocity distributions on the mid-plane of the channel (Case-B, $Re_D = 2 \times 10^4$)

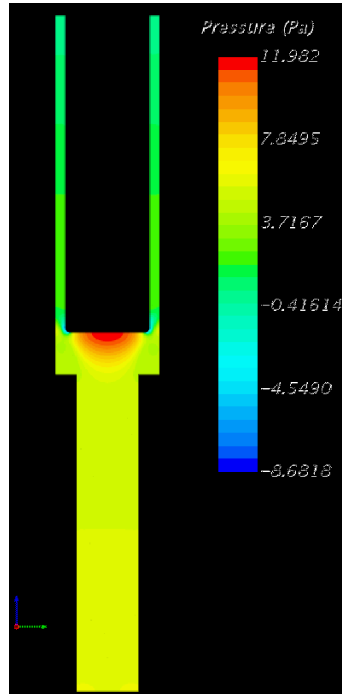
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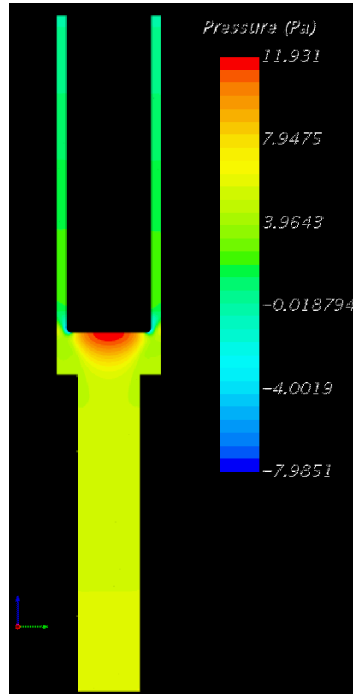
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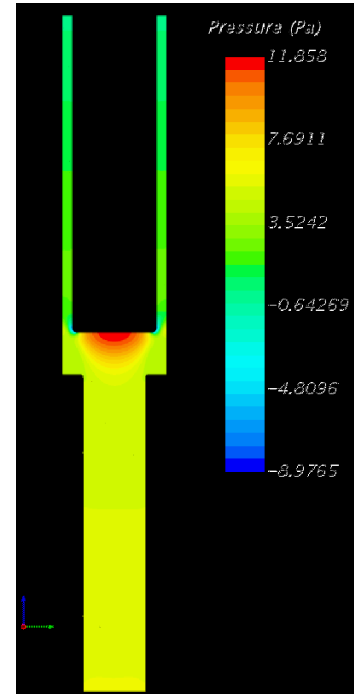
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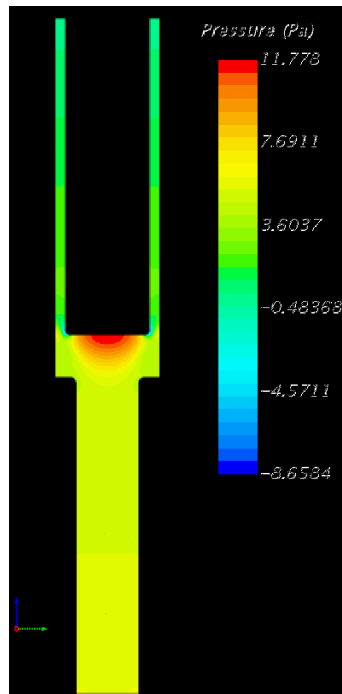
(a) $R_{C, Curv} = 0\text{mm}$ (Case-A)



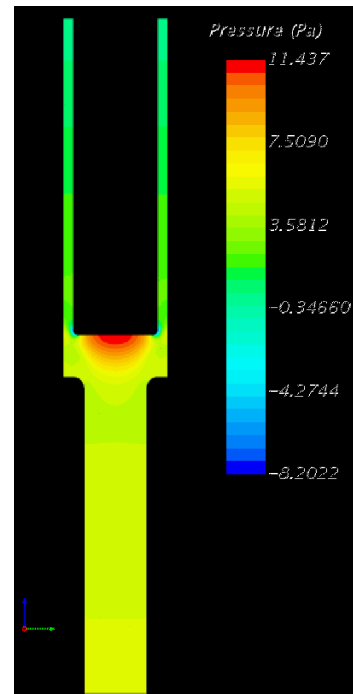
(b) $R_{C, Curv} = 1\text{mm}$



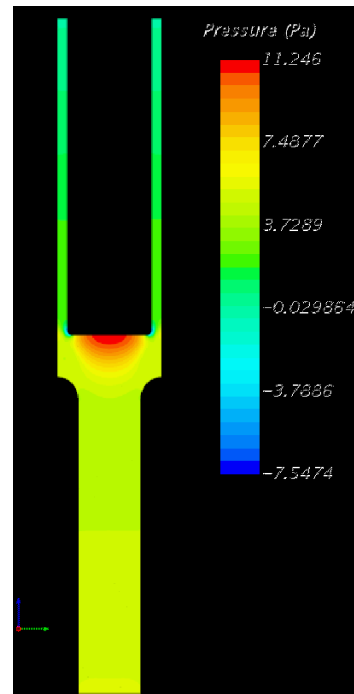
(c) $R_{C, Curv} = 2\text{mm}$



(d) $R_{C, Curv} = 5\text{mm}$



(e) $R_{C, Curv} = 10\text{mm}$



(f) $R_{C, Curv} = 20\text{mm}$

Figure 8 Pressure distributions on the mid-plane of the channel (Case-B, $Re_D = 2 \times 10^4$)

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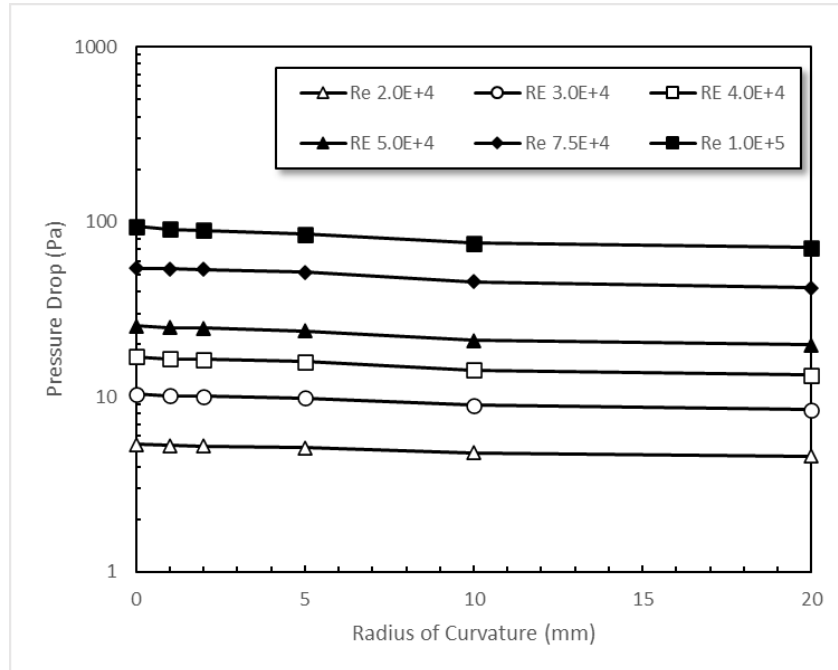


Figure 9 Pressure drop of Case-B geometry plotted as a function of radius of curvature

D. NEK5000 MODEL DESCRIPTION

In Nek5000, the dimensionless, incompressible, constant-viscosity forms of the conservation of mass and momentum equations were solved. These are given by

(4)

(5)

Where the inlet diameter and inlet mean velocity were used as reference values for length and velocity, respectively. This leads to the definition of the Reynolds number as

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(6)

Which is consistent with the definition used in the Star-CCM+ analysis. It is important to note that the only non-trivial input parameter for each Nek5000 simulation is the Reynolds number. This encompasses the effects of fluid density, viscosity, and flow rate. Turbulence was modeled using an LES approach, which captures all but the smallest scale structures in the flow. The model is implemented using a filtering approach, where the velocity is filtered after every time step, adding dissipation at the smallest scales.

A recycling boundary condition was used in the Nek5000 simulations for the inlet. The velocity profile from 4.5 diameters downstream of the inlet was interpolated back onto the inlet and appropriately scaled to ensure a consistent mass flux. Recycling the boundary condition in this way ensures that turbulence is well characterized at the inlet boundary.

Nek5000 requires a mesh consisting entirely of hexahedral elements. As an inherent part of the spectral element method, the element mesh is further subdivided into Gauss-Lobatto-Legendre (GLL) quadrature points where the number of GLL points is based on the spatial approximation order. In this work a consistent blocking structure was used which could accommodate the investigated edge radii. Cross sections of two of the meshes used, one for the sharp-edged and one for the case with both fillets set to 5mm, are shown in Figure 10 with the overlaid GLL points at 7th order accuracy.

Mesh-independence was confirmed for the sharp-edged case by gathering statistical pressure drop data at 5th, 7th, 9th, and 11th spatial approximation orders. Each subsequent increase in the approximation order represents a geometric increase in spatial resolution. This sort of mesh independence study is known as p-type study. The pressure drop data is plotted in Figure 11, with the average values and percent differences compared to the 11th order data given in Table 4. The difference between 5th and 11th order was demonstrated to be only 2%, which is quite reasonable. The average next-to-wall y^+ value is also shown for each mesh. Typically a value of less than 1 is recommended for a wall-resolved method, however consistent results are obtained at an average value of 1.21, it is therefore concluded that a 7th order mesh is well resolved. It is expected that this case will have the highest resolution requirements due to the nature of flow around sharp edges and that a 7th order mesh will be sufficient for the remaining cases. The mesh statistics for all LES cases are shown in Table 5.

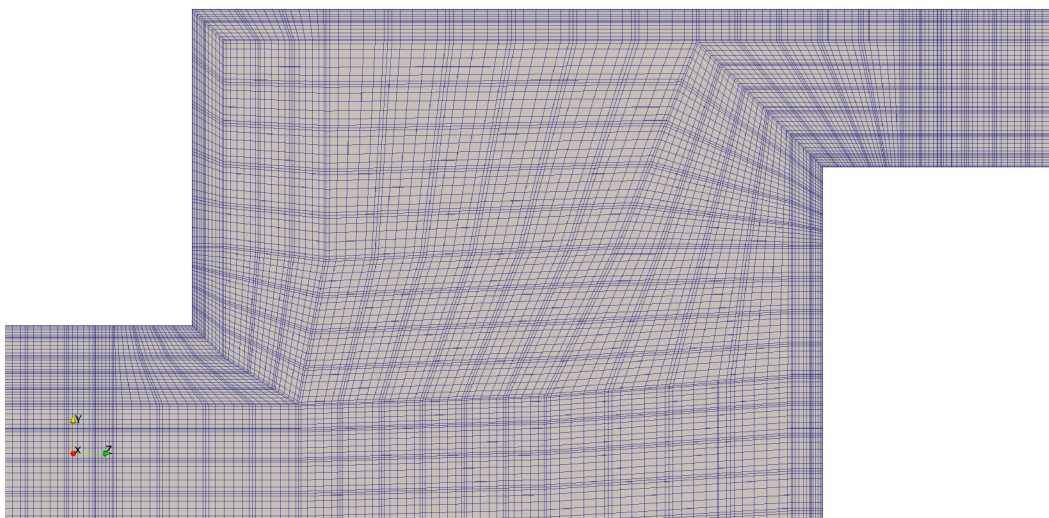
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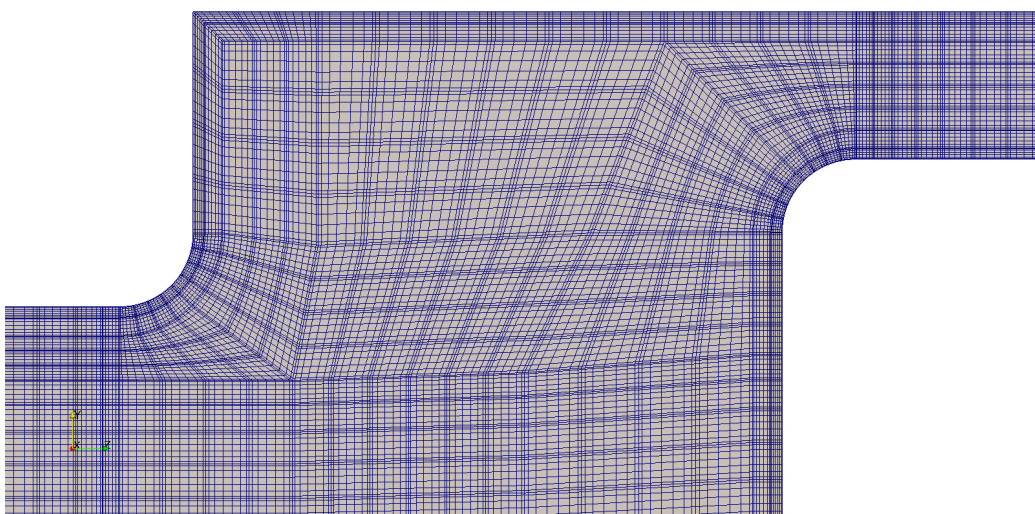
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(a) sharp-edged case



(b) 5mm fillets on inlet and annulus edges

Figure 10 Cross section of the 7th order Nek5000 meshes for (a) the sharp-edged case and (b) a rounded edge case.

