

# Kr/Xe Separation and Capture Overview - US/UK collaboration

April 2021

Amy K Welty, Mitchell Greenhalgh, Troy G Garn, Meghan S Fujimoto





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**April 2021** 

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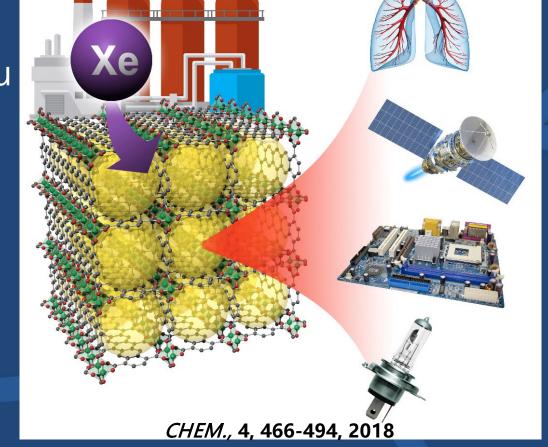
http://www.inl.gov

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# Kr/Xe Separation and Capture from Used Nuclear Fuel Reprocessing Off Gas

Praveen K. Thallapally, Alex Robinson, Jian Liu (PNNL) Mitchell Greenhalgh, Troy Garn, Meghan Fujimoto, Amy Welty (INL)

April, 2021





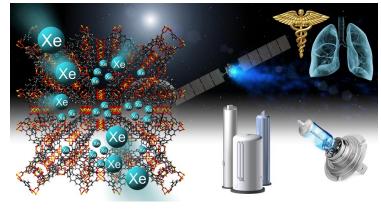
# **Current technology**

### Current Technology

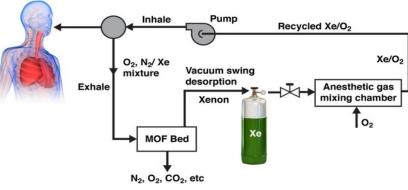
- > Cryogenic removal of Xe and Kr
  - Projected to be expensive
  - Potential for O<sub>3</sub> accumulation ⇒ hazardous conditions
  - 85Kr decay product Rb is a liquid at storage temperatures and corrosive
  - corrosion of storage canisters

### Porous materials

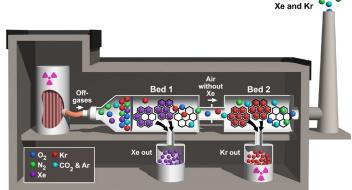
- Remove Xe and Kr in separate step:
- Remove Xe at ambient or low temperatures
   Recover process costs by selling Xe?
- Remove Kr at near room temperature
- MOFs and COFs (PNNL)
- AgZ and HZ (INL)



