

Visually Determining the Thermal Expansion of a Triple Bubbler System in Pyroprocessing Molten Salt

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Visually Determining the Growth and Expansion of a Triple Bubble Defect in Pyroprocessing Molten Salt

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OUTLINE

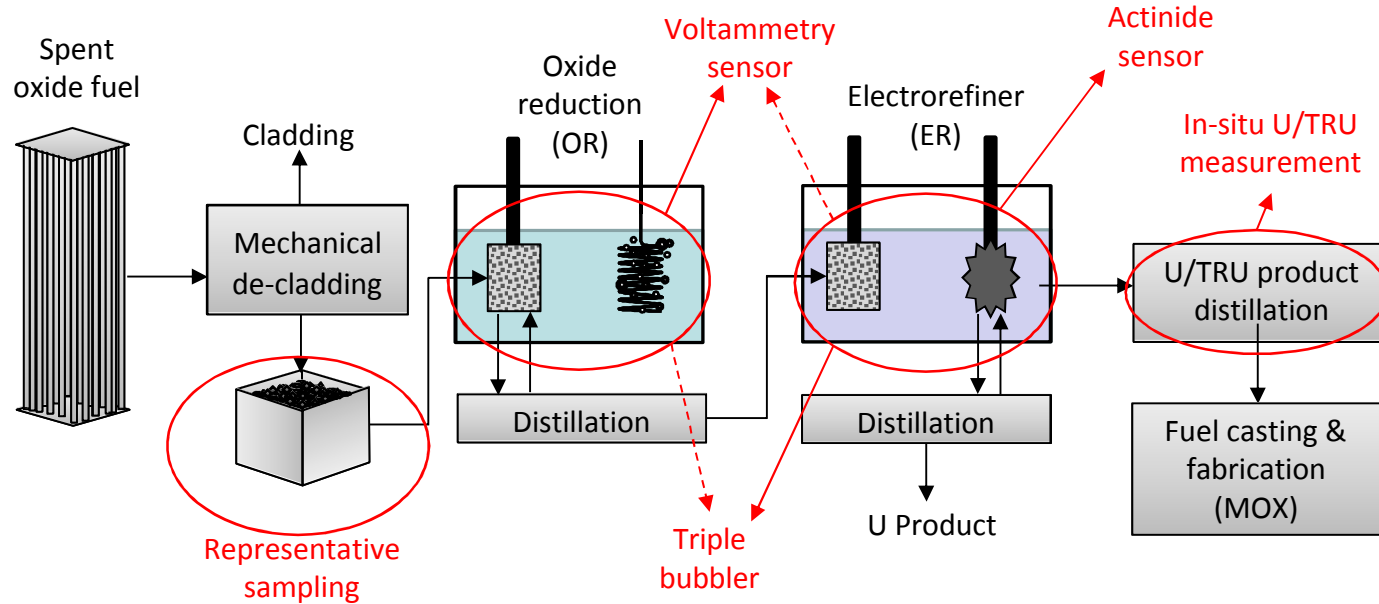
- Background
- Motivation
- Approach
- Experimental Setup and Math
- Results and Analysis
- Conclusions
- Future work



PYROPROCESSING

○ Key locations for process monitoring and material accountability.

-----> Other efforts (INL and other Labs).



BACKGROUND

- Nuclear material accountancy (NMA) is pivotal in pyroprocessing.
- Process monitoring (PM) of electrorefiner (ER) constituents.
- Double bubbler assemblies are currently used in aqueous processes.



MOTIVATION

- Two main challenges to overcome in order to implement the bubbler successfully in the ER
 - Thermal expansion
 - Calibration of probe