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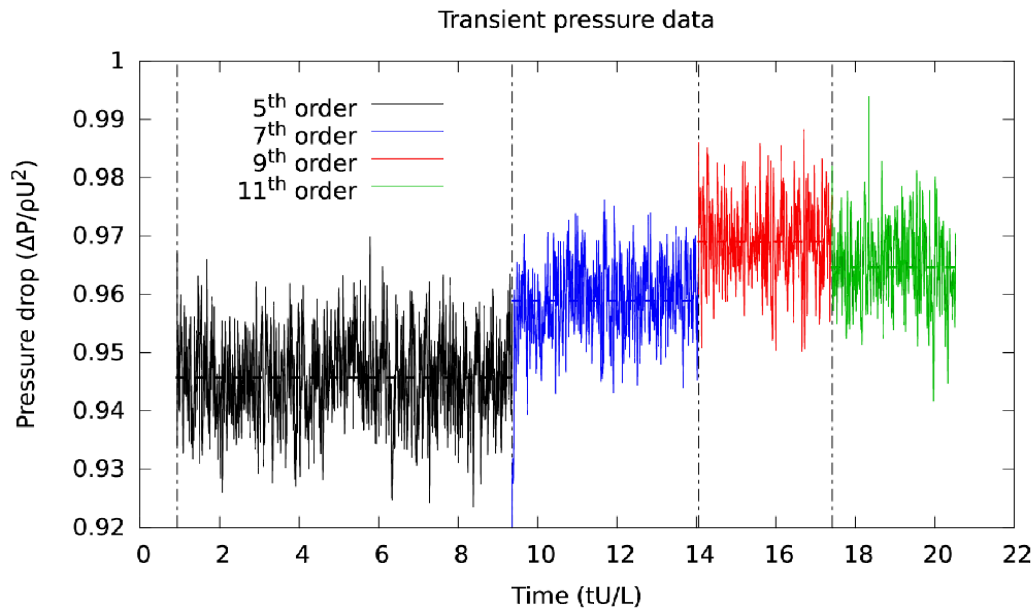


Figure 11 Transient pressure drop data for the sharp-edged case at varying spatial approximation orders, the dashed lines indicate averaged values.

Table 4 Pressure drop and percent differences for the sharp-edged case at varying spatial approximation order

Order	Average y^+ of the first GLL point	Average pressure drop	Percent difference
5	2.15	0.946	1.98
7	1.21	0.959	0.598
9	0.77	0.969	0.452
11	0.53	0.965	--

Table 5 Meshing statistics for the Nek5000 analysis

Test Case	$R_{C,Curv}$ (mm)	$R_{A,Curv}$ (mm)	Number of elements	Number of degrees of freedom (millions)	Average y^+
Case-A	0.0 (fixed)	0.0	81,040	27.5	1.21
		2.0	77,040	26.1	1.18
		5.0	79,040	26.8	1.15
		10.0	83,040	28.1	1.13
Case-B	2.0	5.0 (fixed)	74,720	25.3	1.14
	5.0		79,040	26.8	1.15
	10.0		83,360	28.3	1.14

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E. NEK5000 RESULTS

LES cases were run with Nek5000 for an inlet Reynolds number of 20,000. For a flow of liquid sodium with a density of 860 kg/m^3 and viscosity of 0.0003 kg/m-s , this corresponds to an inlet velocity of 0.12 m/s . A Reynolds number of 20,000 was chosen as higher values proved to be too expensive computationally. All simulations were run until the recycling inlet condition reached a statistically fully developed state and an additional duration to allow the full domain to reach a statistically steady state. This corresponded to approximately 20 flow-through times ($t = 20 \text{ L/U}$). The instantaneous pressure drop was then recorded at every time step for an additional 10-20 flow-through times and time-averaged to reduce statistical uncertainty.

The overall loss coefficients and the corresponding pressure drop in Pa are provided in Table 6 and the loss coefficients predicted by LES in Nek5000 are compared to those predicted with RANS in Star-CCM+ in Figure 12 for the varying outlet radius and Figure 13 for the varying inlet radius. The LES data was curve fit using an exponential function and uncertainty bands of $\pm 5\%$ and $\pm 20\%$ are shown for reference. It can be seen that the RANS model in Star-CCM+ consistently predicts about a 20% lower pressure drop compared to the LES model in Nek5000. It is likely that the LES results are more accurate due to the higher-fidelity nature of the model and the significant recirculation zones present in the flow, which RANS models are known to have difficulty in predicting accurately.

Table 6 Pressure drop results for the LES cases

Test Case	$R_{C, \text{Curv}}$ (mm)	$R_{A, \text{Curv}}$ (mm)	Loss coefficient	Pressure drop (Pa)
Case-A	0.0 (fixed)	0.0	1.93	11.2
		2.0	1.49	8.6
		5.0	1.15	6.7
		10.0	0.924	5.4
Case-B	2.0	5.0 (fixed)	1.14	6.6
	5.0		1.12	6.5
	10.0		1.10	6.4

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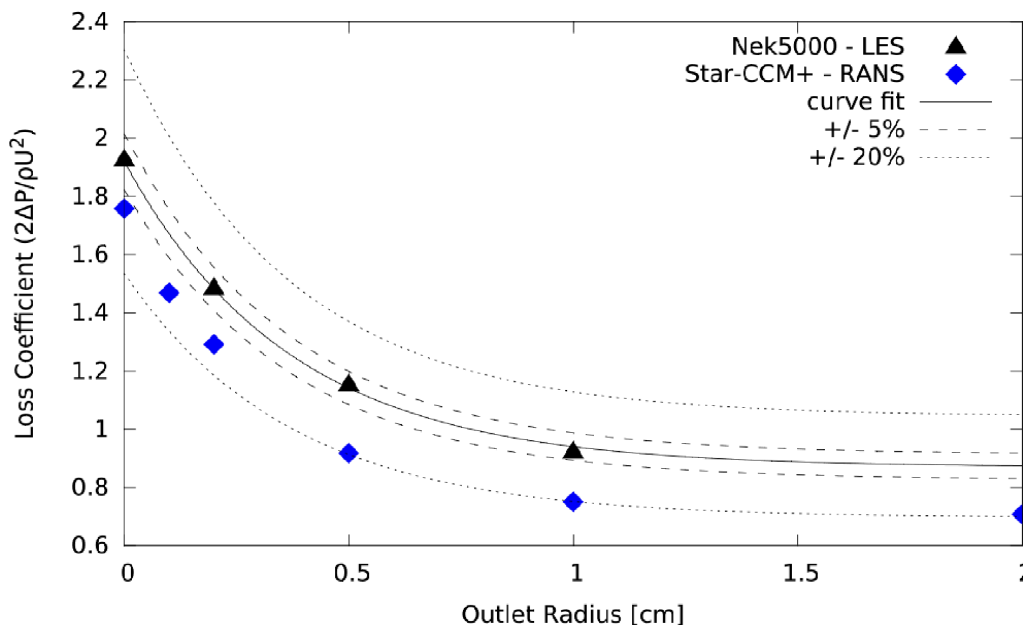


Figure 12 Variation in the overall loss coefficient for variable outlet edge roundedness

Colormaps showing profiles of the instantaneous and average velocity distributions on a midplane slice across the transition region for the sharp-edged case are shown in Figure 14 with the pressure profiles shown in Figure 15 with the colormaps of the time-averaged distributions for the remainder of the cases presented in **Appendix E**. From the results presented in Figures 12 & 13, both models predict very similar trends in behavior. It can then reasonably be concluded that the effect of increasing the edge radius on the outlet has by far the more significant effect on the overall pressure drop. This is likely due to the presence of the vena contract, which can be seen in the velocity colormaps just after the transition to the annulus. As the outlet radius is increased, the effect of the vena contracta can be observed to decrease in magnitude.

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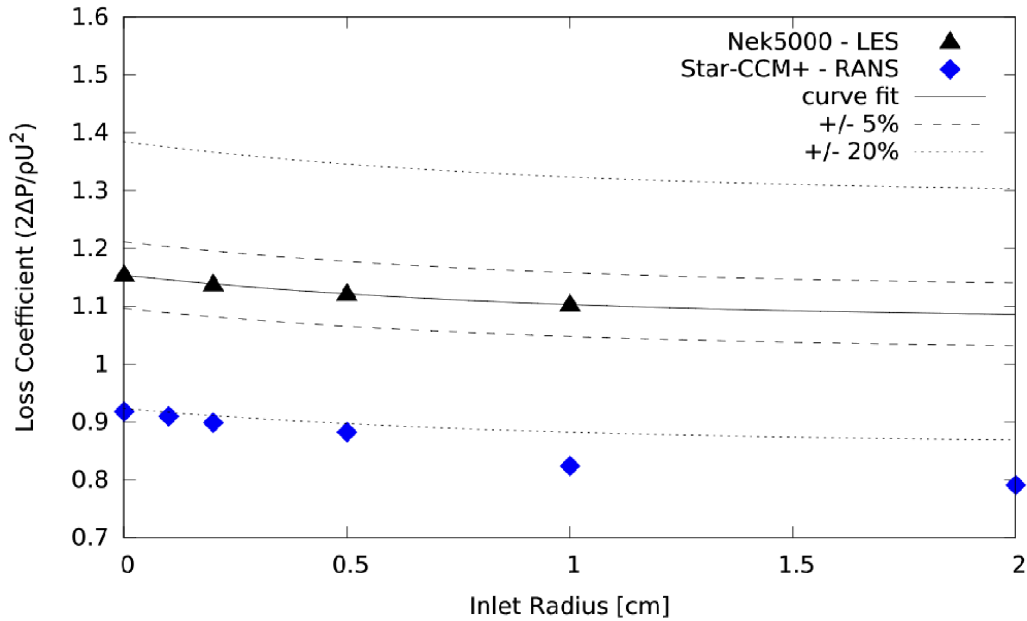


Figure 13 Variation in the overall loss coefficient for variable inlet edge roundedness

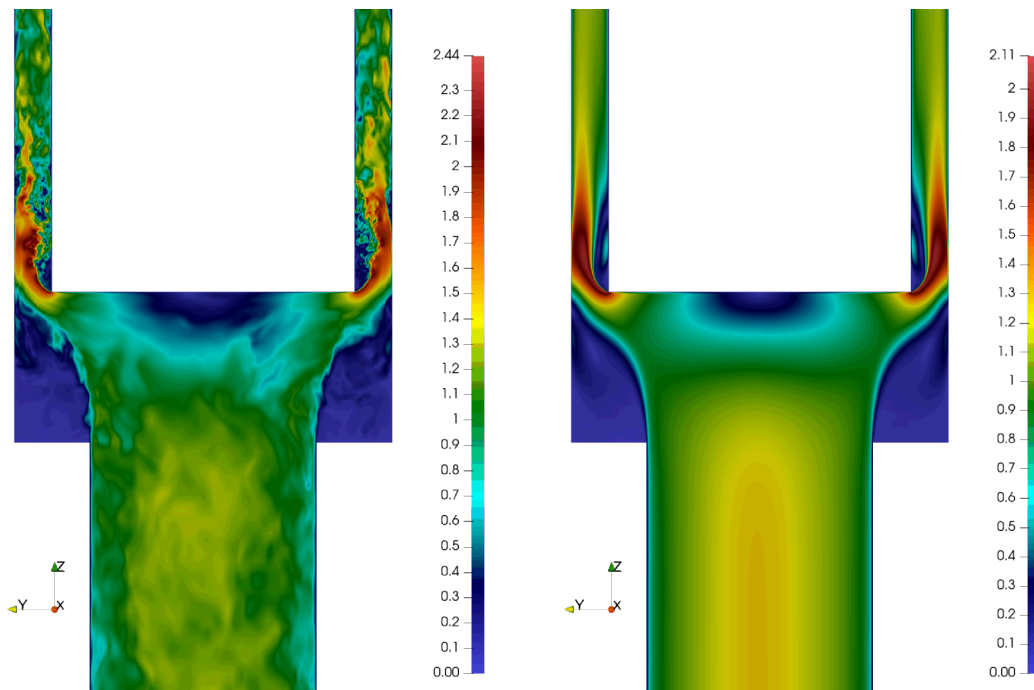


Figure 14 Velocity (u/U) predicted by Nek5000 for the sharp-edged case showing both (left) instantaneous and (right) time-averaged profiles.