ACS. Mat. Lett., 2020, 3, 233-238



Chem. Eur. J., 23, 10758 - 10762, 2017

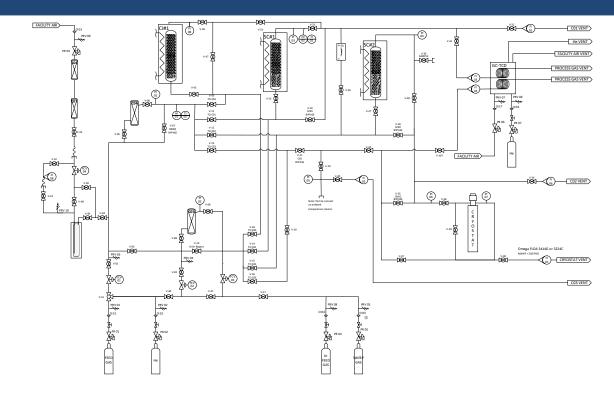


Acc. Chem. Res. 2015, 48, 2, 211-219

# Capabilities@PNNL and INL

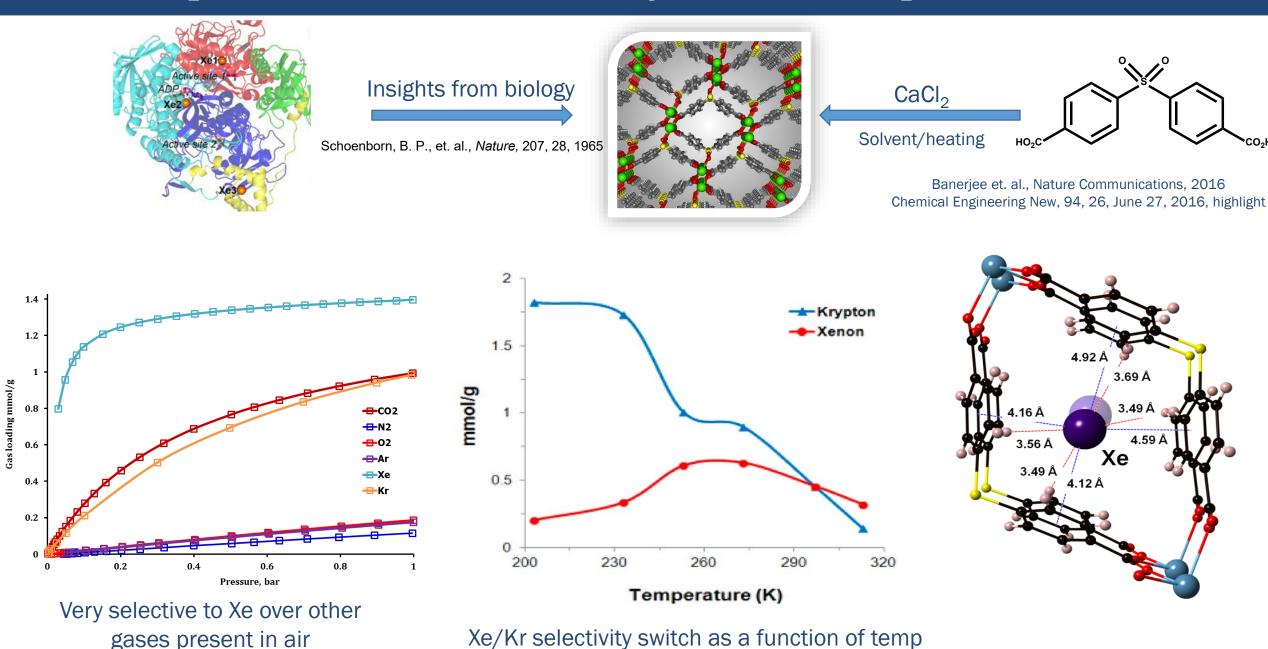


- > Computationally inspired material discovery
- Porous material characterization and testing
- ➤ Milligram to kilogram scale synthesis
- Bench scale demonstration in collaboration with industrial partners
- ➤ Full Patent on noble gas separation using MOFs and related materials USPTO WO/2017/218346A1
- Filled a provisional patent on making mechanically robust particles using PNNL proprietary approach
- ➤ Licensed the large-scale synthesis of material technology to Inna Venture, LA

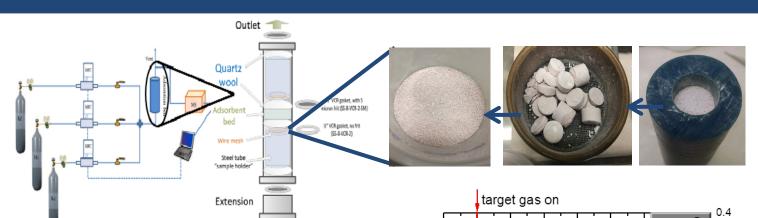


- ☐ Flexible test system designed to emulate real-world conditions
  - Operates at nearly any applicable temperature, pressure, or flow condition
  - ☐ Dual-stream, continuous gas analysis
- Zeolite sorbent production: Patent awarded 2014 (US 8,686,083 B2)
- □ Customer/partner sorbent testing

# Bio-inspired Material Discovery: Room Temperature Sorbent



# Single Column Breakthrough Experiments and Desorption



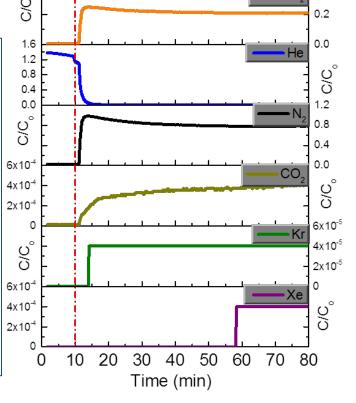
| Property                 | Value                 |
|--------------------------|-----------------------|
| Pressed Pressure         | 75 MPa                |
| Size                     | 500 – 850             |
| BET Surface area         | 15 m²/g               |
| BET Surface area, powder | 120 m <sup>2</sup> /g |