APPROACH

- Visual measurements
- Calibration with multiple salts



EXPERIMENTAL SETUP



THIRD TUBE
10CM ABOVE LOWER
TUBES PROVIDES
MEASUREMENT OF
FLUID DENSITY

SMALL BULKHEADS
TO PREVENT BUBBLES FROM LOWER
TUBES IMPINGING ON UPPER TUBE

HOLES IN BULKHEADS
GUIDE KOVAR TUBES
BUT ARE NOT FIXED TO THEM
ALLOWING FOR DIFFERENTIAL
THERMAL EXPANSION OF
SST SHROUD

TWO TUBES FOR SUBMERGENCE PRESSURE
DIFFERENT SIZES ALLOW CORRECTION FOR
SURFACE TENSION

THREE SUBMERGED
TUBES ARE KOVAR
ALLOY - VERY LOW
THERMAL EXPANSION

HANDLING FITTING
FOR IN-CELL USE

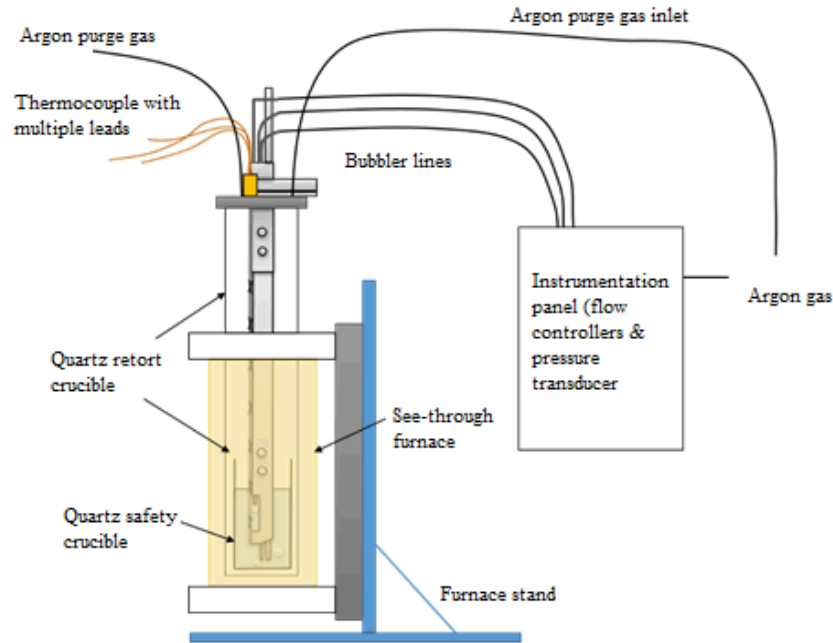
SHORT TUBE TO
