



Use of Novel Diglycolamide Extractants in Liquid-liquid Separations of Light Rare Earths

March 2022

Changing the World's Energy Future

Addyson Lyn Barnes, Ramedy G Flores, Mitchell Greenhalgh, Kevin L Lyon, Santa Jansone-Popova, Bruce Moyer, Mac Foster



DISCLAIMER

This information was prepared as an account of work sponsored by an agency of the U.S. Government. Neither the U.S. Government nor any agency thereof, nor any of their employees, makes any warranty, expressed or implied, or assumes any legal liability or responsibility for the accuracy, completeness, or usefulness, of any information, apparatus, product, or process disclosed, or represents that its use would not infringe privately owned rights. References herein to any specific commercial product, process, or service by trade name, trade mark, manufacturer, or otherwise, does not necessarily constitute or imply its endorsement, recommendation, or favoring by the U.S. Government or any agency thereof. The views and opinions of authors expressed herein do not necessarily state or reflect those of the U.S. Government or any agency thereof.

Use of Novel Diglycolamide Extractants in Liquid-liquid Separations of Light Rare Earths

**Addyson Lyn Barnes, Ramedy G Flores, Mitchell Greenhalgh, Kevin L Lyon,
Santa Jansone-Popova, Bruce Moyer, Mac Foster**

March 2022

**Idaho National Laboratory
Idaho Falls, Idaho 83415**

<http://www.inl.gov>

**Prepared for the
U.S. Department of Energy
Under DOE Idaho Operations Office
Contract DE-AC07-05ID14517**

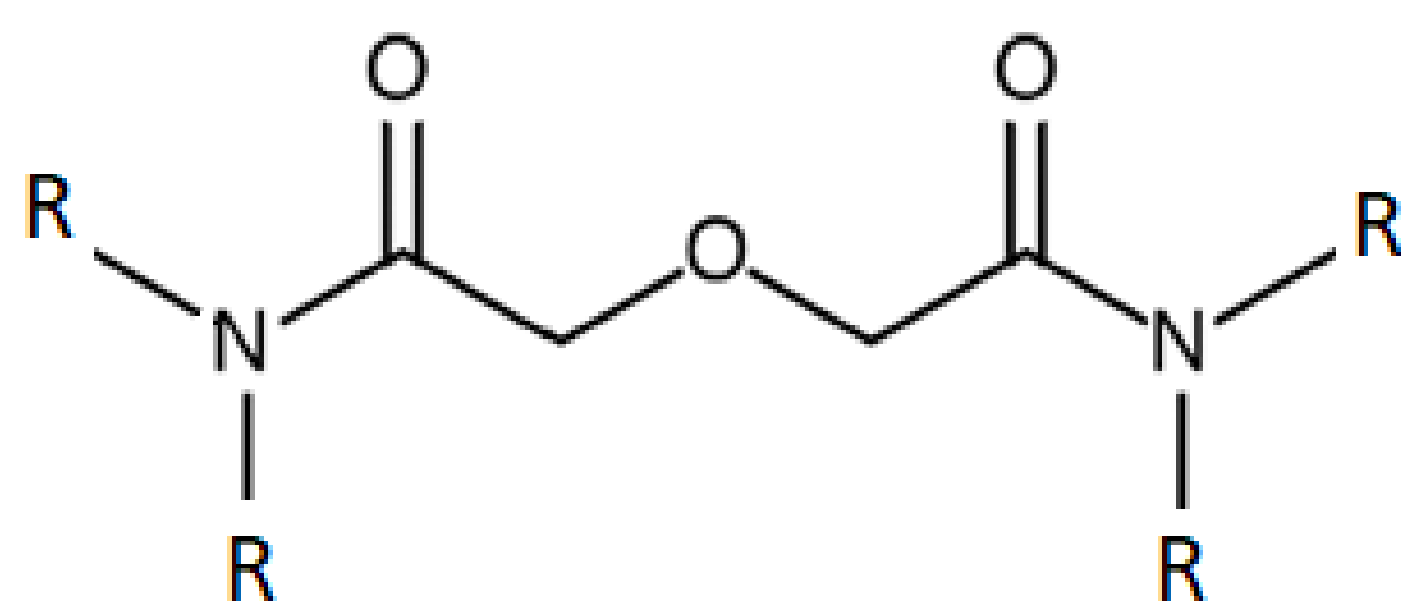
1.2.14 Use of Novel Diglycolamide Extractants in Liquid-Liquid Separations of Light Rare Earths