### > Conditions

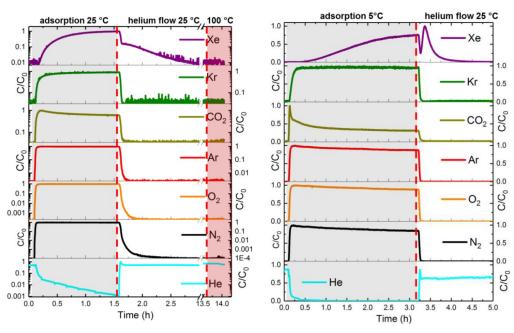
- Air = 78% N<sub>2</sub>, 21% O<sub>2</sub>, 0.9% Ar, 0.03% CO<sub>2</sub>, 1300 ppm Xe, 130 ppm Kr
- Flow rate = 20 cm<sup>3</sup>/min
- $T = 25 \, ^{\circ}\text{C} (298\text{K})$
- MOF = CaSDB

### > Results

- Xe capacity = ~30 mmol/kg vs 8 mmol/kg (NiMOF) and 22 mmol/kg (CC3)
- >95% of the Xe captured from air
- Xe/Kr (selectivity) = 15

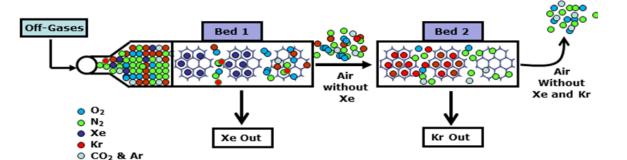


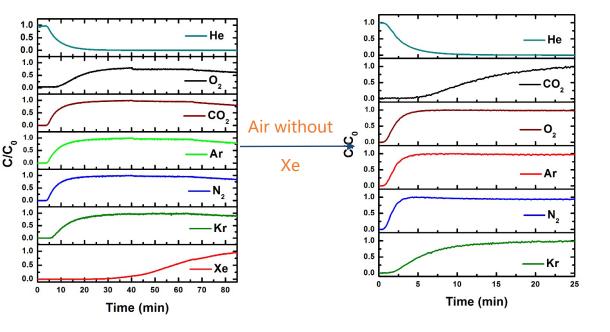
### Desorption experiments



Wet gas (RH 48%)

# Two Column Breakthrough Experiments





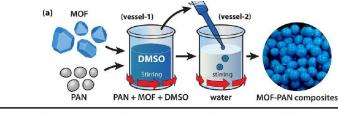
- A two-bed technique to remove and separate
  - Bed 1 remove Xe from air
  - Bed 2 remove Kr
    - Yields air without Xe and Kr
    - Off-gas can be released

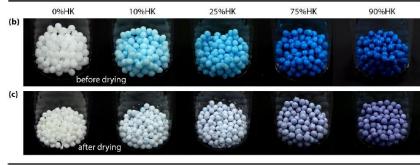
| Gas           | Breakthrough Time (min) | Capacity (mmol/kg)     | Selectivity of Xe |
|---------------|-------------------------|------------------------|-------------------|
| Xe            | 18                      | 16 (33.8) <sup>a</sup> |                   |
| Kr            | 1                       | $0.11(0.75)^{a}$       | 14                |
| $CO_2$        | 5                       | 1.2                    | 3                 |
| $N_2$         | 0.08                    | 47                     | 209               |
| Ar            | 0.08                    | 5.28                   | 210               |
| $O_2$         | 0.08                    | 12                     | 206               |
| 10 14 4 111 1 |                         |                        |                   |

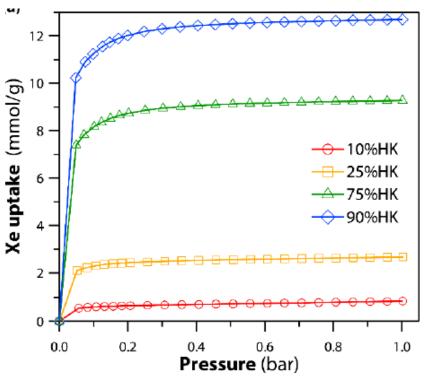
<sup>&</sup>lt;sup>a</sup> Capacity at equilibrium

| Gas             | Breakthrough Time (min) | Capacity (mmol/kg) | Selectivity of Kr |
|-----------------|-------------------------|--------------------|-------------------|
| Kr              | 2.5                     | 0.13               |                   |
| CO <sub>2</sub> | 7.5                     | 0.90               | 0.3               |
| $N_2$           | 0.25                    | 80.8               | 9.9               |
| Ar              | 0.25                    | 9.09               | 9.3               |
| O <sub>2</sub>  | 0.25                    | 21.2               | 9.3               |