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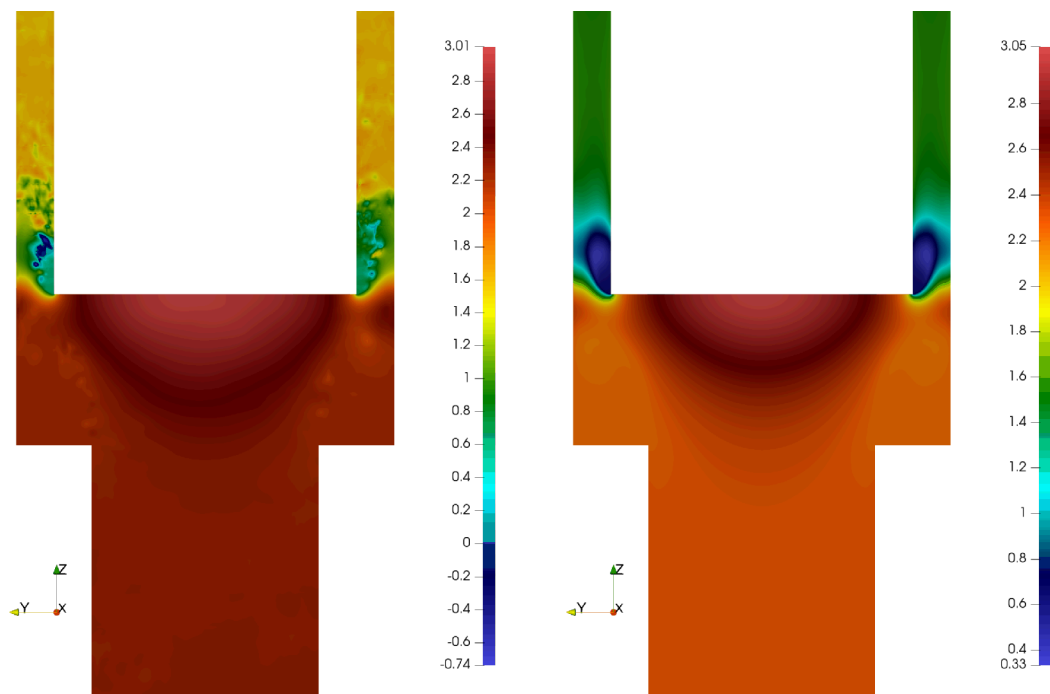


Figure 15 Pressure ($P/\rho U^2$) predicted by Nek5000 for the sharp-edged case showing both (left) instantaneous and (right) time-averaged profiles.

SUMMARY

In this ECAR, the computational fluid dynamics (CFD) simulation of the duct with a cross-section varying from circle to annulus was performed to evaluate the effect of edge-rounding of the internal edges. The edge of circular channel and the edge of inner annular channel were rounded with the radius of curvature ranged from 0 mm to 20 mm. The CFD results show that the pressure loss of the duct can be reduced by increasing the radius of the rounded edge. Case-A results showed that the pressure drop can be significantly reduced by the edge-rounding, e.g., the pressure drop was reduced approximately 56% by the radius of curvature of 5.0mm, and reduced 70% by the radius of curvature of 20.0 mm although its effectiveness would be attenuated as the radius of curvature of edge increases. Results from Case-B showed the impact of rounding the inlet edge was practically negligible compared to the outlet edge. This ECAR could provide a guideline to determine the optimum inlet module design of the VTR fuel rod bundle.

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- [1] S. Cheng and N. Todreas, "Hydrodynamic models and correlations for bare and wire-wrapped hexagonal rod bundles — Bundle friction factors, subchannel friction factors and mixing parameters," *Nuclear Engineering and Design*, vol. 92, no. 2, pp. 227-251, 1986.
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- [5] C. Baxi and M. Dalle Donne, *Heat Transfer and Fluid Flow in Nuclear Systems*, Pergamon Press Inc., 1981, pp. 410-462.
- [6] I. Idelchik, *Handbook of Hydraulic resistance*, 3rd Edition, New York: Begell House, 2001.
- [7] Siemens PLM Software, "STAR-CCM+ Documentation," 2019.

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Appendix A. MESH STRUCTURE OF STAR-CCM+ MODEL

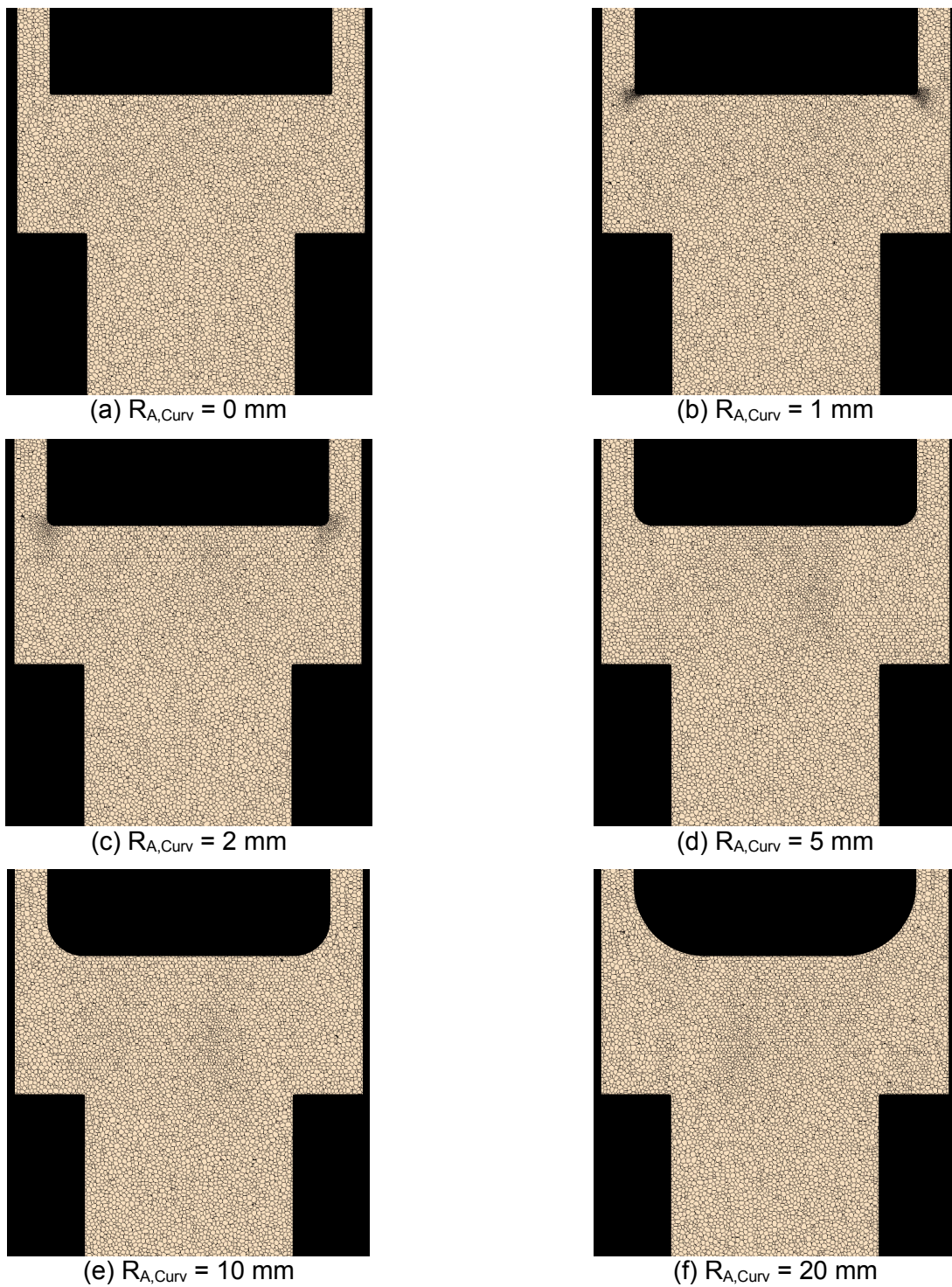
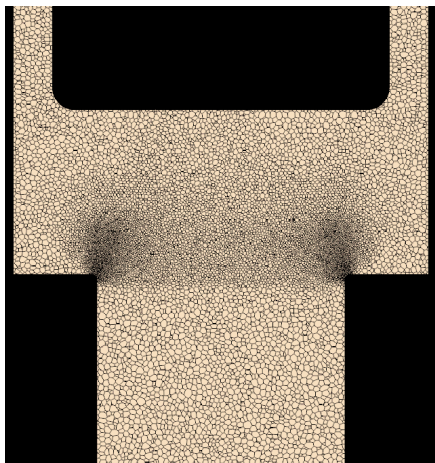


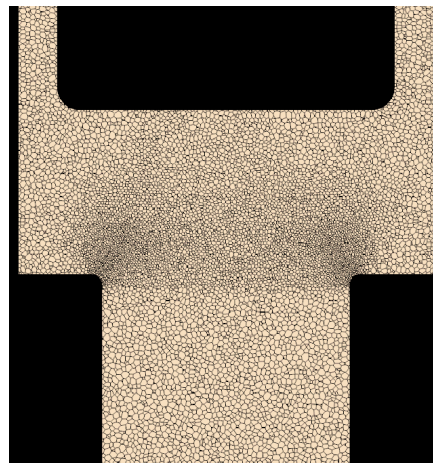
Figure A.1. Mesh structure in vicinity of transition region (Case-A).

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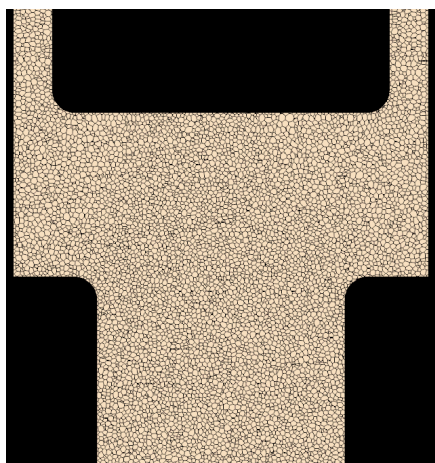
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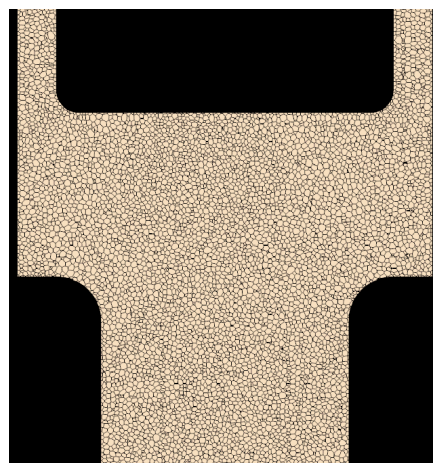
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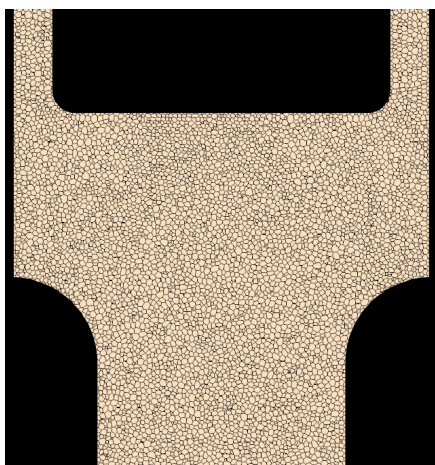
(b) $R_{A,Curv} = 5\text{mm}$, $R_{C,Curv} = 2\text{ mm}$



(c) $R_{A,Curv} = 5\text{mm}$, $R_{C,Curv} = 5\text{ mm}$



(d) $R_{A,Curv} = 5\text{mm}$, $R_{C,Curv} = 10\text{ mm}$



(e) $R_{A,Curv} = 5\text{mm}$, $R_{C,Curv} = 20\text{ mm}$

Figure A.2. Mesh structure in vicinity of transition region (Case-B).