Addyson Barnes¹, Santa Jansone-Popova², Mac Foster³, Ramedy Flores¹, Mitch Greenhalgh¹, Bruce Moyer², Kevin Lyon¹

¹Idaho National Laboratory, Idaho Falls, ID 83415, ²Oak Ridge National Laboratory, Oak Ridge, TN 37831, ³Marshallton Research Laboratories, Tobaccoville, NC 27050

Background

- Modified diglycolamide (DGA) extractants show high affinity for lanthanides and improved separation factors compared to phosphonic acids used commercially.
- Previous studies with DGAs include flowsheet design and implementation into solvent extraction equipment but at low extractant concentration.
- Current efforts focus on developing another novel DGA with different alkyl chains that can extract light rare earths using a higher ligand concentration than previous DGAs, creating a more competitive product for light rare earth separation.

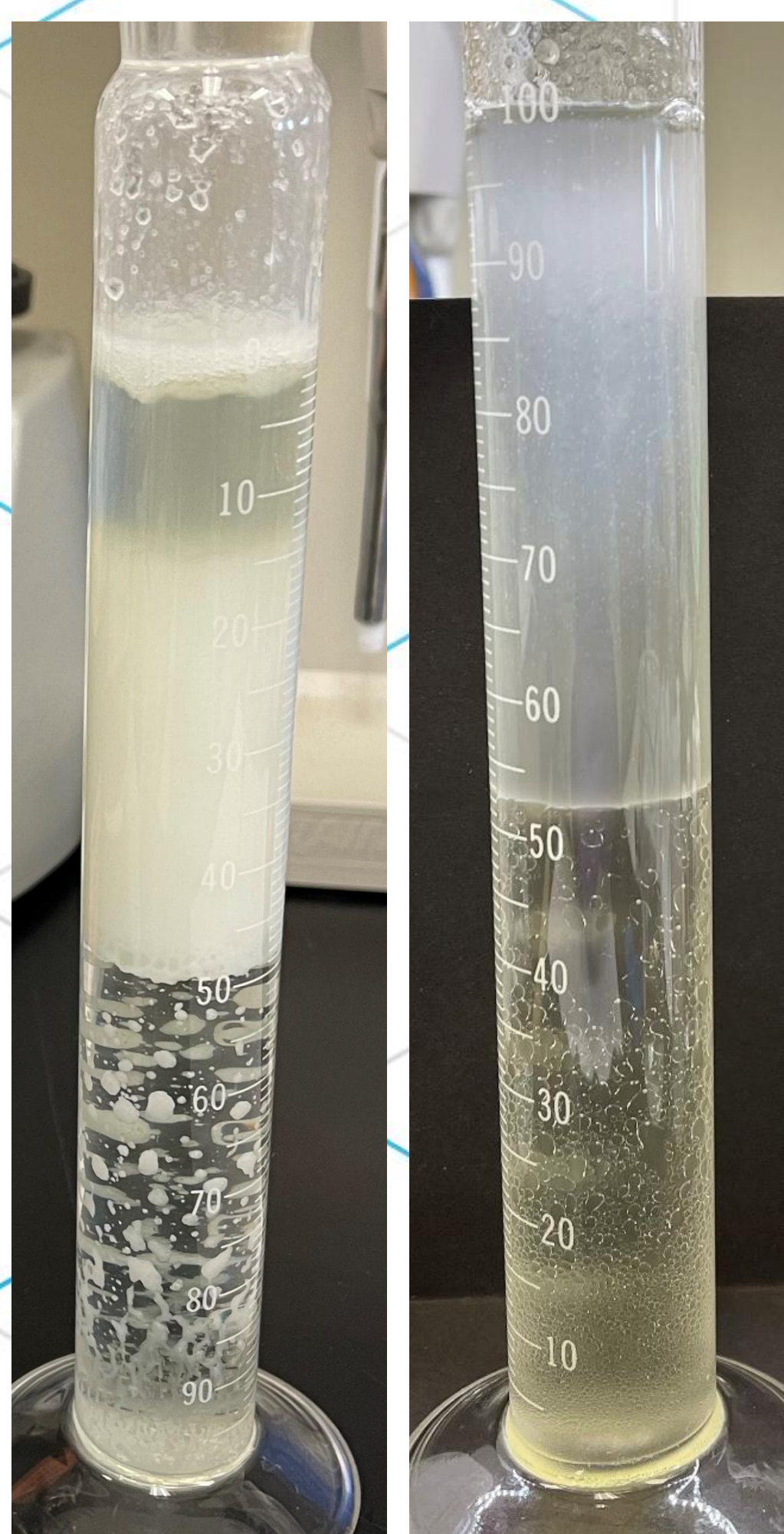


- The scope of this project is to test a recently developed DGA (DGA-6) for application in solvent extraction equipment.
- Evaluation includes dispersion testing, preliminary flowsheet design to determine an organic to aqueous phase ratio (O/A), and an acid dependency study.

Dispersion Testing

- Provides insight into aqueous/organic pair compatibility with solvent extraction equipment
- Extractant is mixed with a simulated leach liquor containing La, Ce, Nd, and Pr. The break time and interfacial heights are used to quantify the dispersion number.
- Problematic gelling of the extractant can occur with heavy metal loading, higher DGA concentrations, and at larger scales.

Determining an adequate DGA concentration:



- DGA concentration was decreased until a fair dispersion rating or better was achieved in a batch contact with the simulated leach liquor.
- Final extractant composition: 0.25 M DGA with 5v% Exxal-13 in Isopar-L

DGA-6 Concentration	Dispersion Number Rating
0.5 M – small scale	Fair
0.5 M – large scale	Gel Formation
0.4 M – small scale	Good
0.4 M – large scale	Gel Formation
0.3 M – large scale	Poor
0.25 M – small scale	Fair
0.25 M – large scale	Good