# Low Temperature MOF Sorbent for Xenon







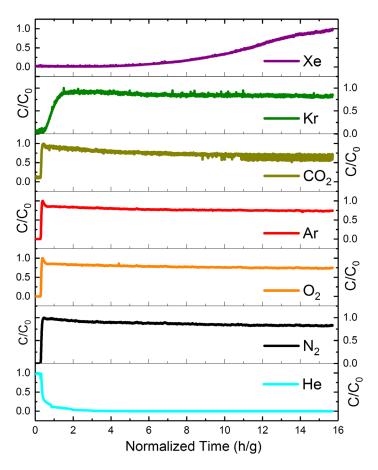
### **Conditions**

- Air = 78% N<sub>2</sub>, 21% O<sub>2</sub>, 0.9% Ar, 0.03% CO<sub>2</sub>, 1300 ppm Xe, 130 ppm Kr
- Flow rate = 20 cm<sup>3</sup>/min
- T = -78 °C
- MOF = CuBTC

### > Results

- Xe capacity = ~900 mmol/kg;
- >99% of the Xe captured from air;
- 12 times higher capacity than CaSDB MOF

### Low temperature (-78 C)



# Major Accomplishments

- Developed novel engineered form sorbents
  - AgZ-PAN and HZ-PAN
  - Patent awarded for the process
- Designed custom adsorption system
- Evaluated solid phase adsorption of Xe/Kr
- Published two journal articles
  - Journal of Nuclear Science and Technology, 51:4, 476-481, DOI: 10.1080/00223131.2014.877404
  - Journal of Nuclear Science and Technology, DOI:10.1080/00223131.2015.1126205
- Investigated sorbent cycling effects
- Demonstrated separation of Xe from Kr in a dual column system
- Produced a pure Kr stream from a Kr/Xe/Air mixture
- Evaluated desorption of Kr and Xe
- Performed other adsorption testing for external customers

# Engineered from sorbent development

# Mordenite powders incorporated into a macroporous polymer (PAN)

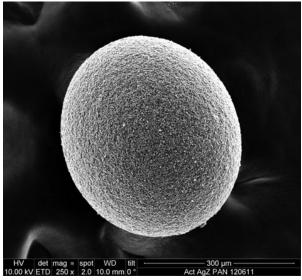
- H and Na powders ~80 wt. %
- Spherical beads 0.3-1.4 mm diameter
- Bulk density 0.3-0.4 g/mL
- Na form converted to silver form
- Patent awarded 2014 (US 8,686,083 B2)

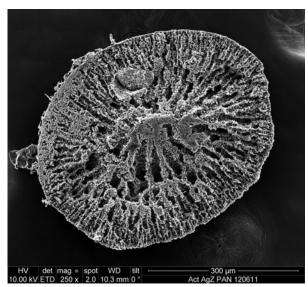
### HZ-PAN Sorbent

- BET surface area = 336 m<sup>2</sup>/g
- Micropore area  $(0.4-1.0 \text{ nm}) = 250 \text{ m}^2/\text{g}$

# AgZ-PAN Sorbent

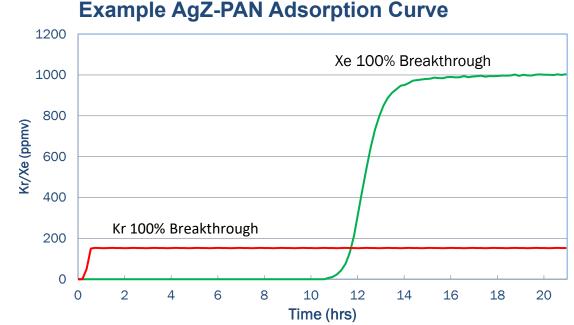
- BET surface area = 250 m<sup>2</sup>/g
- Micropore area  $(0.4-1.0 \text{ nm}) = 190 \text{ m}^2/\text{g}$