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Appendix B. THE STAR-CCM+ VELOCITY DISTRIBUTION RESULTS

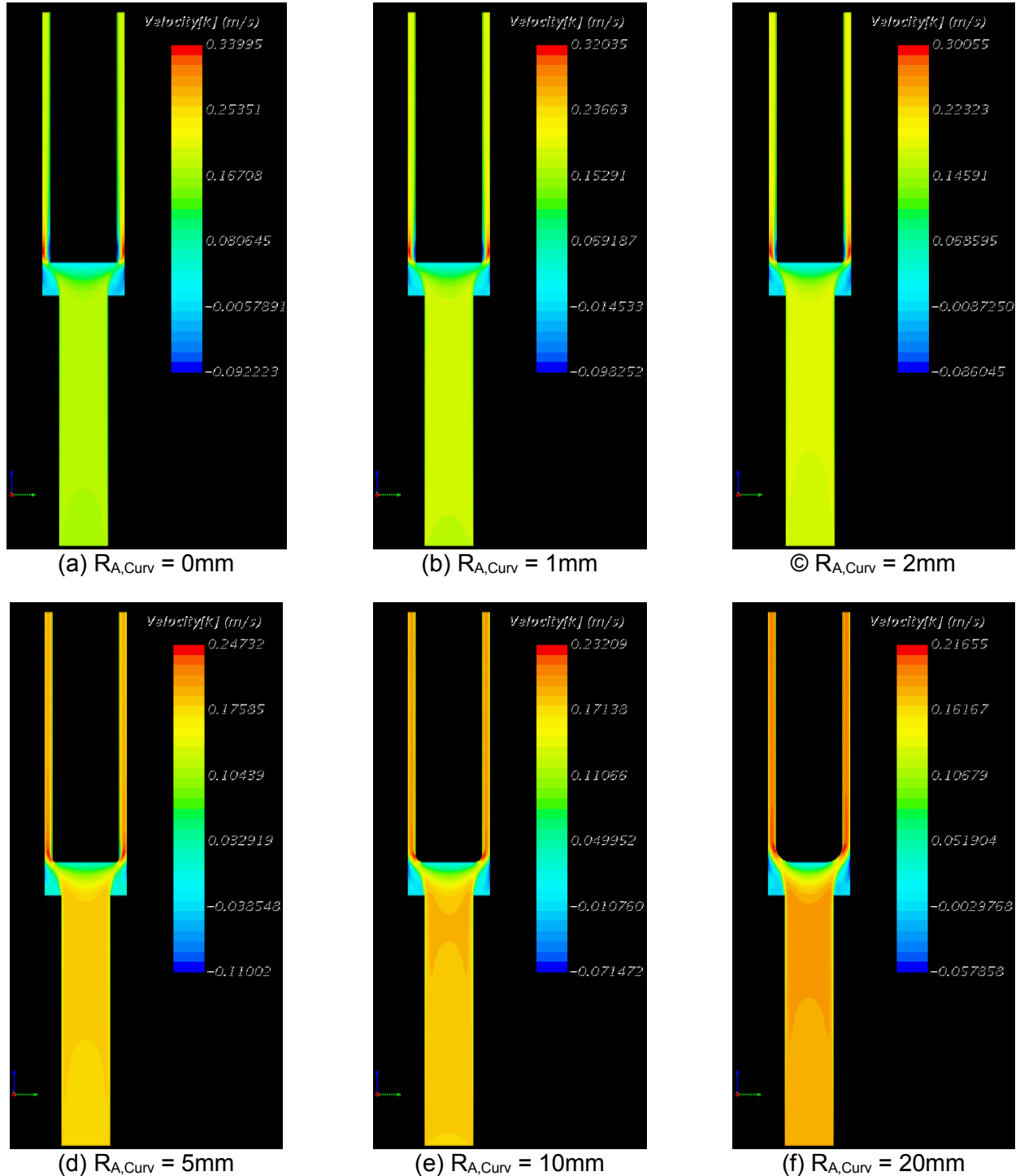


Figure B.1. Velocity profiles on the mid-plane of the channel (Case-A, $Re_D = 3 \times 10^4$).

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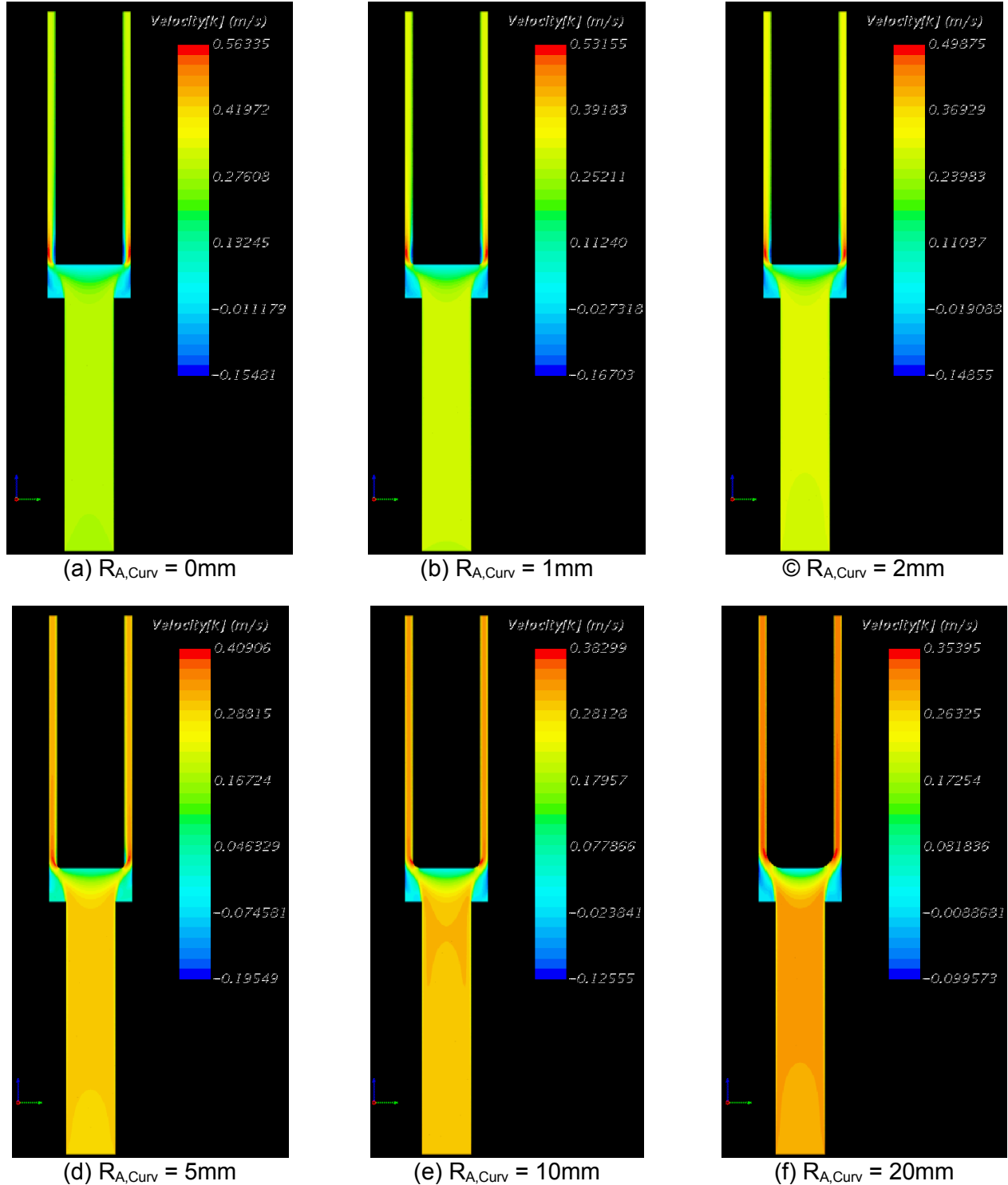


Figure B.2. Velocity profiles on the mid-plane of the channel (Case-A, $Re_D = 5 \times 10^4$)

Title: Computational Evaluation on Effect of Edge-rounding in Duct with Cross-section varying from Circle to Annulus

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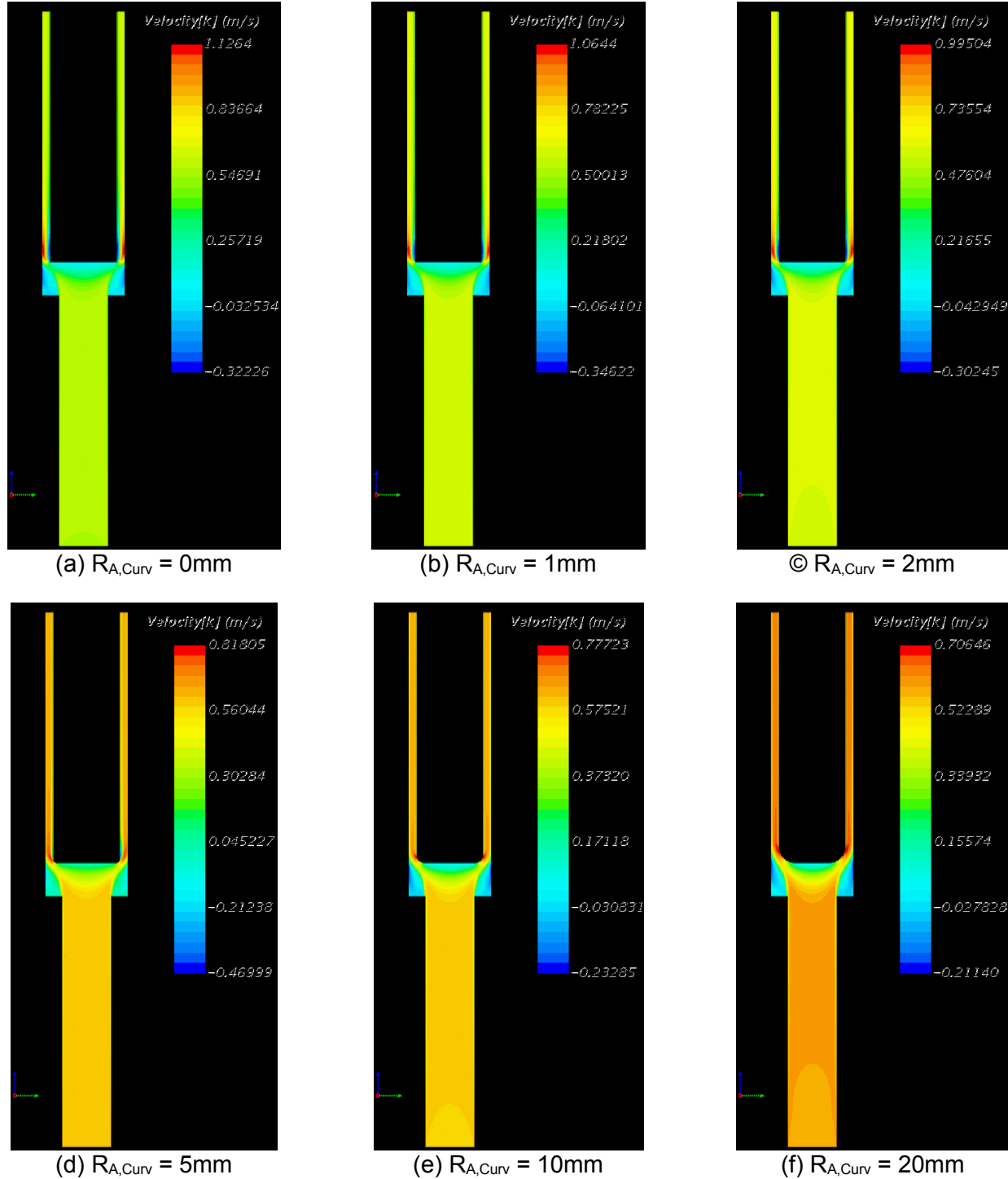


Figure B.3. Velocity profiles on the mid-plane of the channel (Case-A, $Re_D = 1 \times 10^5$).