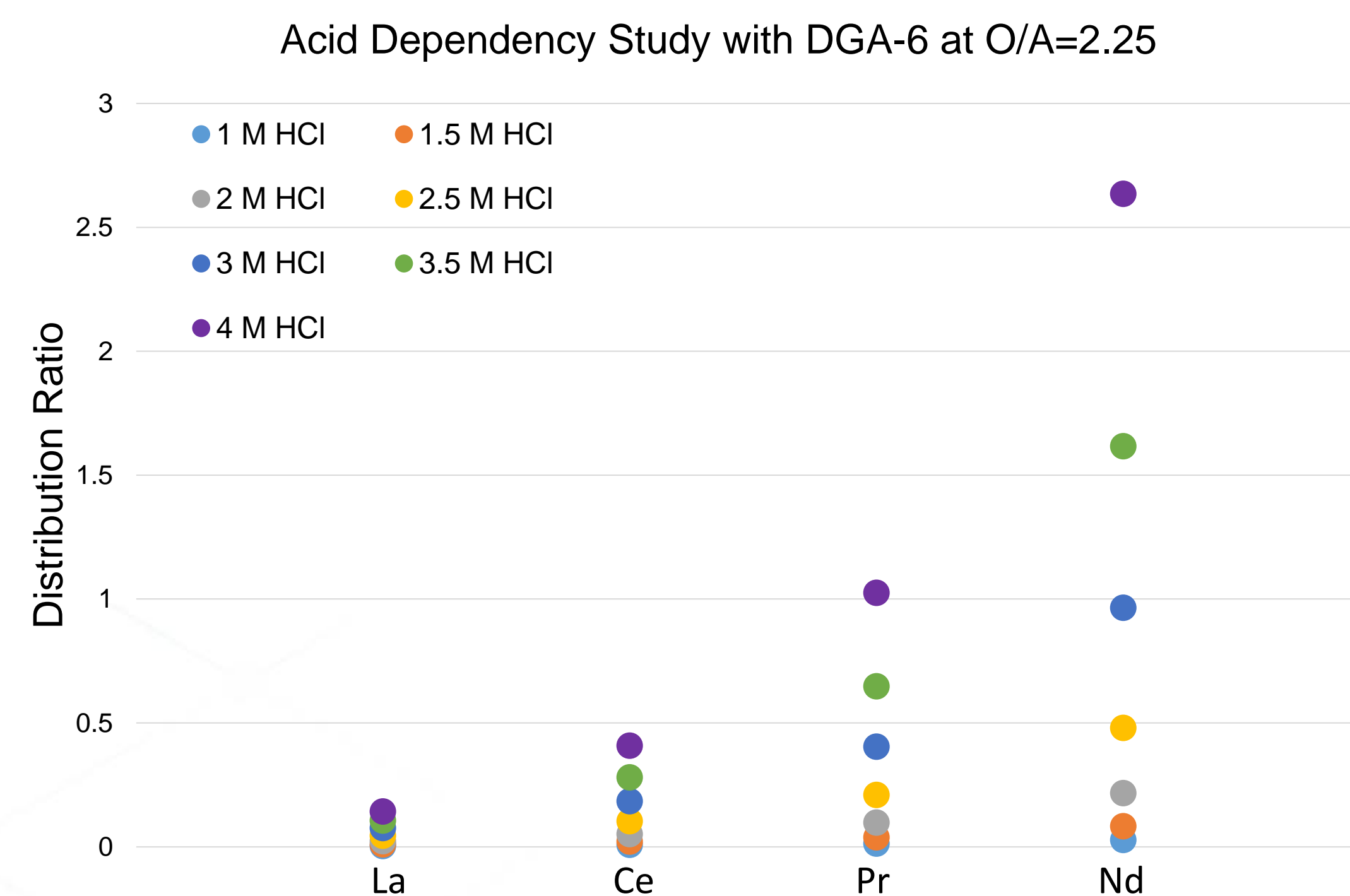
Preliminary Flowsheet Design

- Used assumptions derived from previous DGA experiments and phosphonic acid flow sheets to make necessary estimations for calculations
- Performed mass balance on the extraction, scrub, and strip sections in a DGA-6 preliminary flowsheet to determine the O/A in the extraction section:

O/A=2.25

Acid Dependency Study

- The acid concentrations in simulated leach liquors were varied to maximize extraction as well as separation of La and Ce from Nd and Pr



- Increased acid concentration directly correlates with distribution ratio as well as the split between La and Ce from Pr and Nd.

% Extraction				
[H+]	La	Ce	Pr	Nd
2.5 M	9.5%	19.9%	34.4%	57.0%
3 M	15.3%	30.9%	50.8%	74.2%
3.5 M	20.6%	41.5%	64.7%	86.1%
4 M	25.3%	51.0%	75.2%	93.2%

- Target acidity maximizes Pr and Nd recovery while minimizing co-extraction of Ce and La to reduce scrubbing requirements.

Future Work

- Further batch contact testing will be performed with the simulated leach liquor at the desired acid concentration, replicating counter current flow. Analysis will provide data for number of stages required in the final flowsheet design.
- The final flowsheet will be executed in mixer settlers with the DGA extractant provided by Marshallton Research Laboratories.