MEASURE PRESSURE
IN SHROUD

MACOR GLASS
INSULATOR PLATE
AND BUSHING

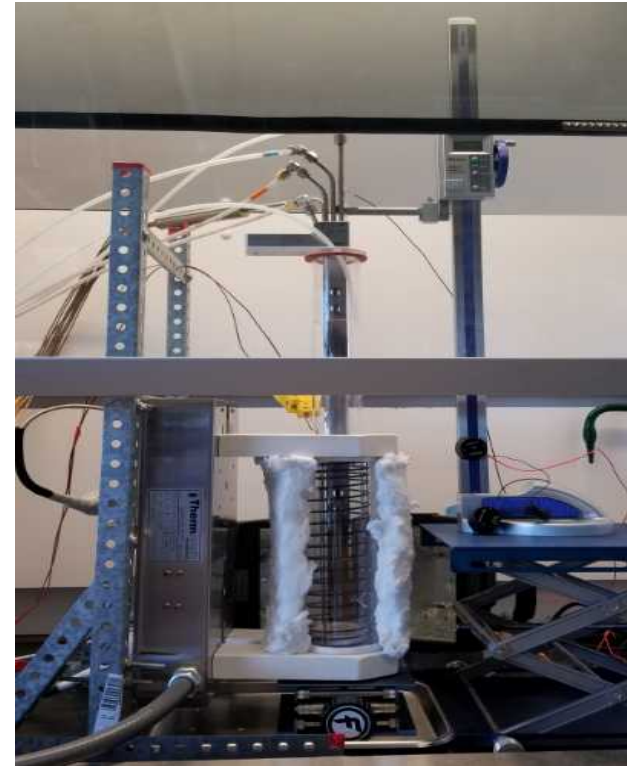
HOLES IN SHROUD
TO ALLOW MEASURING
STATIC PRESSURE IN
ER

SPRAY CERAMIC COATING
THROUGH BAFFLE AREA





Transparent Tube Furnace Schematic



Transparent Tube Furnace





Oxygen Two-Zone Furnace



Pressure and Mass Control Board



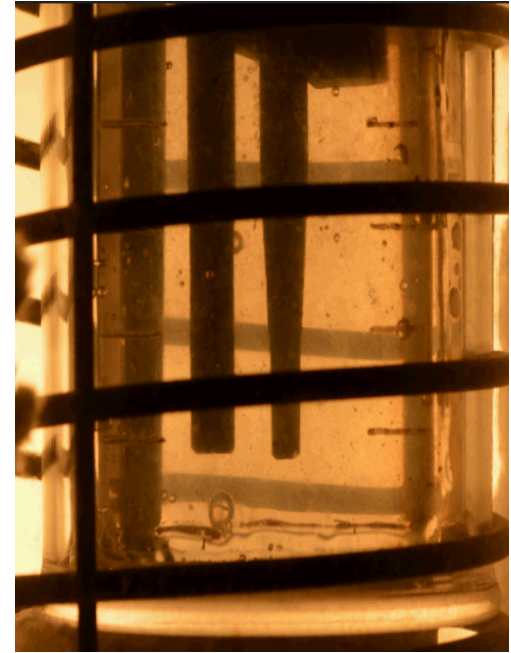
Bubbler in Molten LiCl-KCl Eutectic



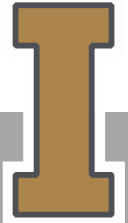
450°C



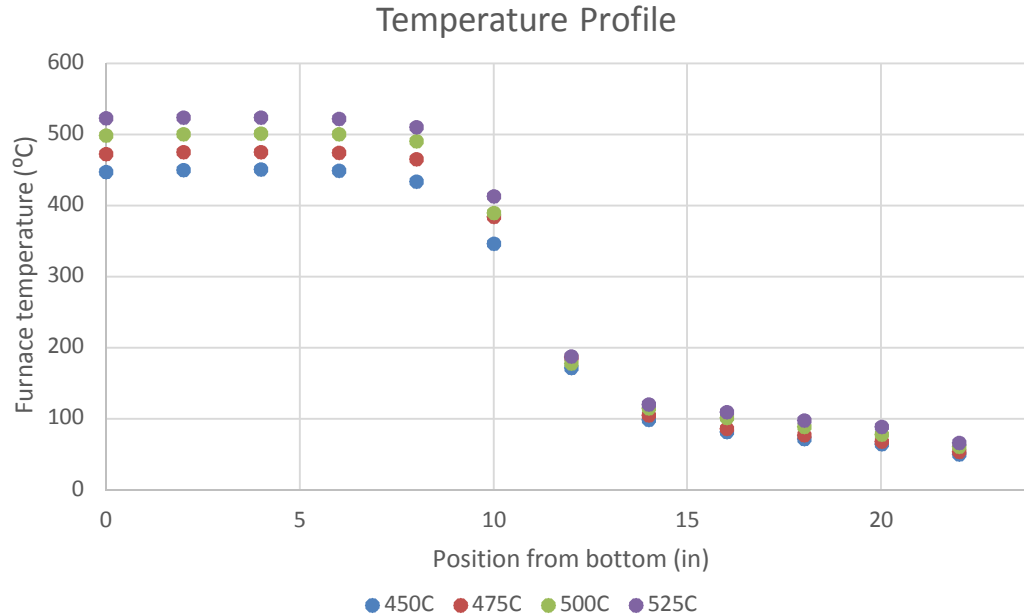
475°C



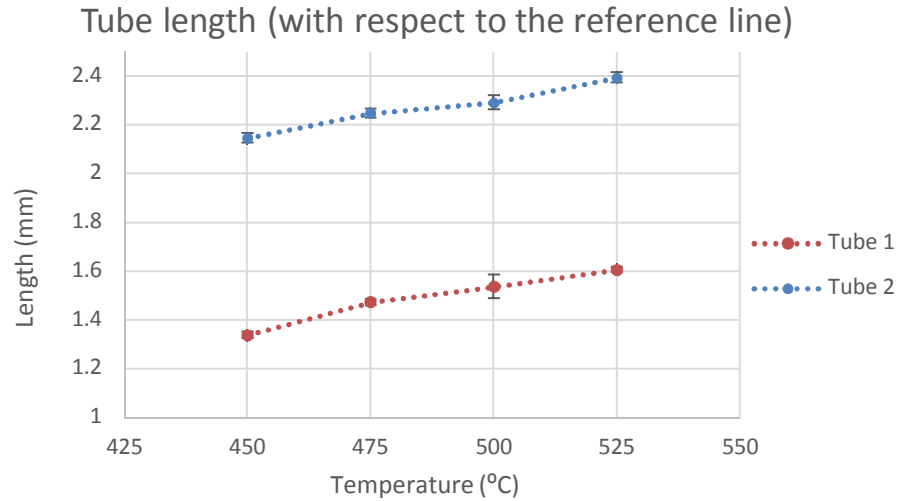
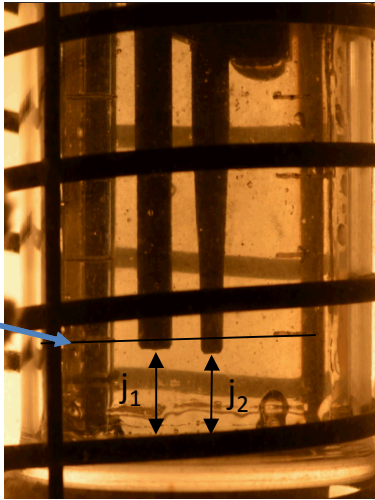
525°C