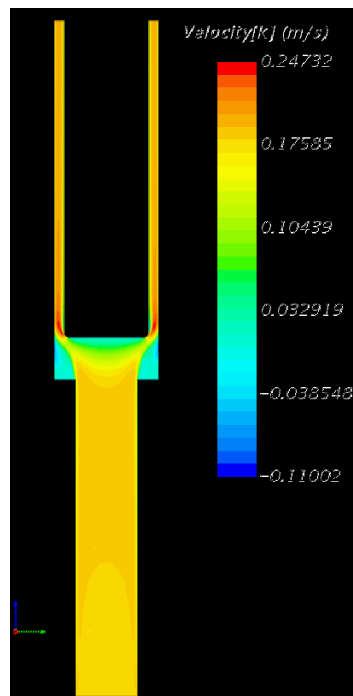
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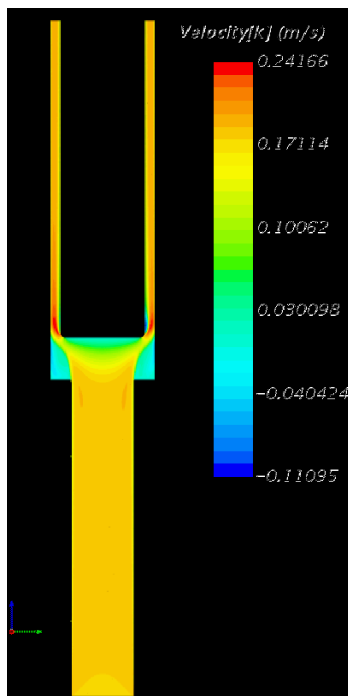
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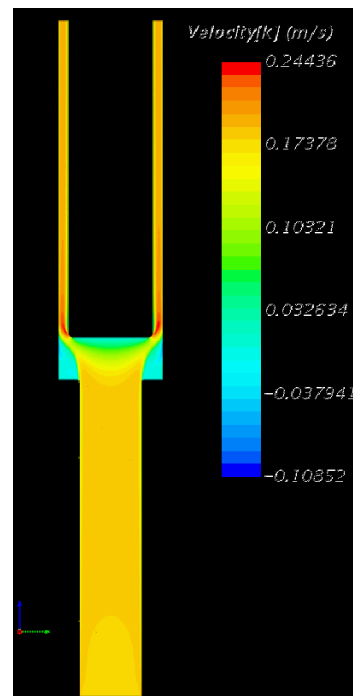
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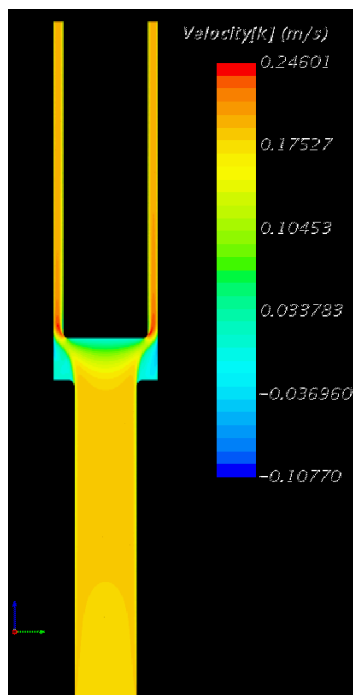
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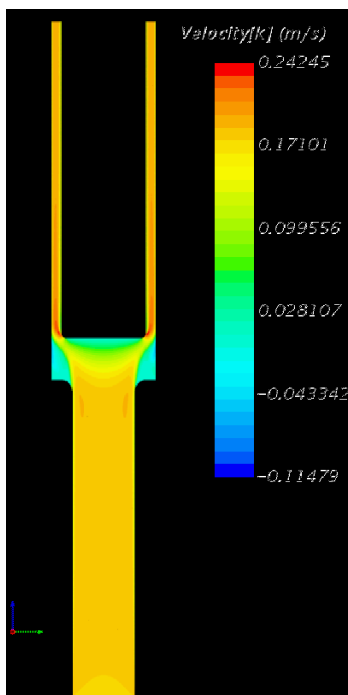
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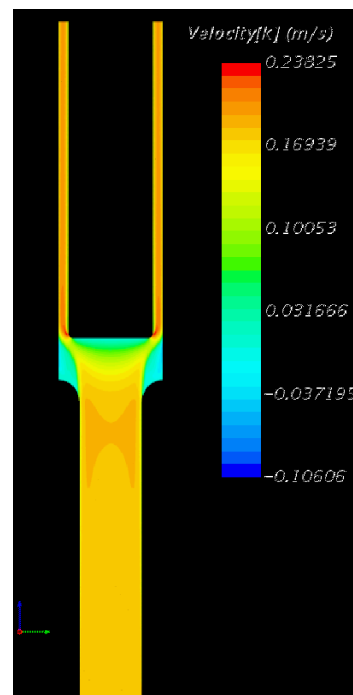
(c) $R_{C, Curv} = 2\text{mm}$



(d) $R_{C, Curv} = 5\text{mm}$



(e) $R_{C, Curv} = 10\text{mm}$



(f) $R_{C, Curv} = 20\text{mm}$

Figure B.4. Velocity distributions on the mid-plane of the channel (Case-B, $Re_D = 3 \times 10^4$).

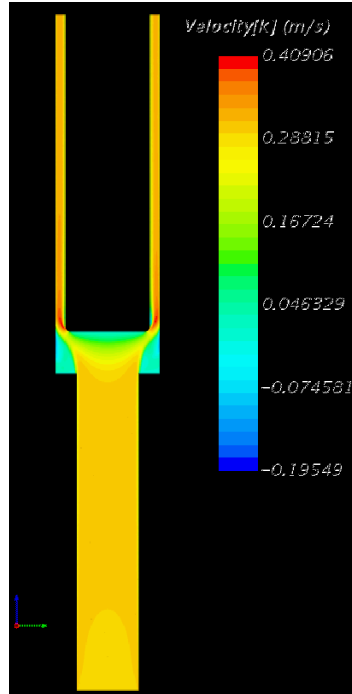
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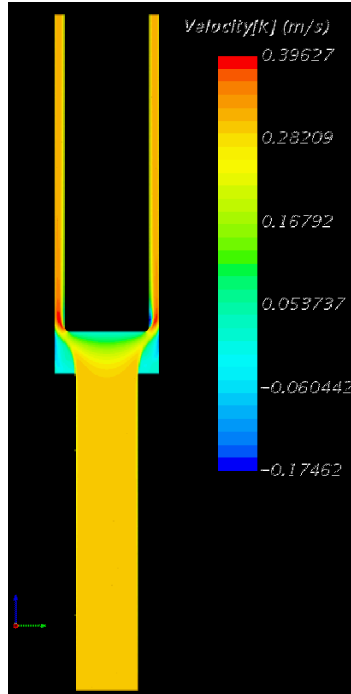
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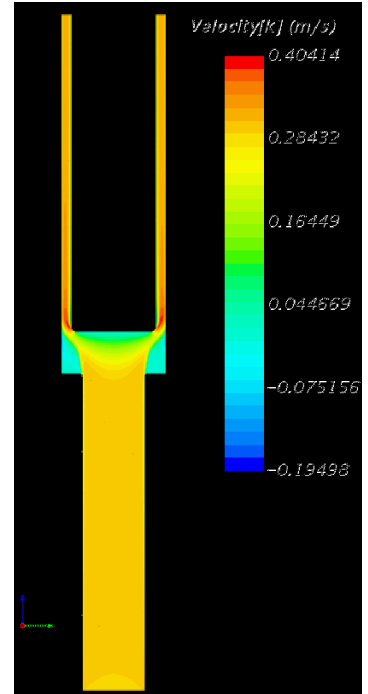
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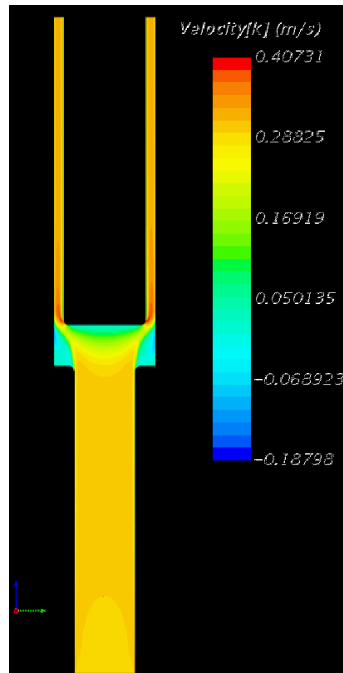
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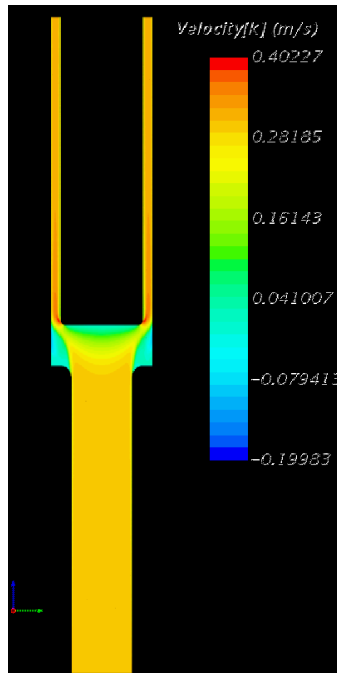
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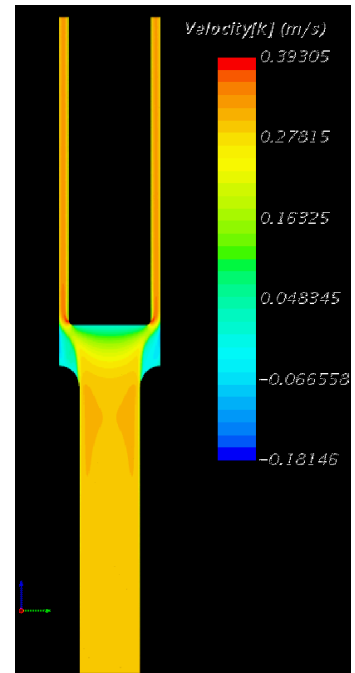
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(e) $R_{C, Curv} = 10\text{mm}$



(f) $R_{C, Curv} = 20\text{mm}$

Figure B.5. Velocity distributions on the mid-plane of the channel (Case-B, $Re_D = 5 \times 10^4$)

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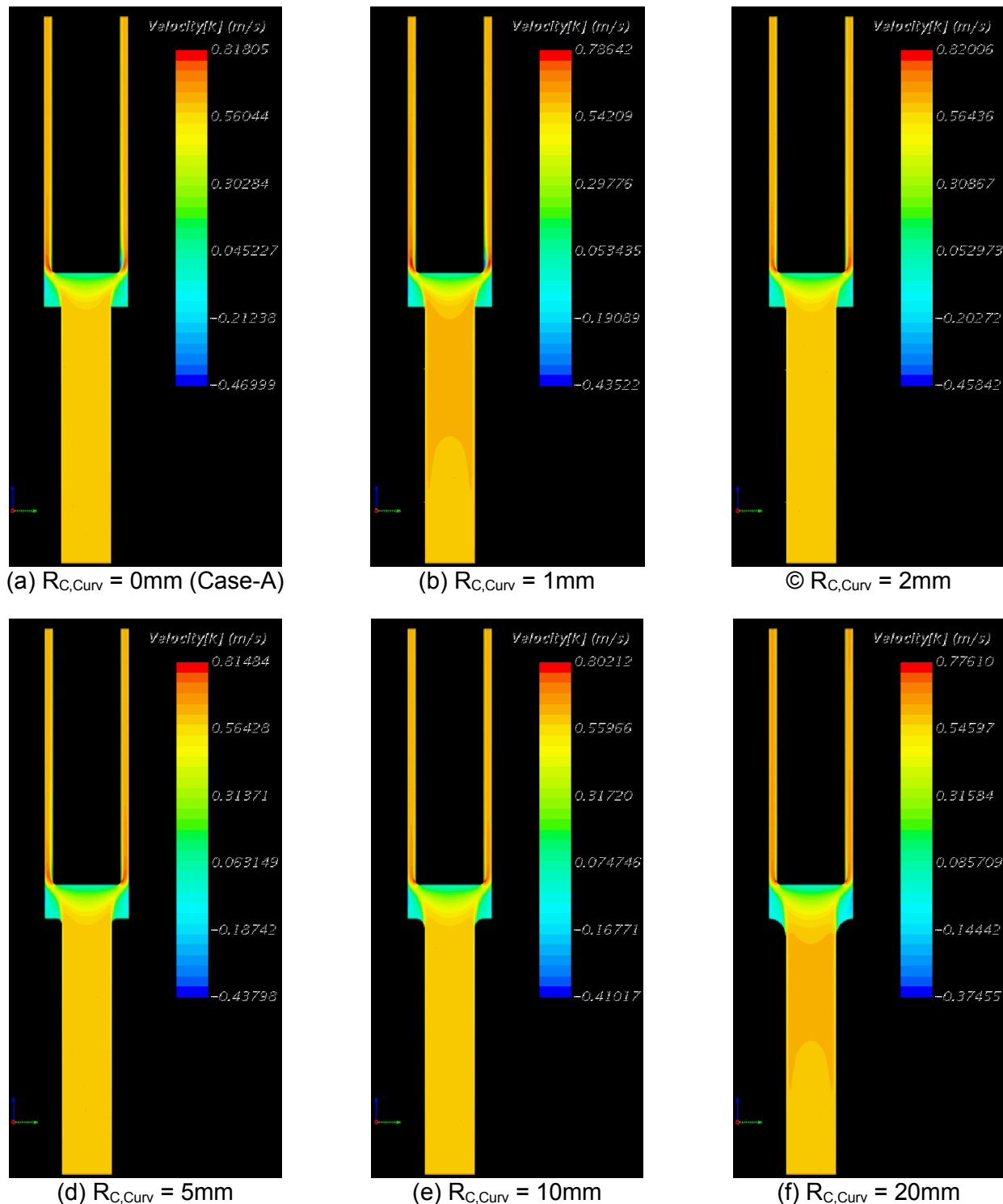


Figure B.6. Velocity distributions on the mid-plane of the channel (Case-B, $Re_D = 1 \times 10^5$).