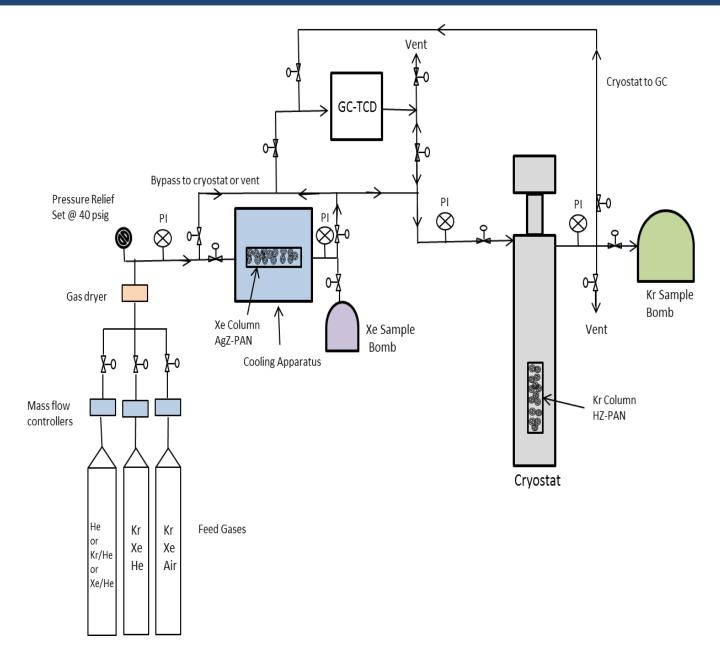
# **INL Adsorption Testing**

- AgZ-PAN
  - Highly selective for Xe over Kr
  - Temperatures 295 to 220 K
- HZ-PAN
  - High capacity for Kr in air
  - 191 K temperature
- Removal of Xe from Kr
  - Reduction in captured Kr volume
- Demonstrate feasibility of Xe removal with solid phase sorbents
- Produce pure Kr waste stream
- Determine adsorbed phase composition of both columns



# FY-15 Dual Column Tests

- Test Conditions
  - 1000 ppmv Xe, 150 ppmv Kr
  - Flow rate 50 sccm
  - 18.3 grams AgZ-PAN
  - 4.45 grams HZ-PAN
  - Superficial velocity
    - Xe column 23.0 cm/min
    - Kr column 18.7 cm/min
  - Column temperatures
    - Xe column 295 or 253 K
    - Kr column 191 K
  - Test times (stop
    - 55 minutes (295 K)
    - 105 minutes (253 K)



# AgZ-PAN and HZ-PAN cycle testing

## Cycling tests

- Evaluate sorbent efficacy over numerous thermal cycles
- Flow gas through columns at proposed adsorption/desorption temperatures
- Air and He evaluated as desorption gases
- Measure sorbent capacity intermittently to ensure sorbent doesn't lose performance

### AgZ-PAN

- Temperature range of 293 to 420 K
- Results, 100 cycles without decrease in capacity measurements
- An increase in capacity over time has been observed

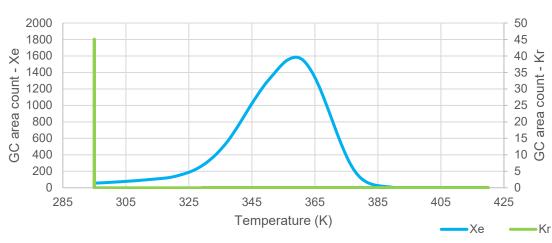
### HZ-PAN

- Temperature range 191 to 420 K
- 24 cycles and counting, no decrease in capacity observed to date

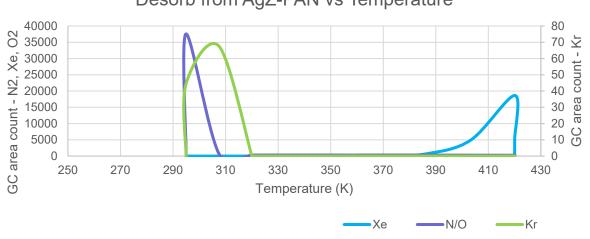
# FY-18 Desorption Studies

- AgZ-PAN
  - Xe/Kr separation
  - Ambient temperature adsorption
  - Adsorbed phase contains Xe, Kr and air
  - Desorption requires purge gas (He)
  - Ramp temperature slowly over 12 hours
  - Step temperature and soak 6 hours
  - 99-100% Xe separation