RESULTS: Transparent Tube Furnace



Reference
line

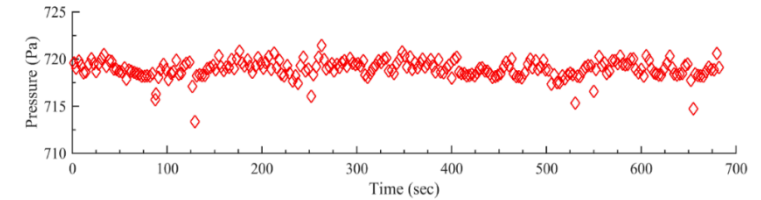
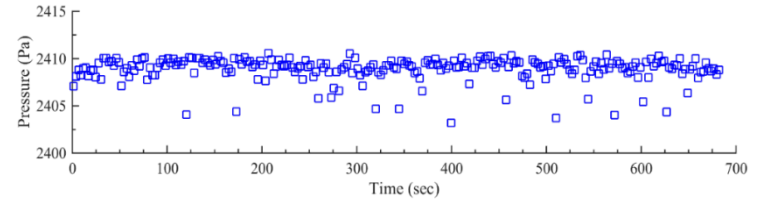
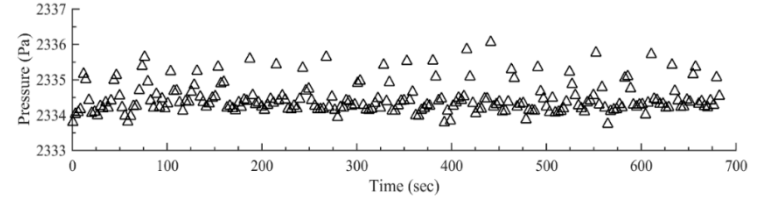
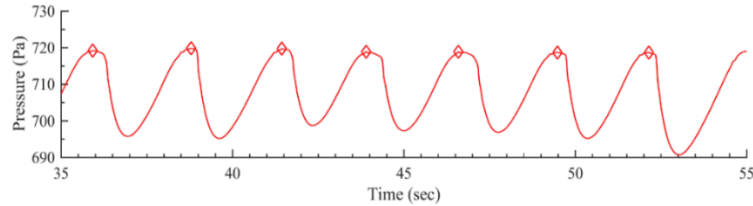
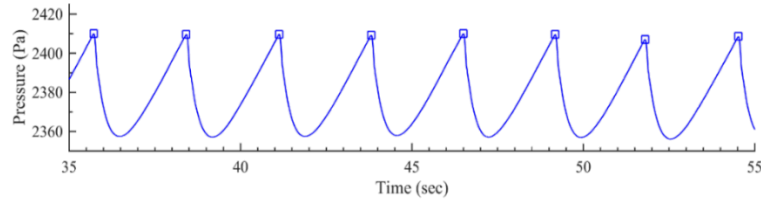
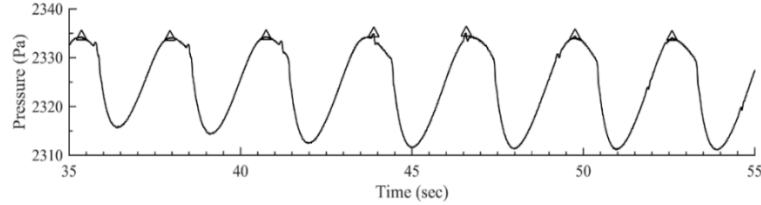