Appendix C. THE STAR-CCM+ PRESSURE DISTRIBUTION RESULTS

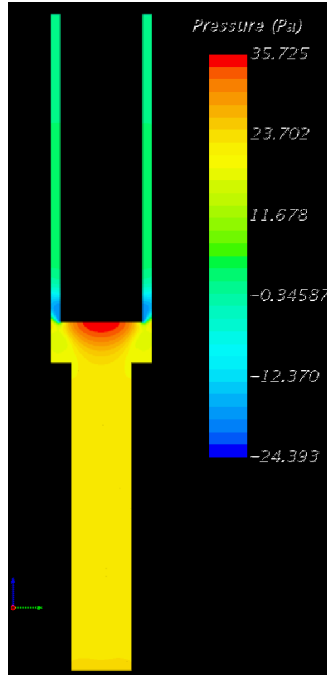
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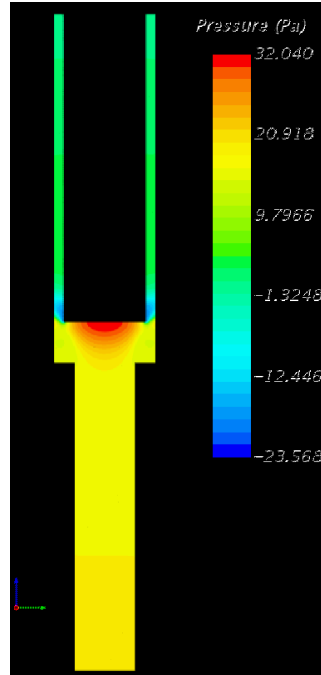
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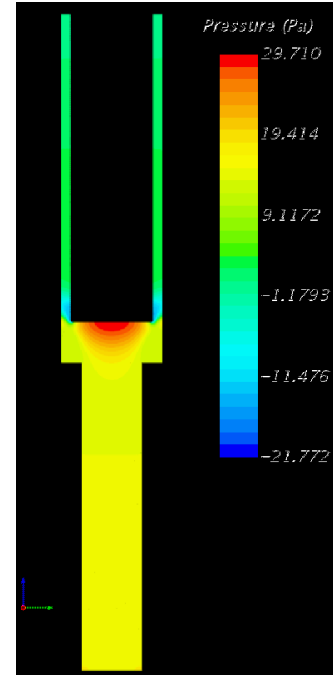
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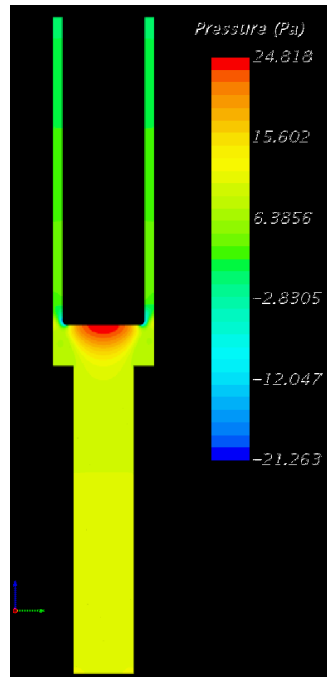
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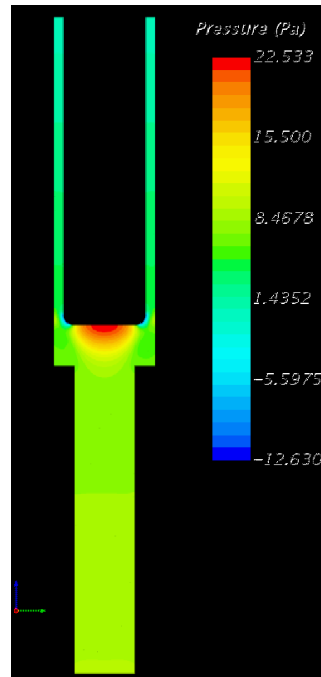
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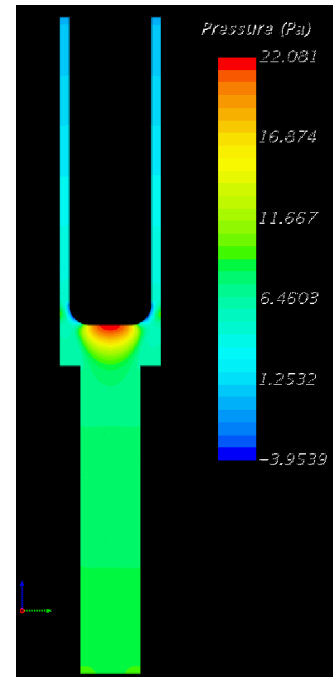
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(e) $R_{A,Curv} = 10\text{mm}$



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Figure C.1. Pressure distributions on the mid-plane of the channel (Case-A, $Re_D = 3 \times 10^4$).

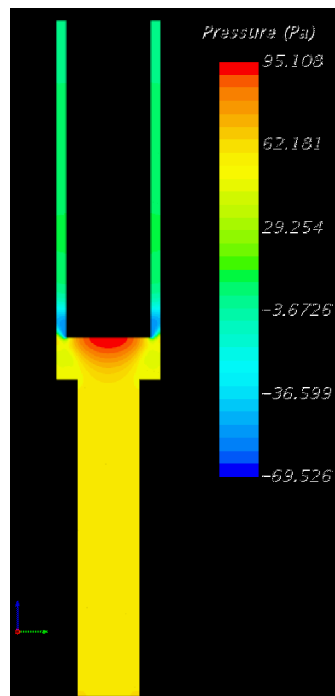
Title: Computational Evaluation on Effect of Edge-rounding in Duct with Cross-section varying from Circle to Annulus

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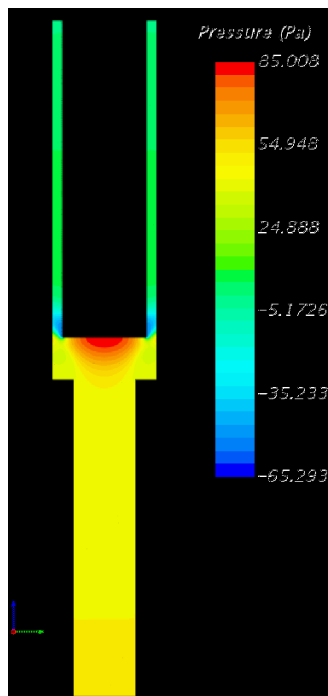
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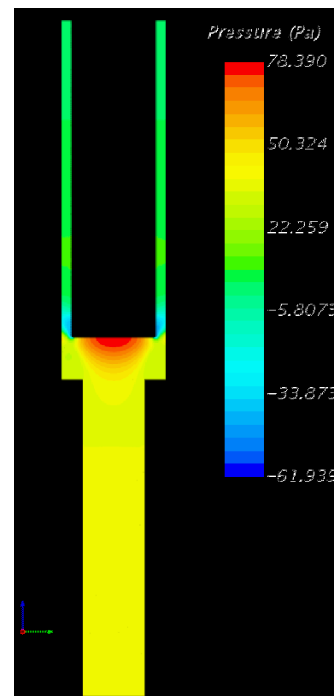
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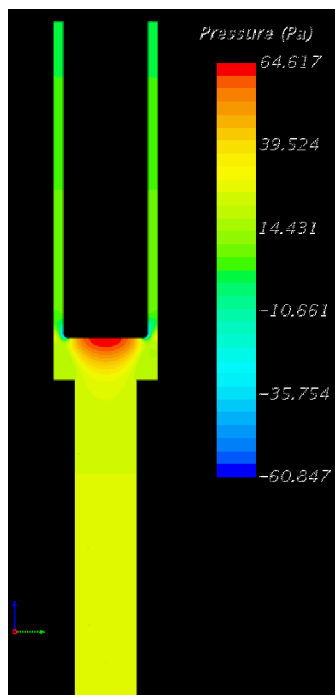
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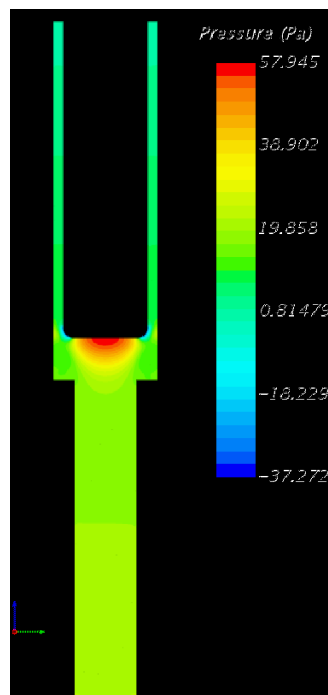
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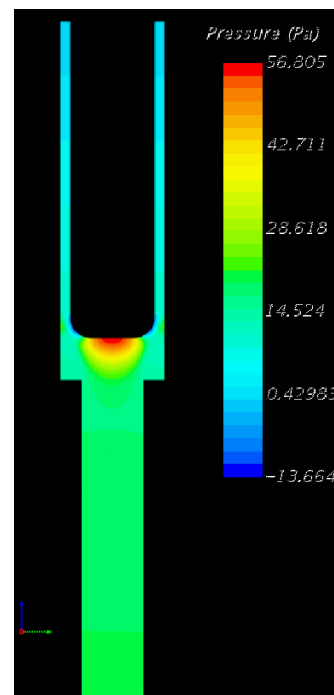
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(e) $R_{A, Curv} = 10\text{mm}$



(f) $R_{A, Curv} = 20\text{mm}$

Figure C.2. Pressure distributions on the mid-plane of the channel (Case-A, $Re_D = 5 \times 10^4$)

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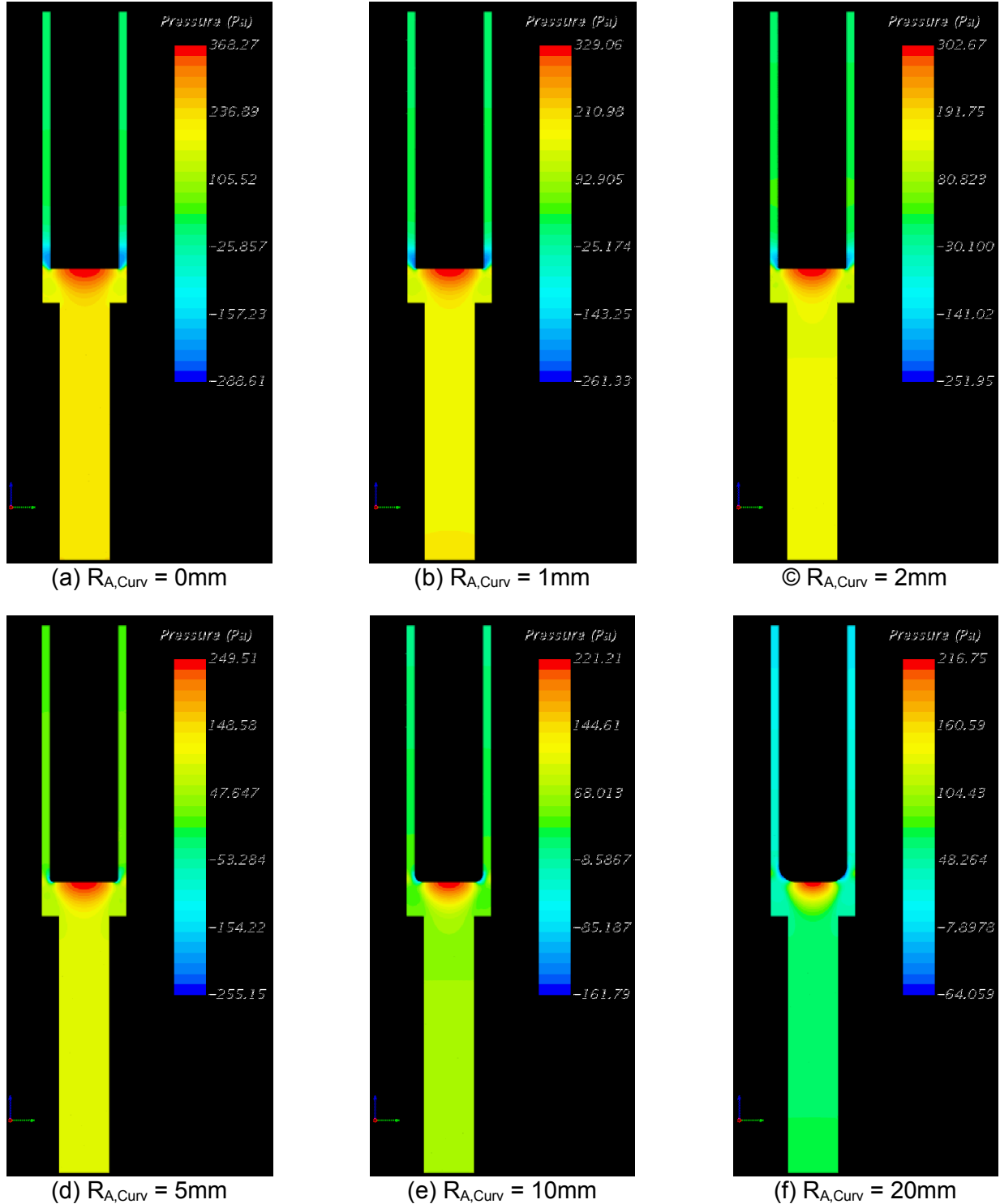
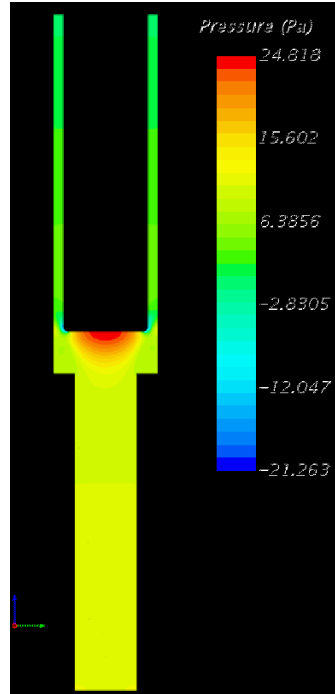