### Desorb from AgZ-PAN vs Temperature



### Desorb from AgZ-PAN vs Temperature



# Outside Interest from Research

### **PNNL**

### GAIN voucher with Flibe Energy

Noble gas management using MOFs with Liquid Fluoride Thorium Reactor

### **Praxair**

Interested in MOF technology to separate Xe from oxygen rich stream at room temperature /Kr separation

Involved in discussions with several companies including

### **DTRA Fundamental science**

Awarded a grant to understand the role of surface chemistry and pore size on noble gas adsorption

### DOE NP Isotope program

Involved in discussion with various labs who are working on isotope program to selectively trap noble gases

### INL

- GAIN voucher with GE-Hitachi
  - Enabling System Technologies to Improve the Economics and Performance of Existing LWRs and Advanced BWR Plants: Improving Off-gas System Performance
  - Recommendation made to improve monitoring and performance of off-gas system.
- Phase II SBIR with TDA Research Inc. from NASA
  - Testing of sorbents for Nuclear Thermal Propulsion (ground testing)
  - Testing Complete
- Licensed patent with Global Phosphate Solutions
  - "Phosphate Sponge"
  - Received R&D100 Special Recognition Green Tech Award

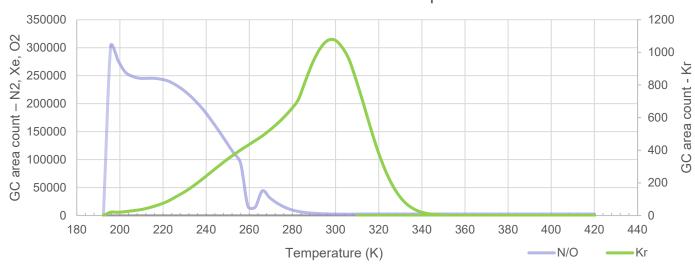
# Current/Future Research

- Continued MOF development with thin-bed testing
- Continued deep-bed testing of promising sorbents
- Focus on applied testing and optimization
- Advanced reactor off-gas treatment sorbents
- Alternate reprocessing (e.g. pyroprocessing) off-gas treatment sorbents

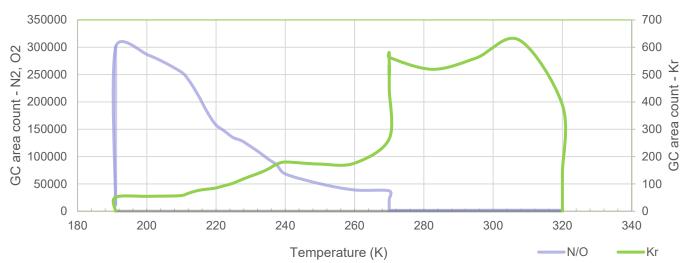
# **Backup Slides**

# FY-18 Desorption Studies





### Desorb from HZ-PAN vs Temperature



### HZ-PAN

- Kr capture
- 191 K adsorption
- Adsorbed phase contains
  Kr and air
- Desorption requires purge gas (He)
- Ramp temperature slowly over 12 hours
- Step temperature and soak 9 hours
- ~80% Kr separation
- 3.5 to 5 times Kr concentration

# FY-19 and 20 Desorption

# Desorption of HZ-PAN and AgZ-PAN

- AgZ-PAN Xe Desorb
- Investigated flow rate and temperature
- Viability of alternative sweep gas
  - Air
  - Argon
  - Nitrogen
- HZ-PAN Kr Desorb
  - Low flow Argon
  - Removal at near ambient temps

Moles of Kr

1.0E-06

5.0E-07

0.0E+00

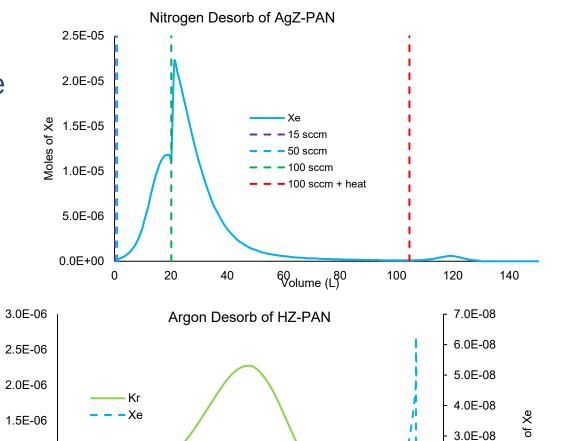
190

210

230

250

Temperature (K)



270

290

310

2.0E-08

1.0E-08

0.0E+00

330