Thermal expansion in bubbler tubes

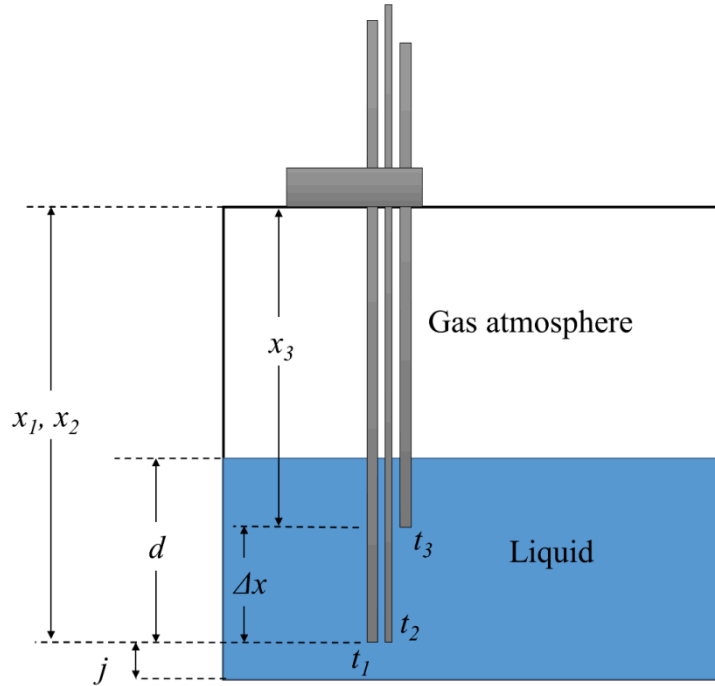
°C	Visually Observed		Expected (calculated)		% diff (j_1)	% diff (j_2)
	j_1 (mm)	j_2 (mm)	j_1 (mm)	j_2 (mm)		
450	10.10 ± 0.13	9.34 ± 0.13	9.81 ± 0.09	9.20 ± 0.09	-2.95	-1.52
475	9.98 ± 0.13	9.26 ± 0.13	9.75 ± 0.10	9.14 ± 0.10	-2.30	-1.36
500	9.93 ± 0.13	9.21 ± 0.13	9.66 ± 0.10	9.05 ± 0.10	-2.72	-1.80
525	9.85 ± 0.13	9.11 ± 0.13	9.58 ± 0.11	8.97 ± 0.11	-2.78	-1.58



Bubbler Pressure Data



MATHEMATICAL MODEL



$$\rho = C_P \frac{P_1 - P_3}{g \Delta x}$$

$$\gamma = \alpha \frac{P_2 - P_1 + 0.69 r_1 g \rho}{1000}$$

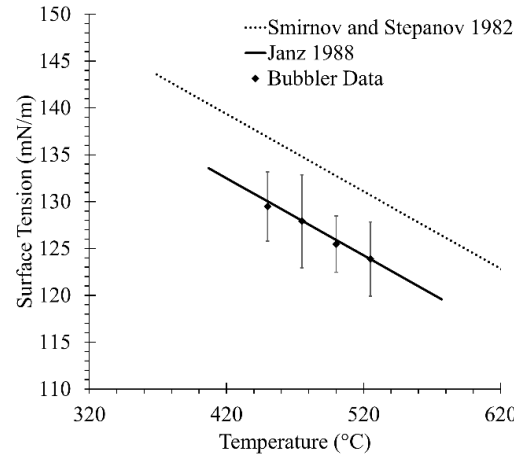
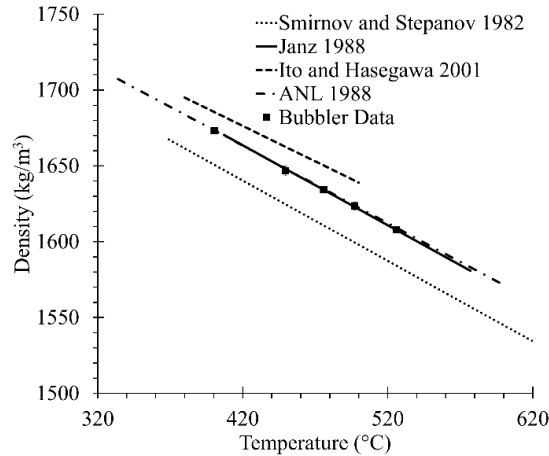
$$d = \frac{P_1 - P_B}{g \rho}$$