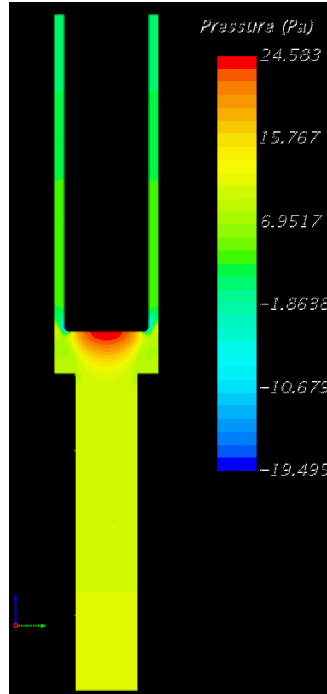
Figure C.3. Pressure distributions on the mid-plane of the channel (Case-A, $Re_D = 1 \times 10^5$).

Title: Computational Evaluation on Effect of Edge-rounding in Duct with Cross-section varying from Circle to Annulus

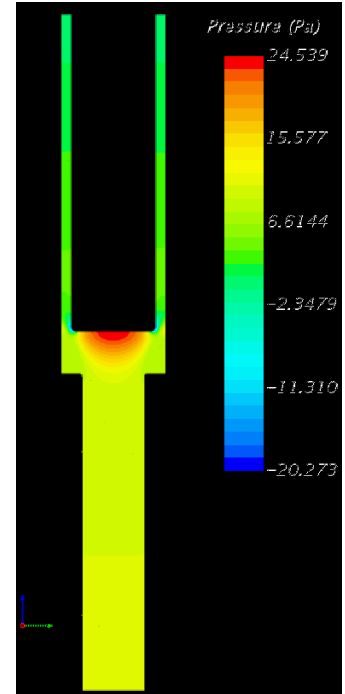
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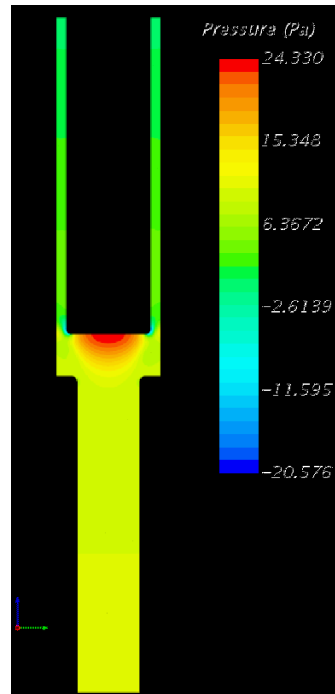
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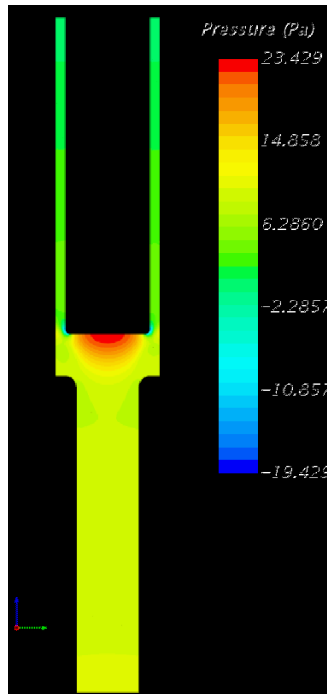
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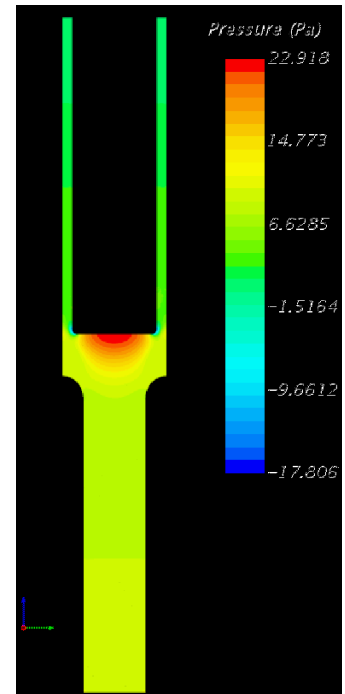
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(d) $R_{C, Curv} = 5\text{mm}$



(e) $R_{C, Curv} = 10\text{mm}$



(f) $R_{C, Curv} = 20\text{mm}$

Figure C.4. Pressure distributions on the mid-plane of the channel (Case-B, $Re_D = 3 \times 10^4$).

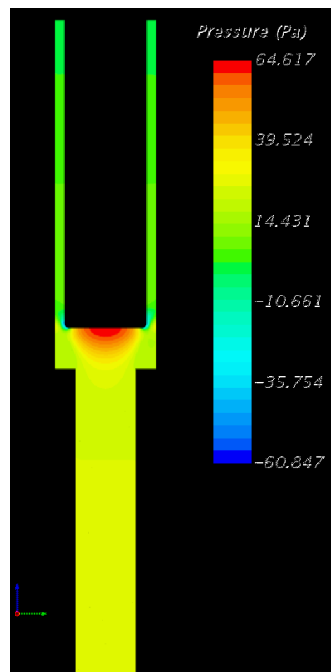
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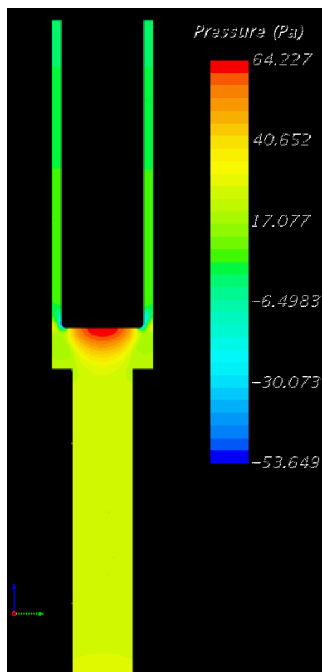
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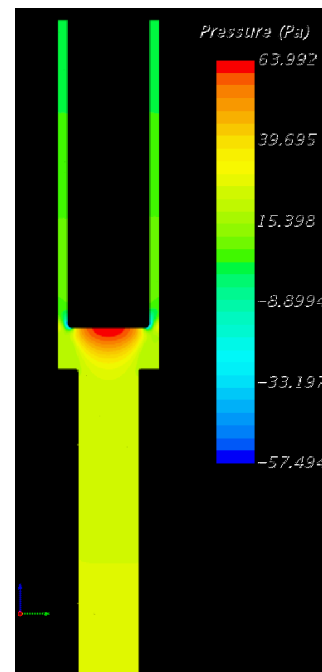
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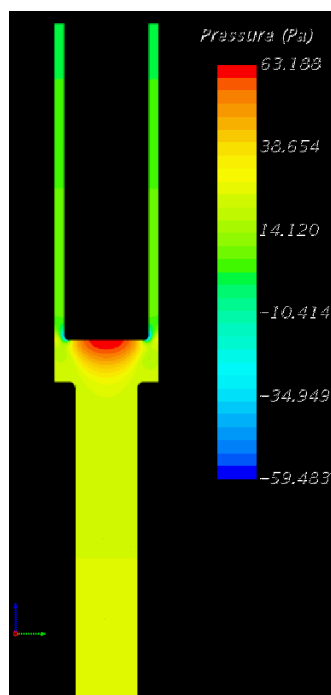
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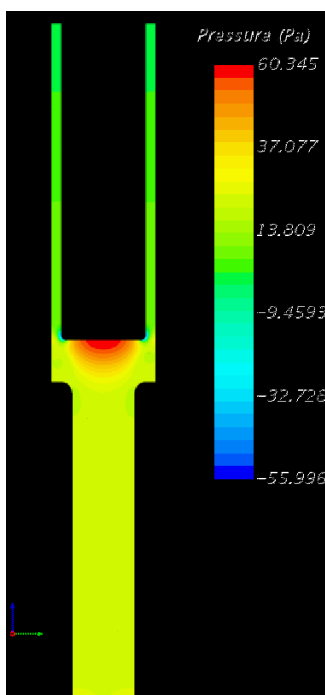
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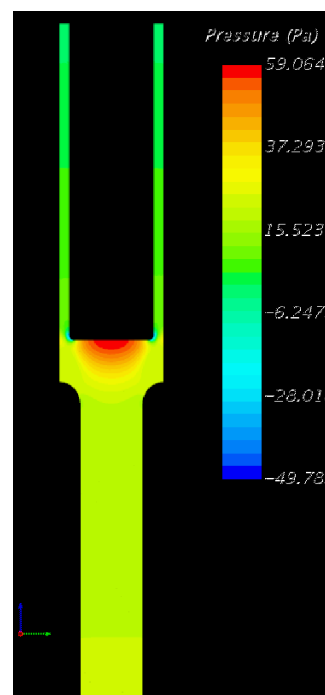
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(e) $R_{C, Curv} = 10\text{mm}$



(f) $R_{C, Curv} = 20\text{mm}$

Figure C.5. Pressure distributions on the mid-plane of the channel (Case-B, $Re_D = 5 \times 10^4$)

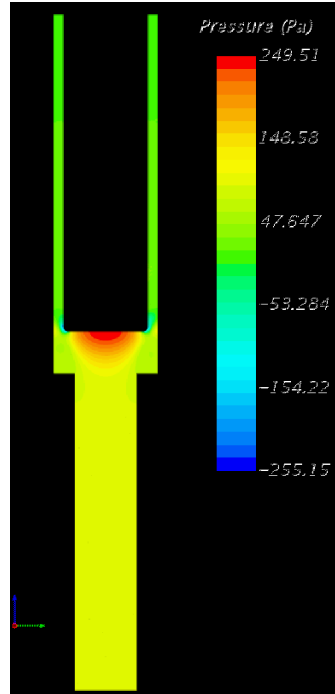
Title: Computational Evaluation on Effect of Edge-rounding in Duct with Cross-section varying from Circle to Annulus

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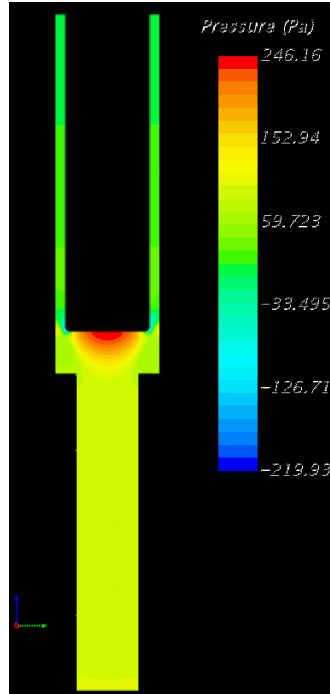
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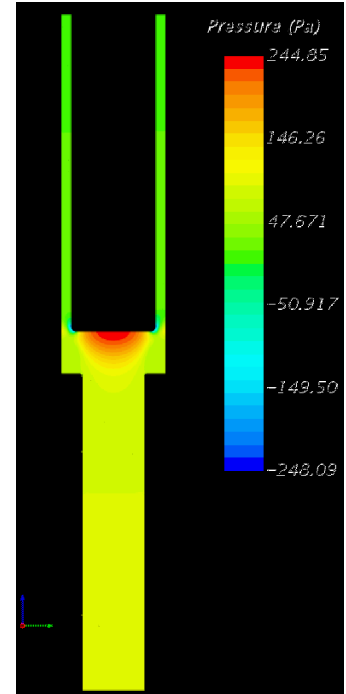
Date: TBD