$$P_B = \frac{2}{3} \rho g r_1 + \frac{2\gamma}{r_1}$$

$$D = d + j_1$$



Calibration in LiCl-KCl Eutectic



T (°C)	C_p	α
456.4	1.0015 ± 0.0018	1.260 ± 0.026
475.7	1.0012 ± 0.0022	1.260 ± 0.035
505.2	1.0019 ± 0.0020	1.260 ± 0.022
524.7	1.0015 ± 0.0022	1.264 ± 0.029
Average	1.0015 ± 0.0020	1.261 ± 0.028
Std	0.0002	0.005

Note: In aqueous testing $C_p = 1.0017$
and $\alpha = 1.16$

Bubbler determined depth matches within 0.4%!

T (°C)	Density (kg/m³)	Surface Tension (mN/m)	Measured Depth (mm)	Calculated Depth (mm)	% Difference
456.4	1644.3 ± 4.2	129.5 ± 3.7	148.56 ± 0.04	148.2 ± 0.4	0.22
475.7	1634.2 ± 5.2	127.9 ± 5.0	149.26 ± 0.05	148.9 ± 0.5	0.27
505.2	1618.6 ± 4.5	125.5 ± 3.0	150.33 ± 0.05	149.8 ± 0.5	0.36
524.7	1608.3 ± 4.9	123.9 ± 4.0	151.42 ± 0.04	150.8 ± 0.5	0.39



Validation

Transparent Furnace Data

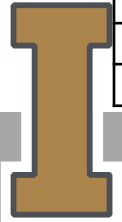
- LiCl-KCl eutectic.
- No contact sensor data.

T (°C)	$\rho^\dagger$ (kg/m ³)	ρ (kg/m ³ , Bubbler)	% diff.	$\gamma^\dagger$ (mN/m)	γ (mN/m, Bubbler)	% diff.	Depth (mm, Bubbler)
400.4	1673.78	1674.9 ± 3.9	-0.07	134.10	130.1 ± 3.9	3.01	150.1 ± 0.3
449.5	1647.96	1647.6 ± 4.9	0.02	130.06	128.1 ± 3.9	1.52	152.6 ± 0.5
475.8	1634.07	1634.5 ± 4.4	-0.03	127.89	123.9 ± 4.1	3.15	154.1 ± 0.4
497.3	1622.77	1623.3 ± 4.6	-0.04	126.12	121.1 ± 4.5	4.07	155.5 ± 0.4
526.0	1607.62	1607.0 ± 4.3	0.04	123.75	119.7 ± 4.0	3.35	156.8 ± 0.4

Two-Zone Furnace Data

- CsCl-LiCl eutectic.
- Property values interpolated/extrapolated.
- Contact sensor potentially biased by the salt meniscus (~0.3 to ~0.8 mm).

T (°C)	$\rho^\dagger$	$\rho^\dagger$	ρ (Bubbler)	$\gamma^\dagger$	γ (Bubbler)	D (Measured)	D (Bubbler)	Residual	% diff.
422.5	2450.92	2420.11	2428.1 ± 6.0	112.40	131.0 ± 3.6	149.06 ± 0.10	148.5 ± 0.4	0.52	0.35
456.6	2426.30	2391.83	2399.7 ± 6.1	109.78	124.4 ± 4.5	151.59 ± 0.10	150.7 ± 0.4	0.88	0.58
476.8	2411.68	2375.04	2382.9 ± 6.3	108.23	123.7 ± 3.3	152.45 ± 0.12	151.2 ± 0.4	1.24	0.82
498.7	2395.87	2356.88	2364.7 ± 6.5	106.55	122.0 ± 3.2	152.94 ± 0.10	151.8 ± 0.4	1.12	0.73
523.6	2377.94	2336.29	2343.8 ± 6.7	104.63	122.1 ± 3.8	154.09 ± 0.11	153.0 ± 0.5	1.12	0.73



FUTURE WORK

- Fundamental Studies
 - Explore different salts, compositions and wider temperature range
 - Explore ER calibration approaches
- Future Directions
 - Adapt/modify bubbler for reduction in material holdup & corrosion



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