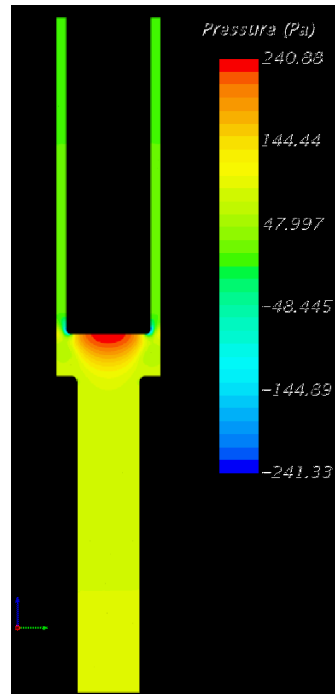
(a) $R_{C, Curv} = 0\text{mm}$ (Case-A)



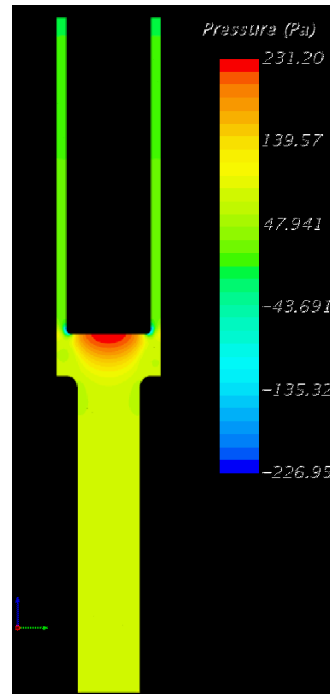
(b) $R_{C, Curv} = 1\text{mm}$



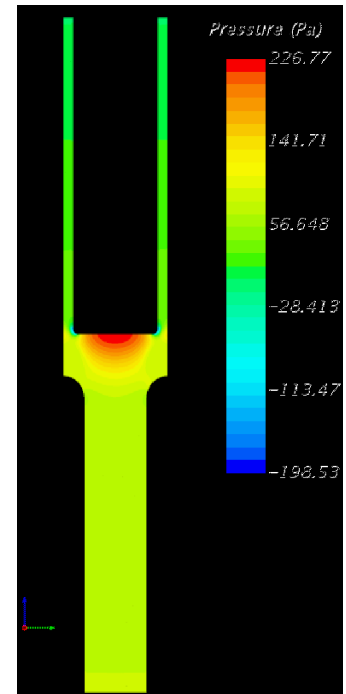
(c) $R_{C, Curv} = 2\text{mm}$



(d) $R_{C, Curv} = 5\text{mm}$



(e) $R_{C, Curv} = 10\text{mm}$



(f) $R_{C, Curv} = 20\text{mm}$

Figure C.6. Pressure distributions on the mid-plane of the channel (Case-B, $Re_D = 1 \times 10^5$).

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Appendix D. THE STAR-CCM+ PRESSURE DROP RESULTS

Table D.1. CFD Results of Pressure Drop (Case-A)

Case-A	Pressure drop (Pa)						
Re number $R_{A, Curv}$ (mm)	2.00E+04	3.00E+04	4.00E+04	5.00E+04	7.50E+04	1.00E+05	2.12E+06
0	10.22	21.21	36.18	55.54	121.76	212.16	88961.72
1	8.54	17.52	29.70	45.49	99.48	173.06	54486.27
2	7.51	15.19	25.57	38.91	84.99	146.72	46879.34
5	5.34	10.36	16.98	25.40	54.36	94.16	24252.13
10	4.37	8.07	12.78	18.69	39.55	65.92	20355.14
20	4.12	7.63	11.95	17.54	36.93	61.28	19973.94

Table D.2. CFD Results of Pressure Drop (Case-B)

Case-B	Pressure drop (Pa)						
Re number $R_{C, Curv}$ (mm)	2.00E+04	3.00E+04	4.00E+04	5.00E+04	7.50E+04	1.00E+05	2.12E+06
0	5.34	10.36	16.98	25.40	54.36	94.16	24252.13
1	5.29	10.13	16.52	24.91	53.75	90.79	22735.15
2	5.23	10.07	16.34	24.75	53.50	89.33	22277.10
5	5.13	9.87	15.87	23.88	51.57	85.19	22005.33
10	4.79	8.98	14.29	21.11	45.69	75.74	20717.10
20	4.60	8.46	13.34	19.81	42.15	71.55	20188.43

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Appendix E. NEK5000 AVERAGED VELOCITY AND PRESSURE DISTRIBUTIONS

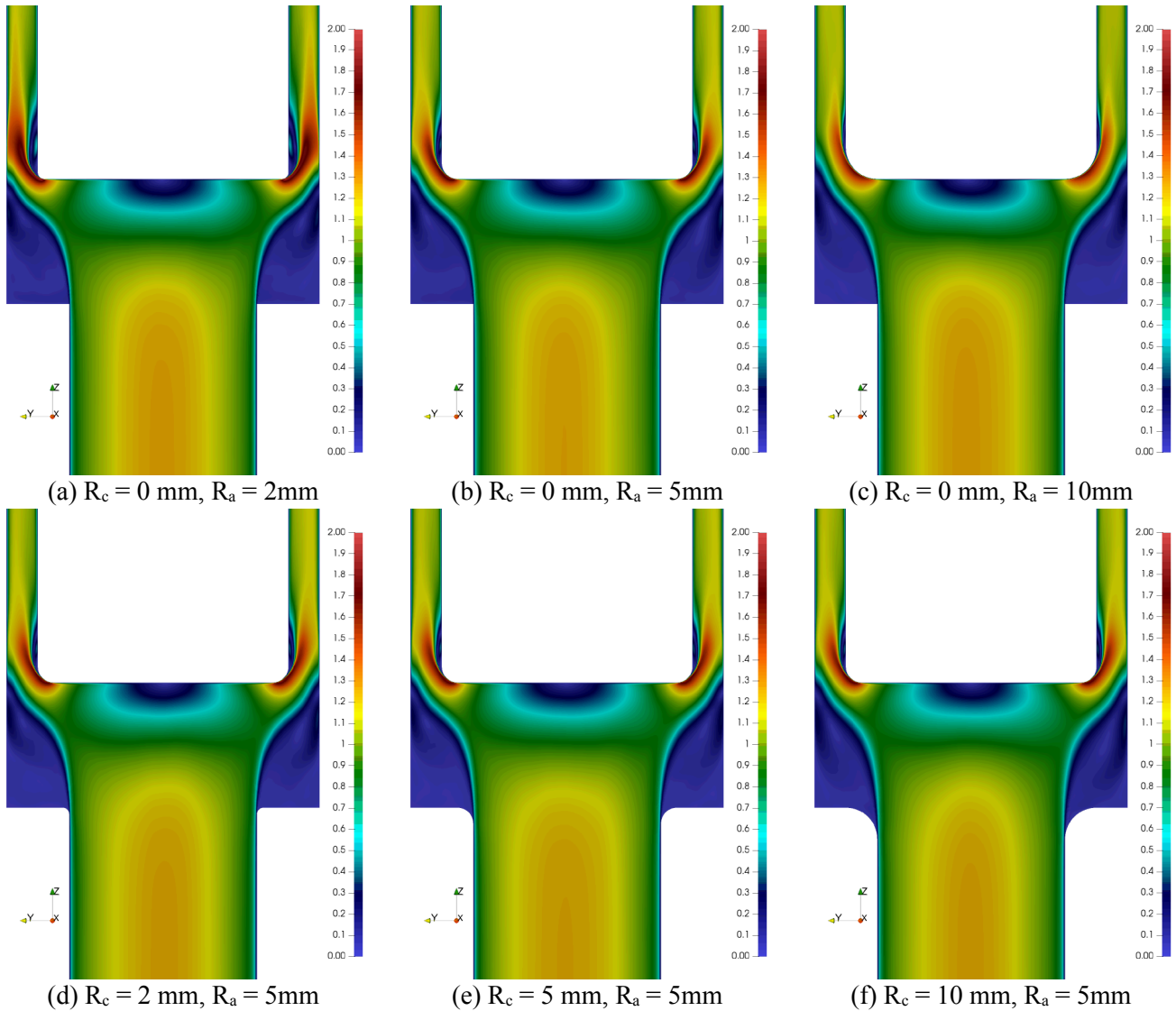


Figure E.1. Time-averaged velocity magnitude distributions across a midplane slice through the transition region at $Re=20,000$ for different edge radii.

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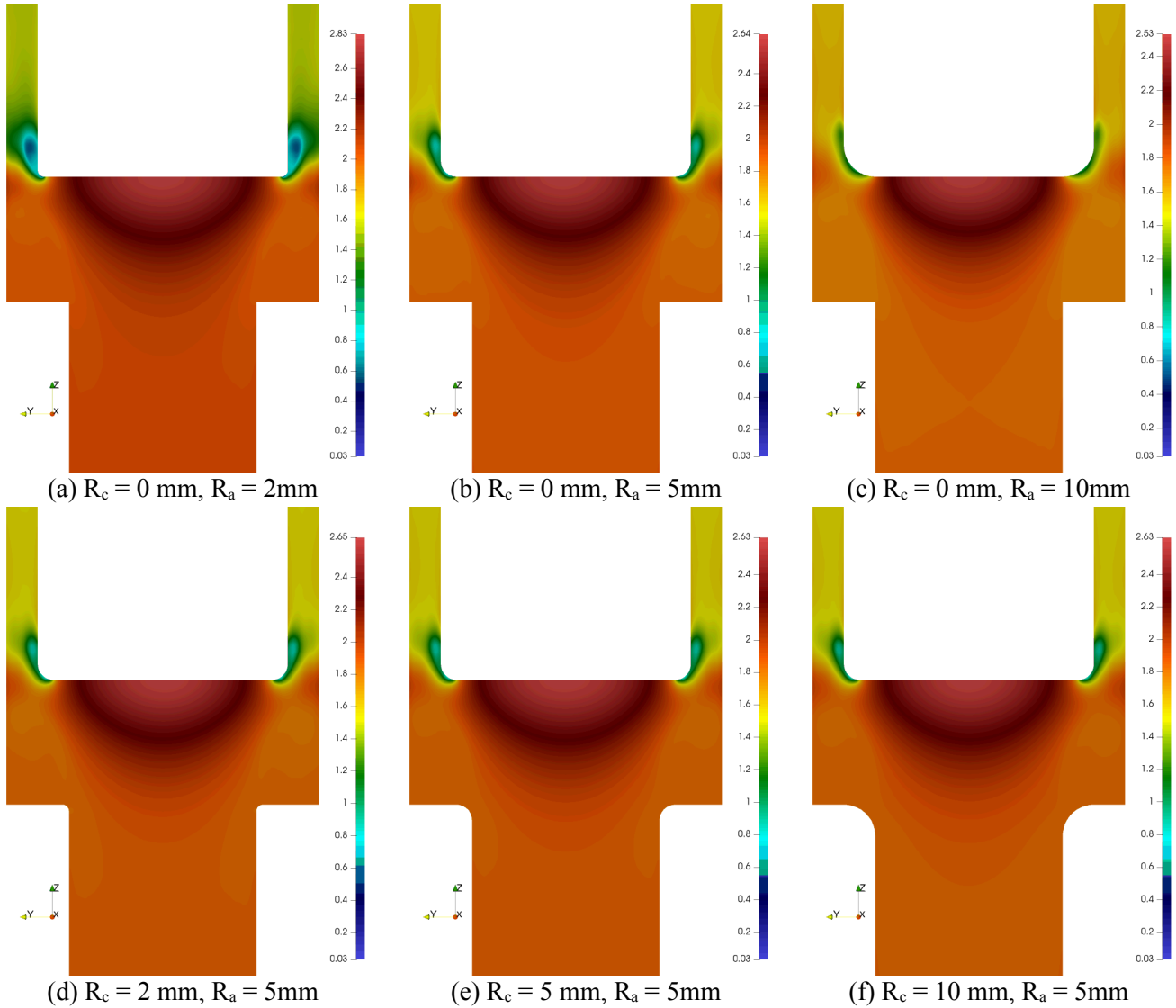


Figure E.2. Time-averaged pressure distributions across a midplane slice through the transition region at $Re=20,000$ for different edge radii.